

# Numerical Treatment of MHD Flow of Casson Nanofluid via Convectively Heated Non-Linear Extending Surface with Viscous Dissipation and Suction/Injection Effects

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**Abstract:** This paper introduces the effect of heat absorption (generation) and suction (injection) on magnetohydrodynamic (MHD) boundary-layer flow of Casson nanofluid (CNF) via a non-linear stretching surface with the viscous dissipation in two dimensions. By utilizing the similarity transformations, the leading PDEs are transformed into a set of ODEs with adequate boundary conditions and then resolved numerically by (4–5)<sup>th</sup>-order Runge-Kutta Fehlberg procedure based on the shooting technique. Numerical computations are carried out by Maple 15 software. With the support of graphs, the impact of dimensionless control parameters on the nanoparticle concentration profiles, the temperature, and the flow velocity are studied. Other parameters of interest, such as the skin friction coefficient, heat, and mass transport at the diverse situation and dependency of various parameters are inspected through tables and graphs. Additionally, it is verified that the numerical computations with the reported earlier studies are in an excellent approval. It is found that the heat and mass transmit rates are enhanced with the increasing values of the power-index and the suction (blowing) parameter, whilst are reduced with the boosting Casson and the heat absorption (generation) parameters. Also, the drag force coefficient is an increasing function of the power-index and a reduction function of Casson parameter.

**Keywords:** Casson nanofluid; viscous dissipation; MHD; heat generation; suction/injection

## 1 Introduction

Due to its large number of applications, the study of non-Newtonian fluids over an extending surface has attained great attention. In fact, the impacts of non-Newtonian behavior can be assessed by its elasticity, but their constitutive equations sometimes identify the rheological properties of the fluid. Provided the rheological parameters, the constitutive equations in the non-Newtonian fluids are more complex and thus giving rise to the complicated equations than the Navier–Stokes equations. Many of the liquids utilized in



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the oil sector, multiplex networks, cooling processes of micro-ships, open-flow switching, and simulating reservoirs are considerable non-Newtonian [1–5]. They show shear-dependent viscosity in different degrees. The concerted impacts of yield stress and boundary absorption on the flow of Casson fluid in a tube were checked by [6]. Casson fluid has special characteristics in the class of non-Newtonian fluids, which are commonly used in food manufacturing, metallurgy, drilling, and bio-engineering activities, etc. The definition of mixed convection stagnation-point flow of Casson fluid was proposed by [7] under the influence of convective boundary condition (CBC). Mukhopadhyay et al. [8] introduced the influence of the mass transfer in the presence of a chemical reaction on the MHD flow of the power-law fluids. Pramanik [9] explored the impact of the flow and heat transfer on Casson fluid's boundary-layer flow ahead of an asymmetric wedge. Mahantha et al. [10] tested the boundary-layer movement of a non-Newtonian fluid in the existence of suction (blowing) at the interface followed by heat transmission to an exponentially expanding plate. Khalid et al. [11] decided to the study of CBC mechanism for 3D hydro-magnetic flow of CNF and Casson fluid induced by linear and nonlinear elongating surfaces. Whereas, MHD Casson fluid of the time-dependent natural convection flowing over a movable vertical surface in a porous medium was observed by [12]. Nadeem et al. [13] inspected the effect of the magnetic parameter on CNF over a non-linearly extending plate.

A large number of examinations on the boundary-layer flow of CNF with various geometries have been carried out in recent years. The analytical solution of CNF in the existence of CBC results in the expanding surface was scrutinized by [14]. Wahiduzzaman et al. [15] deliberated the steady laminar flowing and heat transport of a CNF through a non-linearly expanding vertical cylinder numerically. Sulochana et al. [16] presented a computational problem of the boundary-layer flow over a non-isothermal porous surface of the 3D Casson fluid. The numerical computations of the radiation and the viscous dissipation impacts utilizing CBC for the issue of MHD Casson fluid of 3D flow via an elongating plate in a porous substance with a chemical reaction were intended by [17]. Khalid et al. [18] explored the influence of the magnetic field and the heat supply on a CNF steady flow and heat transmit over an exponentially expanding cylinder over its radial path. Besthapu et al. [19] tested in a porous substance with wall temperature, MHD time-dependent Casson fluid running over a vertical surface. Imtiaz et al. [20] probed CNF mixed convection magneto flow via a non-linear permeable extending plate with the viscous dissipation. Oyelakin et al. [21] looked at the CNF mixed convective flow created by an expanding cylinder under the impact of CBC. Afify [22] analyzed numerically, by using the spectral relaxation process, the impacts of radiation, heat source, and the concerted effect of the Soret and Dufour numbers on the Casson nanofluid via a time-dependent stretchable plate. Ibrahim et al. [23] numerically examined the effects of a chemical reactive flow and a viscous dissipation on CNF and heat transmission across an expanding area. Shah et al. [24] researched CNF mixed convective flowing with the chemically reactive species and heat source. Some neoteric researches related to a study of CNF flow can be found in [25–28].

All of the above studies are related to the examination of the influences of fluid motions over the diverse surfaces in Newtonian and non-Newtonian types. However, numerous studies have been performed to explore different types of flow and thermal impacts of nanofluid flow over various forms of surfaces. Eid et al. [29] investigated the analytical problem of 3D Oldroyd-B magneto nanofluid flow past an extending surface with CBC. Eid et al. [30] debated the concerted impacts of the magnetic field and the heat source (sink) on time-dependent convective heat and mass transmission past a permeable expanding wall of a power-law nanofluid. The heat transfer features of gold-based nanofluid flowing past a power-law expanding sheet were addressed by [31]. Eid et al. [32] inspected the impacts of the slip and heat source (sink) on the unsteady stagnation point flow and heat transport of a nanofluid over an extending plate in a porous material. Eid et al. [33] addressed the steady Sisko nanofluid flow and heat transport past a non-linearly expanding plate with the heat generation (absorption) in a porous material. With the

suction (injection) and the radiation, Hady et al. [34] checked the impact of the magnetic parameter on the two-phase Carreau nanofluid via a permeable non-linearly expanding plate. More related works in relation to these elements can be found in [35–45].

The goal of the current research is to present an inclusive numerical analysis of the impact of the heat absorption (generation) and the suction (blowing) on 2D Casson nanofluid hydro-magneto flow past a non-linear extending plate with the viscous dissipation. Consideration is granted to CBC on temperature. Similar solutions are implemented to transform nonlinear PDEs into ODEs. The outcomes are obtain by using the technique of Runge-Kutta Fehlberg of (4–5)<sup>th</sup>-order (RFK4-5). Embedded parameter behaviors are accentuated through graphical and tabular results.

### 2 Problem Structure

Consider MHD CNF flow in the region ( $y > 0$ ) over an exponentially extendable surface as 2D viscous, steady, and incompressible with the influence of the viscous dissipation and the heat source (sink). The Cartesian coordinates  $(x, y)$  select wherein the  $x$ -axis of the surface is measured while the  $y$ -axis is perpendicular to it. The extendable sheet is expected to have a global velocity profile of the power-law  $u_w(x) = a x^n$  where  $a > 0, n \geq 0$  are constants. The action of the magnetic field is subjected to varying strength  $B(x) = B_0 x^{(n-1)/2}$ . There is no electrical field, but the induced magnetic field is ignored by the weak magnetic number of Reynolds. The temperature of the surface is designated by a relation  $T_w(x) = T_\infty + A x^n$  where  $A > 0$  is a fixed value,  $T_\infty$  is the free stream temperature and  $C_\infty$  is the ambient nanoparticles concentration. The flow model and coordinate scheme are shown in Fig. 1.

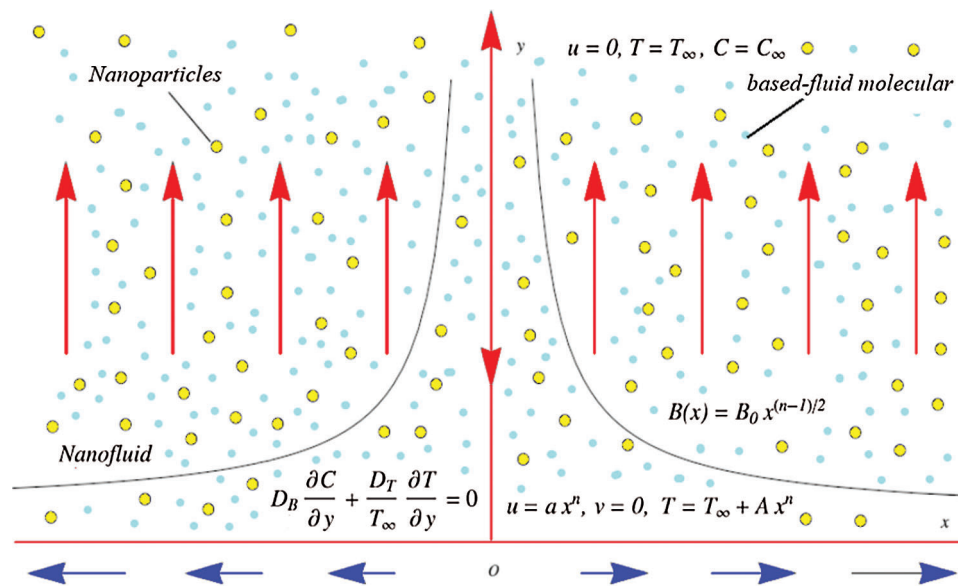


Figure 1: Geometry of flow scheme

The rheological state equation for a Casson fluid isotropic fluid is [13,15]:

$$\tau_{ij} = \begin{cases} 2 \left( \mu_B + P_z / \sqrt{2\pi} \right) e_{ij}, \pi > \pi_c \\ 2 \left( \mu_B + P_z / \sqrt{2\pi} \right) e_{ij}, \pi < \pi_c \end{cases} \quad (1)$$

where  $\pi = e_{ij}e_{ij}$  and  $e_{ij}$  symbols for the  $(i,j)^{th}$  deformation component rate,  $\pi$  is the deformation component rate product,  $\pi_c$  signifies to the non-Newtonian fluid critical value of this multiple,  $\mu_B$  mentions to Casson fluid plastic viscosity and  $P_y$  the fluid yield stress. Let us consider the components of velocity  $V = [u(x, y), v(x, y), 0]$ , the temperature relation  $T = T(x, y)$  and nanoparticle concentration  $C = C(x, y)$ . The momentum, temperature and the concentration equations in a Casson nanofluid following above-mentioned conditions are written as

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \quad (2)$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = v \left( 1 + \frac{1}{\beta} \right) \left( \frac{\partial^2 u}{\partial y^2} \right) - \frac{\sigma B^2(x)}{\rho_f} u \quad (3)$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha \left( \frac{\partial^2 T}{\partial y^2} \right) + \frac{Q_0}{\rho c_p} (T - T_\infty) + \tau \left[ D_B \left( \frac{\partial T}{\partial y} \frac{\partial C}{\partial y} \right) + \frac{D_T}{T_\infty} \left( \frac{\partial T}{\partial y} \right)^2 \right] + \frac{v}{c_p} \left( 1 + \frac{1}{\beta} \right) \left( \frac{\partial u}{\partial y} \right)^2 \quad (4)$$

$$u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} = D_B \left( \frac{\partial^2 C}{\partial y^2} \right) + \frac{D_T}{T_\infty} \left( \frac{\partial^2 T}{\partial y^2} \right) \quad (5)$$

where  $u$  and  $v$  are the components of velocity over the  $x$ - and  $y$ -coordinates respectively,  $\nu$  is the kinematic viscosity,  $\beta = \mu_B \sqrt{2\pi_c} / P_y$  is the parameter of Casson,  $\sigma$  is the conductivity electrical field,  $\rho$  is the density, the thermal diffusivity is denoted by  $\alpha$ ,  $D_T$  and  $D_B$  are the coefficients of the thermophoresis and Brownian diffusions,  $Q_0$  is the coefficient of the heat source (sink) in dimensional form,  $c_p$  stands for the specific heat, and  $\tau = (\rho c)_p / (\rho c)_f$  indicates the nanoparticle material's ratio of the effective heat capacity to efficient liquid heat capacity. The related boundary-conditions of the current problem are

$$\left. \begin{aligned} u = u_w(x) = ax^n, v = v_w, T = T_w(x) = T_\infty + Ax^n, D_B \left( \frac{\partial C}{\partial y} \right) + \frac{D_T}{T_\infty} \frac{\partial T}{\partial y} \text{ at } y = 0 \\ u \rightarrow 0, T \rightarrow T_\infty, C \rightarrow C_\infty \text{ as } y \rightarrow \infty \end{aligned} \right\} \quad (6)$$

The system of Eqs. (2)–(5) and the concerning conditions (6) are non-dimensionalised by the following conversion

$$\left. \begin{aligned} u = ax^n f'(\eta), v = -ax^{\frac{n-1}{2}} \sqrt{\frac{\nu}{a}} \left( \frac{n+1}{2} f(\eta) + \frac{n-1}{2} \eta f'(\eta) \right), \eta = \sqrt{\frac{a}{\nu}} x^{\frac{n-1}{2}} y \\ \theta(\eta) = \frac{T - T_\infty}{T_w - T_\infty}, \phi(\eta) = \frac{C - C_\infty}{C_w - C_\infty} \end{aligned} \right\} \quad (7)$$

Eq. (2) is identically verified and Eqs. (3)–(6) converted to

$$\left( 1 + \frac{1}{\beta} \right) f''' - \eta f'^2 + \frac{n+1}{2} f f'' - M f' = 0 \quad (8)$$

$$\frac{1}{Pr} \theta'' + \frac{n+1}{2} f \theta' - \eta f' \theta + \lambda \theta + Nb \theta' \phi' + Nt \theta'^2 + \left( 1 + \frac{1}{\beta} \right) Ec f''^2 = 0 \quad (9)$$

$$\phi'' + \frac{n+1}{2} Sc f \phi' + \frac{Nb}{Nt} \theta'' = 0 \quad (10)$$

The related conditions are

$$\left. \begin{aligned} f(0) = f_w, f'(0) = 1, \theta(0) = 1, Nb\phi'(0) + Nt\theta'(0) = 0, \quad \text{at } \eta = 0 \\ f'(\infty) \rightarrow 0, \theta(\infty) \rightarrow 0, \phi(\infty) \rightarrow 0 \quad \text{as } \eta \rightarrow \infty \end{aligned} \right\} \quad (11)$$

In the overhead formulas  $M$  is the parameter of the magnetic field,  $Pr$  symbols to the number of Prandtl,  $Nb$  is the Brownian motion parameter,  $Nt$  is the thermophoresis diffusion,  $\lambda$  is the heat generation ( $\lambda > 0$ ) or absorption ( $\lambda < 0$ ),  $Ec$  is Eckert number,  $Sc$  is the Schmidt number,  $f_w$  is the suction (blowing) parameter ( $f_w > 0$  for suction and  $f_w < 0$  for blowing). These are defined as below:

$$\left. \begin{aligned} Pr = \frac{\nu}{\alpha}, Sc = \frac{\nu}{D_B}, M = \frac{\sigma B_0^2}{a\rho}, \lambda = \frac{Q_0}{u_w \rho c_p} \\ Nb = \frac{(\rho c)_p D_B (C_w - C_\infty)}{(\rho c)_f \nu}, Ec = \frac{u_w^2}{(T_w - T_\infty) c_p} \\ Nt = \frac{(\rho c)_p D_T (T_w - T_\infty)}{(\rho c)_f T_\infty \nu}, f_w = \frac{-2\nu_w}{(n+1)a^{1/n} \sqrt{\nu u_w^{(2n-1)/2n}}} \end{aligned} \right\} \quad (12)$$

The amounts of practical attention include the drag force coefficient  $C_f$ , local Nusselt  $Nu_x$  and local Sherwood  $Sh_x$  numbers, are known as follows:

$$C_{fx} = \frac{\tau_w}{\rho u_w^2}, Nu_x = \frac{xq_w}{k(T_w - T_\infty)}, Sh_x = \frac{xq_m}{D_B(C_w - C_\infty)} \quad (13)$$

where  $\tau_w$  is the wall shear stress,  $k$  signalizes to the thermal nanofluid conductivity and  $q_w, q_m$  are the surface heat and mass flux, which are specified by

$$\tau_w = \mu_B \left(1 + \frac{1}{\beta}\right) \left(\frac{\partial u}{\partial y}\right)_{y=0}, q_w = -k \left(\frac{\partial T}{\partial y}\right)_{y=0}, q_m = -D_B \left(\frac{\partial C}{\partial y}\right)_{y=0} \quad (14)$$

Substituting Eqs. (7) and (14) into Eq. (13), we obtain

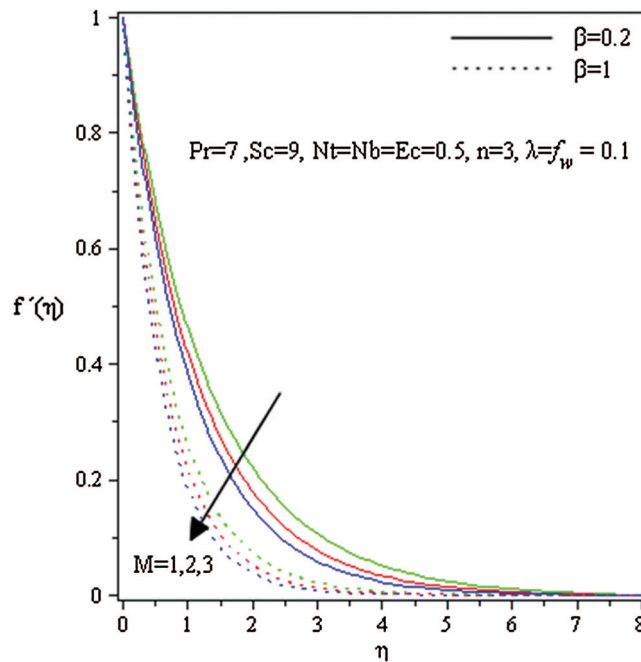
$$Re_x^{1/2} C_{fx} = \left(1 + \frac{1}{\beta}\right) f''(0), Re_x^{-1/2} Nu_x = -\theta'(0), Re_x^{-1/2} Sh_x = -\phi'(0) \quad (15)$$

wherever  $Re_x = \frac{u_w x}{\nu}$  is the local Reynolds number.

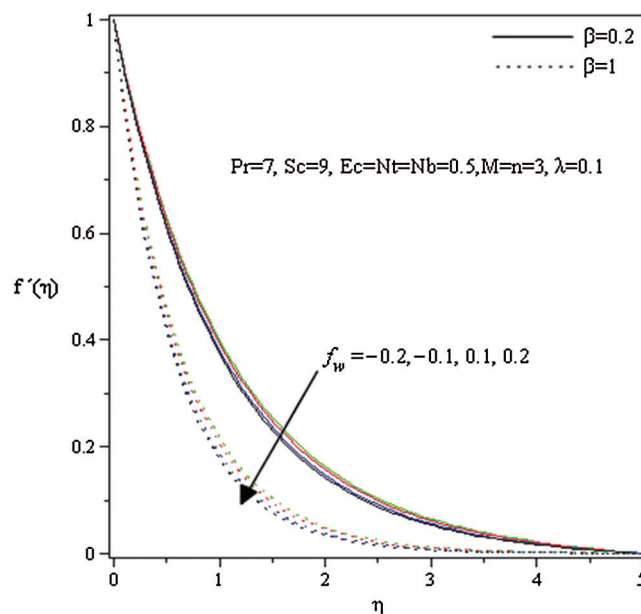
### 3 Results and Discussion

The effects of the different physical parameters values in order to have a physical understanding of the problem like, the magnetic  $M$ , suction (blowing)  $f_w$ , Casson  $\beta$ , Eckert number  $Ec$ , heat source (sink) parameter  $\lambda$ , thermophoretic diffusion  $Nt$ , Brownian diffusion  $Nb$ , the Prandtl number  $Pr$  and power-law index  $n$  on the profiles of velocity  $f'(\eta)$ , temperature  $\theta(\eta)$ , the volume fraction  $\phi(\eta)$ , drag force  $Re_x^{1/2} C_{fx}$ , local Nusselt  $Re_x^{-1/2} Nu_x$  and local Sherwood  $Re_x^{-1/2} Sh_x$  numbers are examined numerically and showed through Figs. 2–17. The validity of the developed code is checked for special cases to evaluate the accuracy of the current results with the previously published results of [13] for the rate of heat transfer at the plate  $Re_x^{-1/2} Nu_x$  for different values of  $n, Pr, Nt, Sc, \beta$  and  $M$  when  $f_w = \lambda = Ec = 0$ , and  $Nb = 0.5$  (Tab. 1) and established a very excellent accordance. This allows us to ensure our numerical findings. Figs. 2 and 3 depict the effects of magnetic parameter  $M$ , suction (blowing)  $f_w$  and Casson parameter  $\beta$  on velocity profile  $f'(\eta)$  for other parameters fixed values. It is detected that the increment in  $\beta$  increases the fluid viscosity due to applied stress that at the latest decelerates the flow of a nanofluid along the

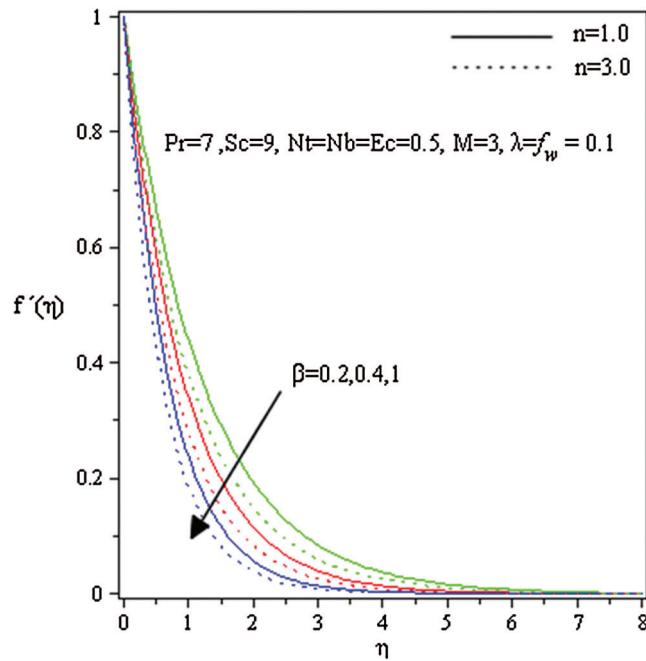
$x$ -direction. Therefore, the velocity of flow and the thickness of momentum-layer are reduced. Similar result is shown in Fig. 2 when the parameter of the magnetic  $M$  increases. Physically, the impact of the magnetic value  $M$  rises due to the Lorentz forces become a stronger along the direction perpendicular to  $x$ -axis that offers more resistance in the fluid flows as a result in the velocity profile is reduced. It is noted that the flow velocity of nanofluid is diminished with a rising different estimations of  $\beta$  and  $M$ . Fig. 3 reveals the flow velocity of a nanofluid is reduced with an upsurge in  $f_w$ . Fig. 4 represents the influence of  $\beta$  on the velocity for both taking values of  $n = 1$  and  $n = 3$ . It is seen that an upsurge in  $\beta$  leads to a reduction in nanofluid movement. That velocity of Casson nanofluid when  $n = 3$  is greater than the Newtonian fluid when  $n = 1$ .



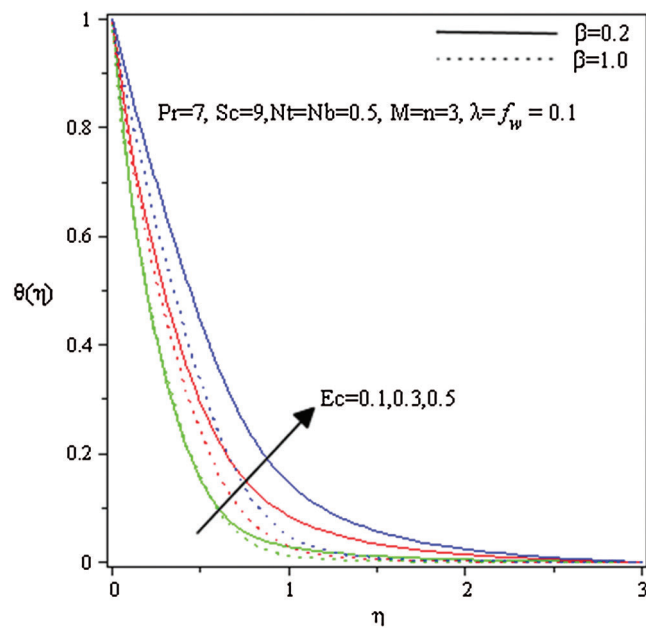
**Figure 2:** Influence of  $M$  and  $\beta$  on  $f'$



**Figure 3:** Influence of  $f_w$  and  $\beta$  on  $f'$



**Figure 4:** Influence of  $n$  and  $\beta$  on  $f'$

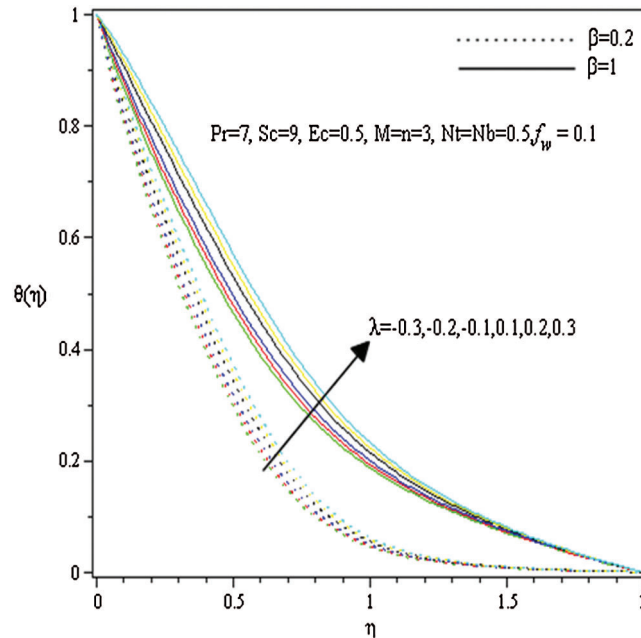


**Figure 5:** Influence of  $Ec$  and  $\beta$  on  $\theta$

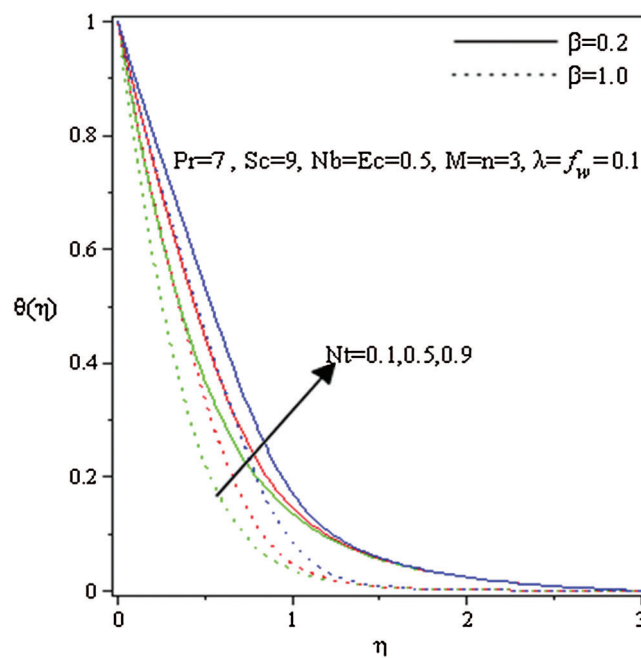
Figs. 5–8 depict the influences of Eckert number  $Ec$ , heat source (sink) parameter  $\lambda$ , thermophoresis parameter  $Nt$  and suction (blowing) parameter  $f_w$ , respectively on temperature profile  $\theta(\eta)$  for two cases  $\beta = 0.2$  and  $\beta = 1$ , whilst the further parameters are constant. In fact, it is clear that a growth in the value of  $\beta$  leads to an increase in the temperature outline. Physically, this happened due to high values of  $\beta$  indicating stronger molecular motion as well as interactions that ultimately increase the fluid temperature. Fig. 5 prepares to perceive the influence of Eckert number on temperature distribution  $\theta(\eta)$ . It is showed that the



fluid's temperature significantly is raised as Eckert number  $Ec$  increases. Physically, the viscosity of the fluid in a viscous flow absorbs the kinetic energy from the fluid's motion and transforms it into internal energy which is heated the fluid. This operation is partly irreversible and is known as the viscous dissipation. Fig. 6 elaborates  $\theta(\eta)$  variation with the different amounts of heat source (sink)  $\lambda$  in a constant worth case of other parameters. It is displayed that the heat source upsurges the temperature and correspondence thermal-layer thickness. This is due to the heat source (sink) raises extra heat to the surface, which defines that the produced heat in the boundary layer is increased and contributes to a higher temperature area.

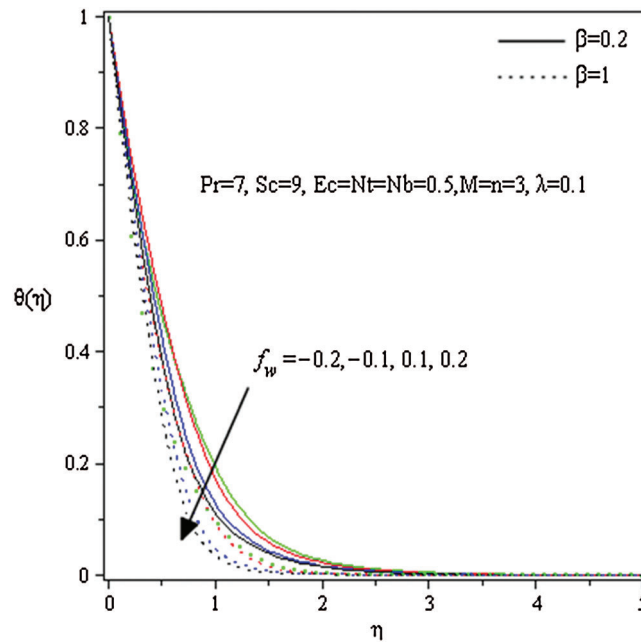


**Figure 6:** Influence of  $\lambda$  and  $\beta$  on  $\theta$

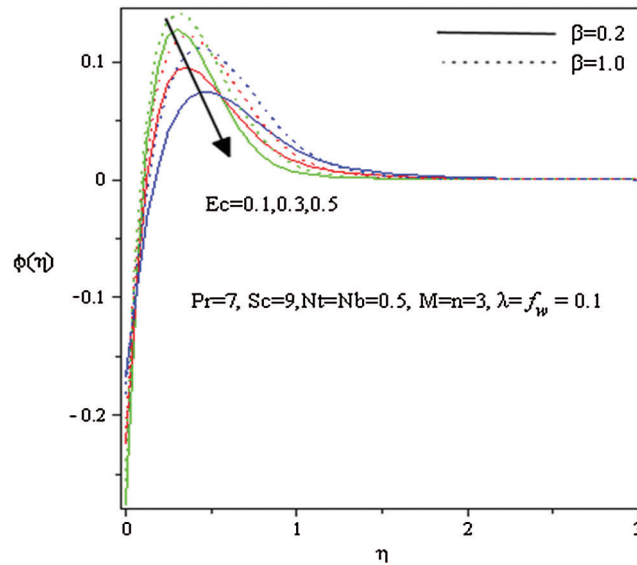


**Figure 7:** Influence of  $Nt$  and  $\beta$  on  $\theta$



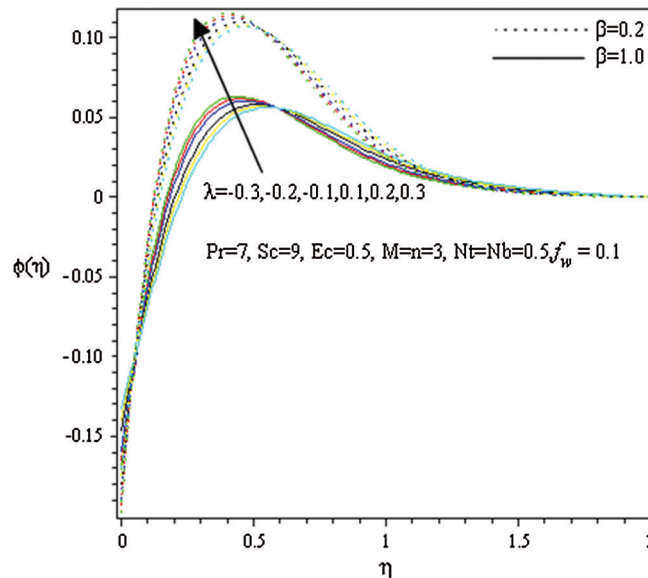


**Figure 8:** Influence of  $f_w$  and  $\beta$  on  $\theta$

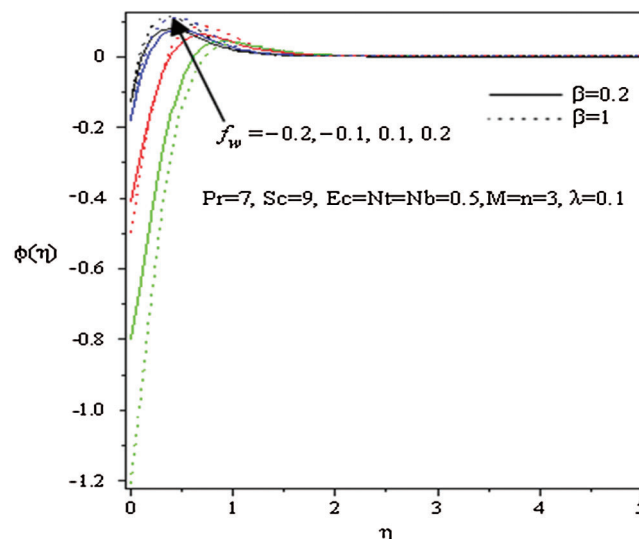


**Figure 9:** Influence of  $Ec$  and  $\beta$  on  $\phi$

Fig. 7 includes the effect of thermophoresis parameter  $Nt$  on the temperature distribution  $\theta(\eta)$ . It is noticed that the temperature outline with the thickness of the thermal-layer is increased with the snowballing values of  $Nt$ . Physically, in the thermophoretic effect, due to the temperature pattern control, the nanoparticles migrate from the hot stretch board to the cold fluid in the ambient. The influence of suction (blowing) parameter  $f_w$  on the heat profile is displayed in Fig. 8. It is noteworthy that an upsurge in  $f_w$  decreases the nanofluid heat and thermal-layer thickness. This is because of the suction; the hot nanofluid is pulled near to surface.



**Figure 10:** Influence of  $\lambda$  and  $\beta$  on  $\phi$



**Figure 11:** Influence of  $f_w$  and  $\beta$  on  $\phi$

Figs. 9–12 represent the effects of Eckert number  $Ec$ , heat source (sink) parameter  $\lambda$ , suction (blowing) parameter  $f_w$  and Brownian diffusion  $Nb$  on the volume fraction  $\phi(\eta)$  for both the cases  $\beta = 0.2$  and  $\beta = 1$ , when the other parameters are fixed. The impact of Eckert parameter on the volume fraction profile is plotted in Fig. 9. It is clearly noted that the concentration distribution is improved with the snowballing of  $\beta$  values. It is also noticed that  $\phi(\eta)$  is declined with the increasing of Eckert number. Fig. 10 illustrates the impact of  $\lambda$  on  $\phi(\eta)$ . It is observed that  $\phi(\eta)$  is declined with the increasing values of  $\beta$  while it is increased with the increment of  $\lambda$ . The suction (blowing) effect on the distribution of  $\phi(\eta)$  is portrayed in Fig. 11. It is observed that  $\phi(\eta)$  outline is raised with the swelling values of both  $f_w$  and  $\beta$ . Fig. 12 reveals the effect of the Brownian  $Nb$  parameter on  $\phi(\eta)$ . It is observed that  $\phi(\eta)$  is decreased with  $Nb$  while it is increased with the parameter  $\beta$ .

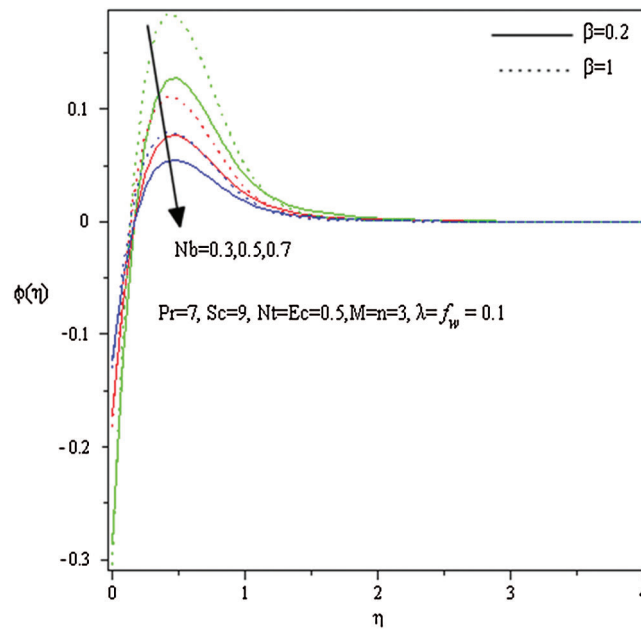


Figure 12: Influence of  $Nb$  and  $\beta$  on  $\phi$

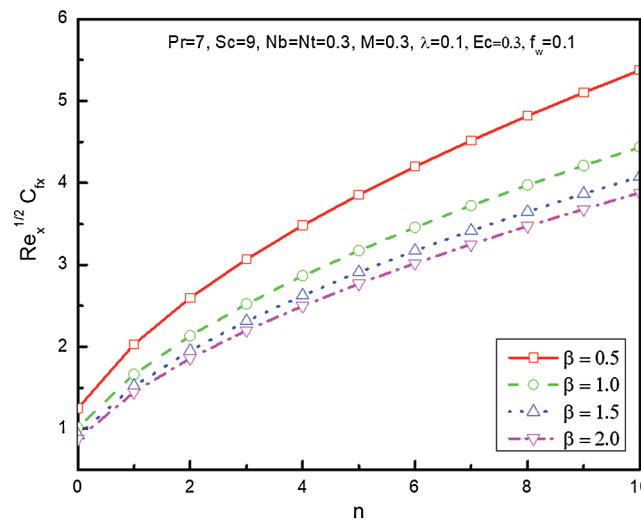


Figure 13: Influence of  $n$  and  $\beta$  on  $Re_x^{1/2}/C_{fx}$

Figs. 13–17 demonstrate the influences of the diverse parameters on the drag force coefficient  $Re_x^{1/2}C_{fx}$ , Nusselt  $Re^{-1/2}Nu_x$ , and Sherwood  $Re^{-1/2}Sh_x$  numbers. Fig. 13 elucidates the effects of  $Re_x^{1/2}C_{fx}$  against  $n$  for different values of  $\beta$ . It is found that  $Re_x^{1/2}C_{fx}$  is increased when  $n$  increases while it is reduced with an increment in  $\beta$ . Fig. 14 depicts the variation of  $Re^{-1/2}Nu_x$  with Eckert number  $Ec$  for diverse values of  $n$ . It is remarked that the heat transfer rate is increased with the snowballing values of  $n$ , whilst an upsurge in Eckert number  $Ec$  occurs a diminish in the magnitude heat transport rate. Fig. 15 demonstrates the variation of  $Re^{-1/2}Nu_x$  with  $\lambda$  for various amounts of  $\beta$ . It is found that an upsurge in both parameters  $\lambda$  and  $\beta$  leads to a reduction in the scale of the Nusselt number. Fig. 16 depicts the Nusselt number differences with  $f_w$  for different values of  $Pr$ . It is simple to understand from the figure that the heat

transport rate is boosted with the increment values of both  $Pr$  and  $f_w$ . Fig. 17 shows the variation of  $Re_x^{-1/2}Sh_x$  with  $f_w$  for different power index values  $n$ . It is remarked that a rise in both  $f_w$  and  $n$  occurs an upsurge in the magnitude of  $Re_x^{-1/2}Sh_x$ .

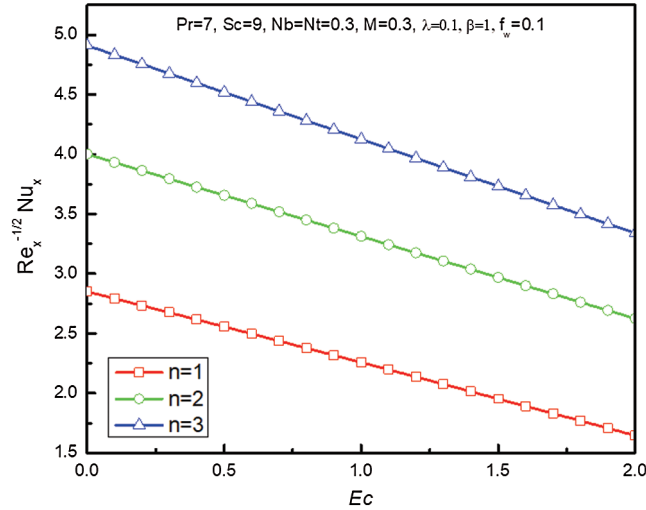


Figure 14: Influence of  $Ec$  and  $n$  on  $Re_x^{-1/2}/Nu_x$

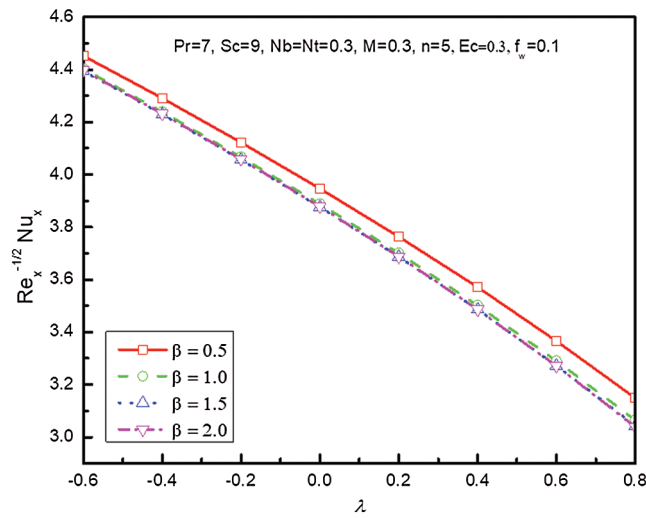


Figure 15: Influence of  $\lambda$  and  $\beta$  on  $Re_x^{-1/2}/Nu_x$

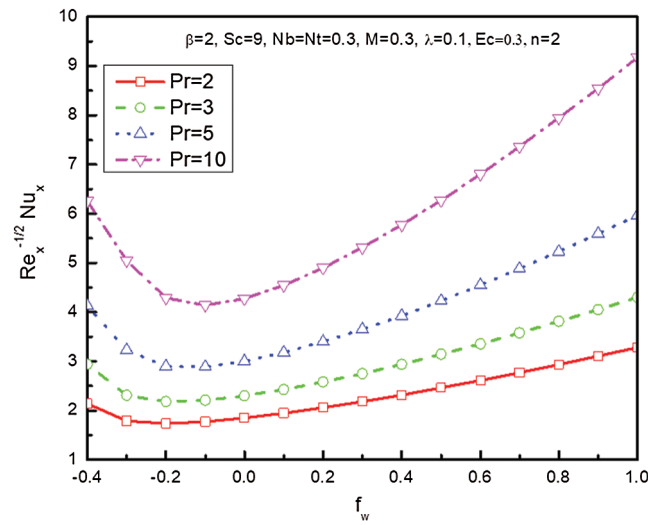


Figure 16: Influence of  $f_w$  and  $Pr$  on  $Re_x^{-1/2}/Nu_x$

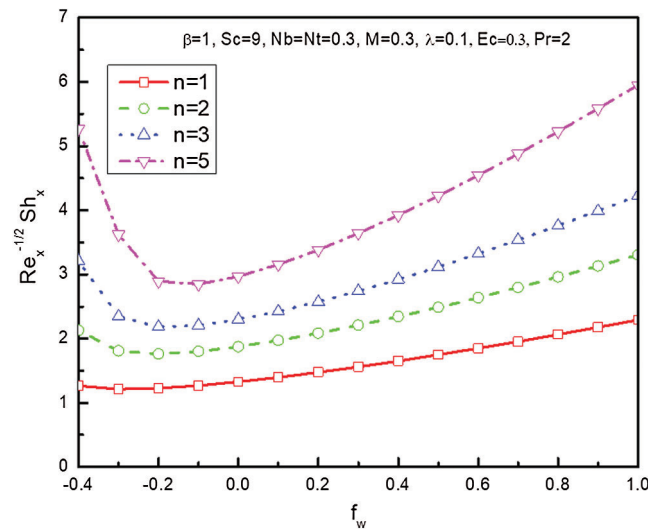


Figure 17: Influence of  $f_w$  and  $n$  on  $Re_x^{-1/2}/Sh_x$

Table 1:  $|\theta'(\eta)|$  for distinct values of  $n, Nt, Pr, Sc, \beta$  and  $M$  when  $Ec = f_w = \lambda = 0$

$n$	$Nt$	$Pr$	$Sc$	$\beta$	$M$	$-\theta'(0)$		
						[13]		Present work
						Shooting technique	bvp4c code	
0.5	0.1	7	20	0.6	3	2.12068	2.12069	2.12068
0.5	0.5	7	20	0.6	3	1.63864	1.63865	1.63864
0.5	0.9	7	20	0.6	3	1.37927	1.37928	1.37927
0.1	0.5	7	5	0.6	3	2.69156	2.69155	2.69154

(Continued)

**Table 1 (continued).**

$n$	$Nt$	$Pr$	$Sc$	$\beta$	$M$	$-\theta'(0)$		
						[13]		Present work
						Shooting technique	bvp4c code	
0.1	0.5	7	10	0.6	3	2.51354	2.51354	2.51353
0.1	0.5	7	20	0.6	3	2.31554	2.31555	2.31554
1.5	0.5	3	20	0.6	3	2.43078	2.43078	2.43078
1.5	0.5	5	20	0.6	3	2.85270	2.85272	2.85270
1.5	0.5	7	20	0.6	3	3.21459	3.21459	3.21459
2	0.5	7	20	0.2	3	3.41143	3.41146	3.41143
2	0.5	7	20	0.6	3	3.31040	3.31042	3.31040
2	0.5	7	20	1.0	3	3.26319	3.26323	3.26319
3	0.5	7	20	0.6	0	4.18830	4.18832	4.18830
3	0.5	7	20	0.6	1	4.14820	4.14822	4.14820
3	0.5	7	20	0.6	3	4.08219	4.08221	4.08219

#### 4 Conclusions

A numerical solution of the effect on the MHD boundary layer flux of CNF on a non-linear extending plate with the viscous dissipation in two dimensions with the heat absorption (generation) and the suction (blowing) are scrutinized. The numerical computations are performed by the assist of 4–5<sup>th</sup>-order Runge-Kutta Fehlberg technique depends on the shooting process. The significant findings of the study are next:

- Velocity profile is reduced with the growing of  $M$ ,  $\beta$ ,  $n$ , and  $f_w$  values.
- Temperature profile is improved with the growing of  $Ec$ ,  $\lambda$  and  $Nt$  values while decreases when  $f_w$  increases.
- Concentration distribution is enhanced with the increasing of  $\lambda$  and  $f_w$  values while decreases when  $Ec$  and  $Nb$  increase.
- Nusselt number is boosted when  $Pr$ ,  $n$ , and  $f_w$  increase while, it is diminished when  $Ec$ ,  $\beta$ , and  $\lambda$  increase.
- Sherwood number is enhanced when  $f_w$  and  $n$  increase.
- Drag force coefficient is boosted when  $n$  increases, while it decreases when  $\beta$  increases.

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