

## Study of Solar Thermal Power Generation Based on Reverse Electrodialysis

Jianjun He\*, Ruifeng Wang, Yefeng Yin, Jian Chen and Chaoran Guo

School of Energy and Power Engineering, Changsha University of Science & Technology, Changsha, 410114, China

\*Corresponding Author: Jianjun He. Email: hejianjun329@126.com

Received: 24 April 2020; Accepted: 08 June 2020

**Abstract:** TPG-RED (Thermal Power Generation Based on Reverse Electrodialysis) was studied to explore the new method of solar thermal power generating based on Reverse Electrodialysis (RED) in this paper. RED is a process that transfers the salinity gradient between sea water and fresh water to electricity. TPG-RED has combined RED with thermal power generation to transfer thermal energy from solar to electricity which has many advantages of huge available temperature range, sustainability, non-pollution, simple structure, and so on. Respectively, using “1 mol/L H<sub>2</sub>SO<sub>4</sub> solution—0.0001 mol/L H<sub>2</sub>SO<sub>4</sub> solution” and “1 mol/L Na<sub>2</sub>SO<sub>4</sub> solution—0.0001 mol/L Na<sub>2</sub>SO<sub>4</sub> solution” as the working medium at 30°C heat source temperature to carry out power generating experiment. After 400 min, both open circuit voltages reached 28.4 and 31.0 mV respectively and initial output current were 267 and 295 μA respectively, after 120 min discharging, the output current was basically stable, reached 7 and 5 μA respectively. The effect of heat source temperature on output current shows that TPG-RED can generate electricity at 20°C–55°C heat source temperature, and the output current increased with the temperature increasing. In the ion exchange membrane solution concentration limit, the output current increased with the concentration difference increasing.

**Keywords:** Solar energy; reverse electrodialysis; thermal power generation; temperature; concentration difference

### 1 Introduction

China's energy consumption is still dominated by fossil energy, which is mostly utilized in the form of thermal energy. Abundant thermal form of energy such as solar thermal and geothermal are stored in the natural world. In recent years, the solar energy as a kind of clean and renewable energy is applied in many areas [1,2]. With the increasing demand of energy conversion and waste-heat utilization, it is important to study how to use solar energy effectively [3,4].

Converting solar energy into electrical energy is one of the most valuable way to utilize solar energy [5]. At present, Solar thermal power plants can produce high-temperature heat that is converted into electricity by conventional power cycles [6,7]. The utilization of high-temperature thermal energy has been relatively mature, but for low-temperature thermal energy, it is still in the research stage.



This work is licensed under a Creative Commons Attribution 4.0 International License, which permits unrestricted use, distribution, and reproduction in any medium, provided the original work is properly cited.

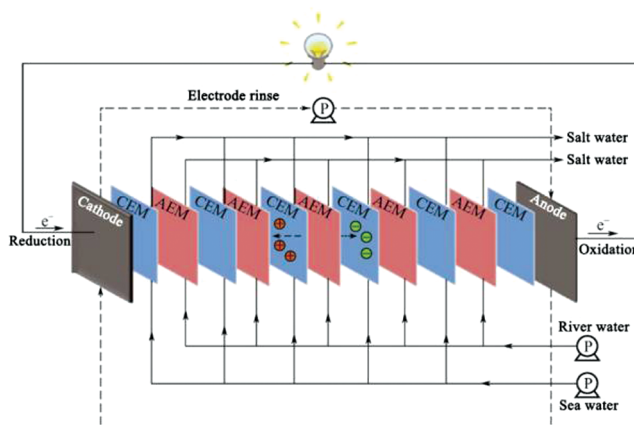
Some thermodynamic cycles, such as the Organic Rankine Cycle (ORC) and the Kalina Cycle are applied to industrial waste heat power generation. ORC system can realize heat recovery of waste heat resources at 70~450°C. when the heat source temperature is 450°C, the thermal efficiency can reach 27.9% [8]. when the heat source temperature is 70°C, but the thermal efficiency is only about 8% [9], the effect is not satisfactory, the cost of investment and maintenance is relatively high in the current technical conditions.

The Kalina cycle is a power cycle with ammonia water mixture as the working medium, it has higher requirements for working medium and exists pollution to the environment [10]. In order to achieve the purpose of low temperature solar energy utilization, a thermally driven electrochemical power generation device (TDEG) is applied in this paper combining a reverse electro dialysis device and a thermal separator, using ammonium bicarbonate solution as working solution, and obtaining a concentrated solution and dilute solution for reverse electro dialysis power generation through a thermal separator solution. The heat source temperature that can be used in this method is about 60°C, and the conversion efficiency is about 31% [11]. For the utilization of low-temperature heat, there is no ideal method of utilization currently.

Reverse Electro dialysis (RED) power generation technology was originally proposed by Pattle, R. E. in “Nature” magazine in 1954 [12]. The research on RED mainly uses the chemical potential difference energy between seawater and freshwater or seawater with different salt concentrations [13]. With seawater and river water as Medium, RED theoretical membrane voltage is about 80 mV [14]. Thermal Power Generation based on Reverse Electro dialysis (TPG-RED) uses a specific electrolyte solution as a medium to convert thermal energy into electrical energy, which has different application value from traditional RED. The author invented a “TPG-RED” [15] based on the theory of RED power generation technology. This paper will study TPG-RED to explore novel methods for direct solar thermal power generation.

## 2 The Design of Thermal Power Generation Based on Reverse Electro dialysis (TPG-RED)

TPG-RED is an innovation based on traditional Reverse Electro dialysis (RED). The basic principle of the traditional RED device is shown in the figure. The device is mainly composed of alternating and parallel installation of anion exchange membrane (AEM), membrane spacers, cation exchange membrane (CEM), cathode and positive plate, as well as pumps, pipelines and various material and liquid storage tanks and other supporting equipment. Seawater and river water are alternately passed between two adjacent membranes to form concentrated saltwater chamber and fresh water chamber arranged in turn. In the influence of concentration difference, The anion and cation in seawater are transmitted through the adjacent anion-cation exchange membrane to the river side to produce electric potential difference. The power generation system is shown in the Fig. 1.



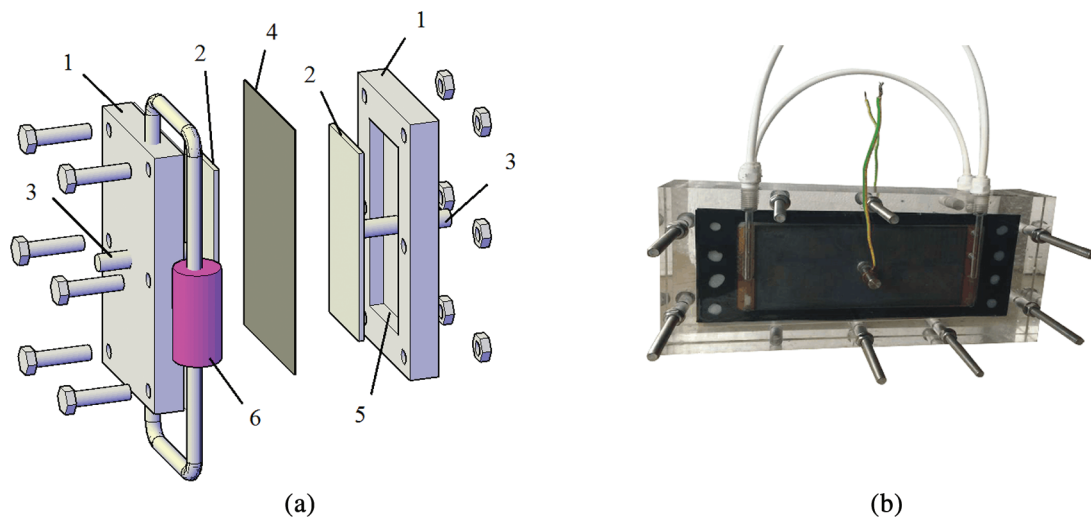
**Figure 1:** Schematic diagram of traditional RED power generation system

TPG-RED replaces the traditional multi-group membrane stack with a single-layer ion selective membrane between each pair of electrodes. Specific working electrolyte solution is used according to the demands of characteristics of the working electrolyte solution. In the selected working electrolyte concentrated solution, the discharge sequence of anions in water are after  $\text{OH}^-$  or the same as  $\text{OH}^-$ , such as  $\text{SO}_4^{2-}$ ,  $\text{F}^-$ ,  $\text{NO}_3^-$ ,  $\text{OH}^-$  and so on, and the discharge sequence of cations are after  $\text{H}^+$  or the same as  $\text{H}^+$ , such as  $\text{Li}^+$ ,  $\text{Na}^+$ ,  $\text{K}^+$ ,  $\text{H}^+$  and so on. The same inert electrode is used for the cathode and anode [16].

### 3 Experimental Device and Process of Thermal Power Generation Based on Reverse Electrodialysis (TPG-RED)

#### 3.1 Experimental Device

Based on design ideas of Thermal Power Generation based on Reverse Electrodialysis (TPG-RED), TPG-RED experimental device is developed [17]. The experimental device is shown in Fig. 2.



**Figure 2:** Experimental device. (a) Schematic diagram of the experimental device: 1—clamping device, 2—Inert electrode, 3—electrode extraction, 4—ion exchange membrane, 5—electrode chamber, 6—heat exchanger. (b) Real products picture of experimental device

The clamping device of CT-100 electro dialysis equipment is adopted in the experimental device, Both the anode and cathode electrodes are adopted with ruthenium coated titanium insoluble electrode. Only one ion exchange membrane is installed between the two electrodes, the ion exchange membrane adopts Hangzhou green environmental protection HoCEMGrion 0011 proton exchange membrane.

#### 3.2 Experimental Process

TPG-RED can be divided into four types depending on the type of electrolyte solution: cationic acid solution, cationic salt solution, anionic alkali solution, anionic salt solution [15]. Among them, in the type of cationic acid solution, different concentrations of acid solution is adopted in the working electrolyte solution, the ion permselective membranes is cation exchange membrane. In the type of cationic salt solution, different concentrations of salt solution is adopted in the working electrolyte solution, the ion permselective membranes is cation exchange membrane. In the type of anionic alkali solution, different concentrations of alkali solution is adopted in the working electrolyte solution, the ion permselective membranes is anion exchange membrane. In the type of anionic salt solution, different concentrations of salt solution is adopted in the working electrolyte solution, the ion permselective membranes is anion

exchange membrane. Experiment of the type of cationic acid solution and the type of cationic salt solution are studied in this paper.

TPG-RED experiment: “Concentrated solution—dilute solution” using “1 mol/L H<sub>2</sub>SO<sub>4</sub> solution—0.0001 mol/L H<sub>2</sub>SO<sub>4</sub> solution” and “1 mol/L Na<sub>2</sub>SO<sub>4</sub> solution—0.0001 mol/L Na<sub>2</sub>SO<sub>4</sub> solution” respectively, making two open circuit electrode in the 30°C heat source temperature, the system converts its own thermal energy into potential energy. After 400 min, a 100 Ω load is connected between the two electrodes, and the the electric power output process is conducted.

“Effect of heat source temperature on output current” experiment: “0.5 mol/L H<sub>2</sub>SO<sub>4</sub> solution—0.0001 mol/L H<sub>2</sub>SO<sub>4</sub> solution” and “0.5 mol/L Na<sub>2</sub>SO<sub>4</sub> solution—0.0001 mol/L Na<sub>2</sub>SO<sub>4</sub> solution” are adopted, a 100 Ω load is connected between the two electrodes. After the current has stabilized, place the device in an electronic incubator to simulate the heat solar source, and different solar radiation temperatures are simulated by setting the thermostat temperature.

“Effect of concentration difference on output current” experiment: 0.0001 mol/L H<sub>2</sub>SO<sub>4</sub> solution is adopted for dilute solution, 0.5, 1, 1.5, 2, and 2.5 mol/L H<sub>2</sub>SO<sub>4</sub> solution are adopted for concentrated solution, change the concentration difference through the concentration variation of the H<sub>2</sub>SO<sub>4</sub> solution, a 100 Ω load is connected between the poles at 30°C, the current is basically stable after 120 min, record the current after stabilization and the concentration of the corresponding H<sub>2</sub>SO<sub>4</sub> solution.

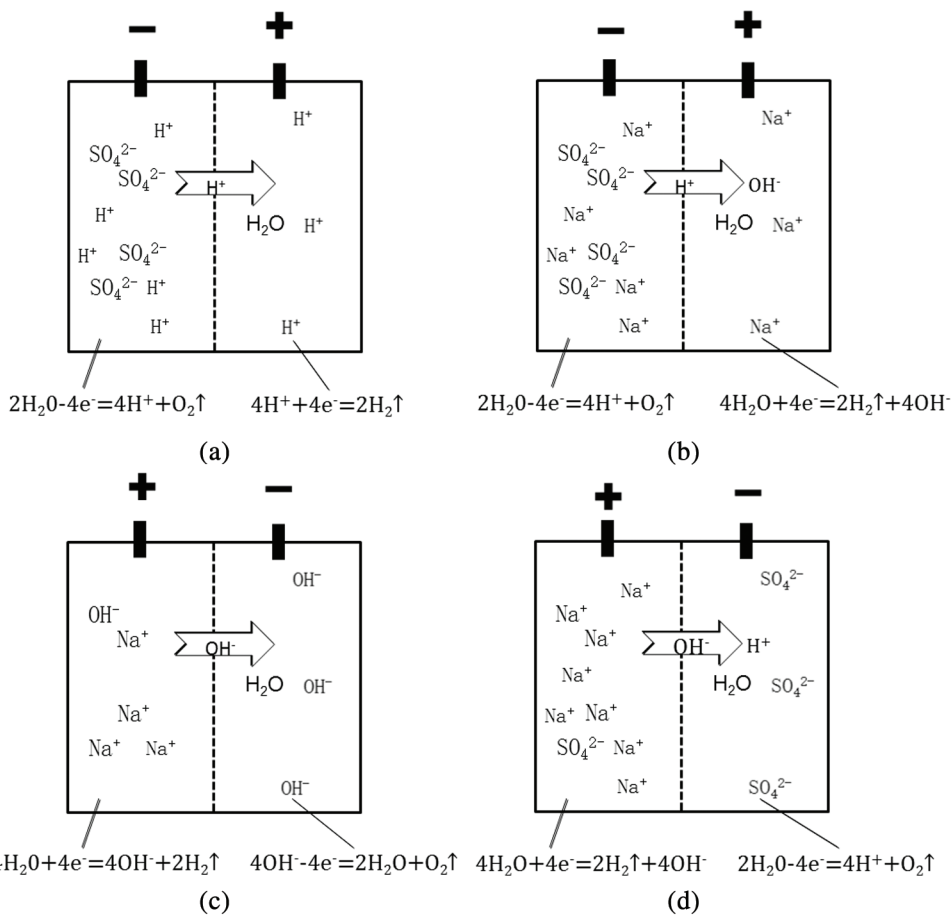
### 3.3 Principle of Power Generation

The TPG-RED power generation principle of cationic sulfuric acid solution type is as shown in Fig. 3a, electrolyzer is divided into compartments by cation exchange membrane (dotted line), high concentration sulfuric acid solution and low concentration sulfuric acid solution are injected separately, both compartments are inserted into the same inert electrode. H<sup>+</sup> diffuses from the high concentration solution into the low concentration solution through the cation membrane, to make negative electricity in high concentration side, positive electrification in low concentration side, and potential difference is produced on both sides of the membrane. After the two electrodes are connected, the water molecules in the high concentration solution lose electronics ( $2\text{H}_2\text{O} - 4\text{e}^- = \text{O}_2\uparrow + 4\text{H}^+$ ), H<sup>+</sup> in low concentration solution gets electronics ( $2\text{H}^+ + 2\text{e}^- = \text{H}_2\uparrow$ ) [17]. The H<sup>+</sup> generated in the high concentration side diffuses again into the low concentration side to discharge. Circulated like this, the concentration difference on both sides of the membrane can be automatically maintained. When the water consumes a certain amount, the supplemental water can run continuously. Due to the diffusion of H<sup>+</sup>, an electric field  $E$  is formed on both sides of the exchange membranes which is opposite to the diffusion direction. H<sup>+</sup> is affected by the electric field force opposite to the direction of diffusion, resulting the H<sup>+</sup> average translational kinetic energy is reduced and the system temperature is lowered, so the system converts thermal energy into electrical energy. Other types of power generation principles are shown in Figs. 3b–3d [15].

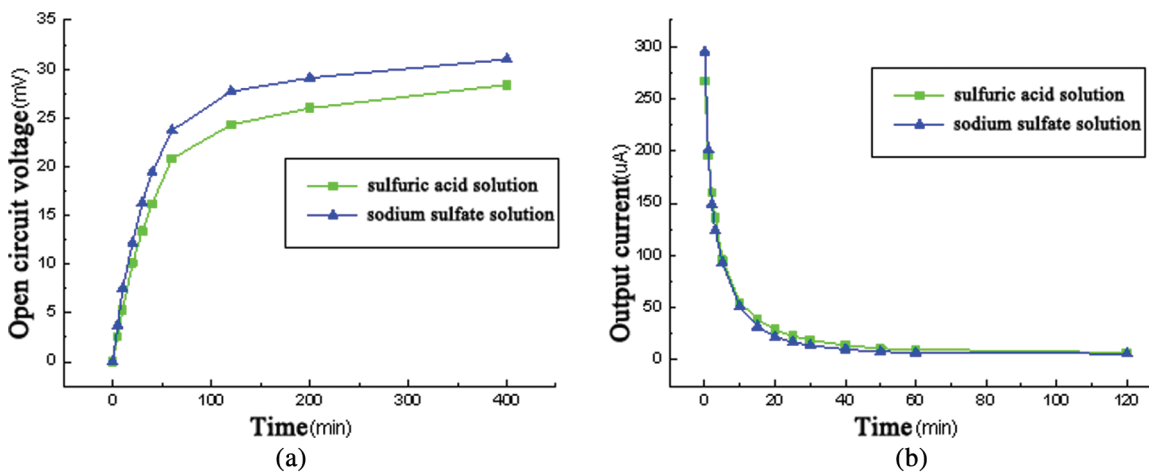
## 4 Results and Analysis

### 4.1 Thermal Power Generation Based on Reverse Electrodialysis (TPG-RED) Experiment

The open circuit voltage of TPG-RED experiment changes with time is as shown in Fig. 4a. After 400 min, the open circuit voltage of “1 mol/L H<sub>2</sub>SO<sub>4</sub> solution—0.0001 mol/L H<sub>2</sub>SO<sub>4</sub> solution” and “1 mol/L Na<sub>2</sub>SO<sub>4</sub> solution—0.0001 mol/L Na<sub>2</sub>SO<sub>4</sub> solution” was gradually increased from 0 to 28.4 mV and 0 to 31.0 mV, as shown in Tab. 1a. The theoretical value of the electric potential difference in TPG-RED can be calculated by the Nernst equation [18]:



**Figure 3:** Schematic diagram of TPG-RED. (a) Schematic diagram of cationic acid solution type. (b) Schematic diagram of cationic salt solution type. (c) Schematic diagram of anion alkali solution type. (d) Schematic diagram of anion salt solution type



**Figure 4:** Curve of TPG-RED generating (a) Curve of open circuit voltage vs. time. (b) Curve of output current vs. time

**Table 1:** Table of TPG-RED generating

(a) Table of open circuit voltage over time														
Solution Time (min)	0	10	20	30	40	50	60	100	200	400				
Open circuit voltage (mv) (sulfuric acid solution)	0	2.5	5	10	13	16	20	24	25	28.4				
Open circuit voltage (mv) (sodium sulfate solution)	0	3	7.5	12	16	19	23	27.5	29	31				
(b) Table of output current vs. time														
Solution Time (min)	0	2	4	6	8	10	15	20	25	30	40	50	60	120
Output current ( $\mu$ A) (sulfuric acid solution)	267	195	158	134	92	53	30	27	25	23	17	15	13	7
Output current ( $\mu$ A) (sodium sulfate solution)	295	200	150	125	90	52	27	25	24	20	15	13	11	5

$$E = \alpha \frac{RT}{zF} \ln \left( \frac{\gamma_s C_s}{\gamma_d C_d} \right) \quad (1)$$

where E is the transmembrane voltage, V; R—the gas constant, the value is  $8.314 \text{ J mol}^{-1} \text{ K}^{-1}$ , T—the Kelvin temperature,  $\alpha$ —the selective permeability of ion-exchange membranes, Subscripts *s*, *d* represent concentrated solution and dilute solution respectively,  $\gamma$  is the activity coefficient of the solution and is expressed by the following formula [19]:

$$\log \gamma = \frac{-Az^2 \sqrt{\mu}}{1 + (a\sqrt{\mu}/B)} \quad (2)$$

where  $\alpha$  is the effective radius of the ion, pm;  $\mu$ —the ionic strength of the solution, mol/L; A, B are temperature-related dimensionless coefficient, the value in  $25^\circ\text{C}$  are 0.509 and 328 respectively. The open circuit voltage gradually increases with time and does not rise directly to the theoretical calculation value, because the open circuit voltage is proportional to the amount of ions diffused from the concentrated solution into the dilute solution, and the amount of diffused ions gradually increases with time; meanwhile, the increase of the open circuit voltage indicates that potential energy is generated during the diffusion process of ions.

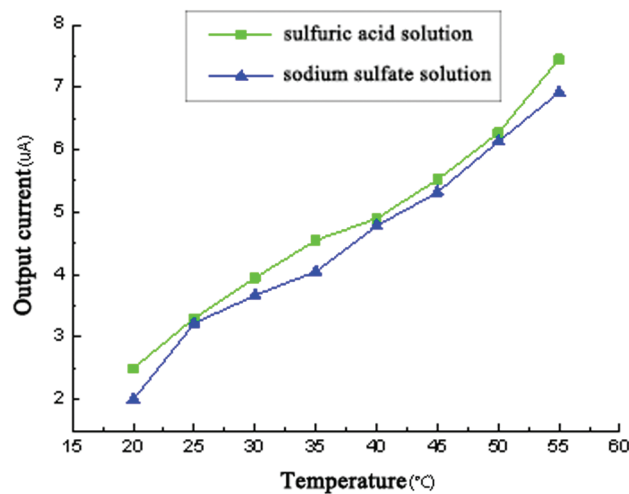
The output current of TPG-RED experiment changes with time as shown in Fig. 4b. The initial output currents of “1 mol/L  $\text{H}_2\text{SO}_4$  solution—0.0001 mol/L  $\text{H}_2\text{SO}_4$  solution” and “1 mol/L  $\text{Na}_2\text{SO}_4$  solution—0.0001 mol/L  $\text{Na}_2\text{SO}_4$  solution” are 267 and 295  $\mu\text{A}$  respectively. After 120 min of discharge, the output current is basically stable, 7 and 5  $\mu\text{A}$  respectively, as shown in Tab. 1b. The current in the first 10 min is large and the rate of decrease is faster. Because the ion diffusion stores more net charge in the two compartments, these net charges move rapidly in the electric field generated by itself, and converting the potential energy into electrical energy. At this time, the diffusion motion in ions remain to store the net charge, but the net charge stored in diffusion per unit time is less than the net charge consumed by the power release, Therefore, the amount of net charge decreases gradually, resulting in a decrease in voltage and output current. Finally, the net charge stored when diffused per unit time is equal to the net charge consumed by power generation, the output current tends to be stable.

#### 4.2 Experiment of the Effect of Heat Source Temperature on Output Current

This experiment explores the effect of heat source temperature on the stable output current. The experimental result is shown in Tab. 2. As shown in Fig. 5, the output current increases with the temperature of the heat source rises, because the rising temperature causes the diffusion rate to increase, resulting in an increase in the output current. At the same time, the power generation system can generate electricity from 20°C to 55°C, so the operating temperature is lower than the general thermal power generation system. The result shows a better low-temperature heat source adaptability in this power generation system.

**Table 2:** Table of output current vs. temperature

Solution Temperature (°C)	20	25	30	35	40	45	50	55
Output current (μA) (sulfuric acid solution)	2.5	3.3	4	4.5	4.9	5.4	6.2	7.4
Output current (μA) (sodium sulfate solution)	2	3.2	3.6	3.9	4.8	5.3	6	6.9



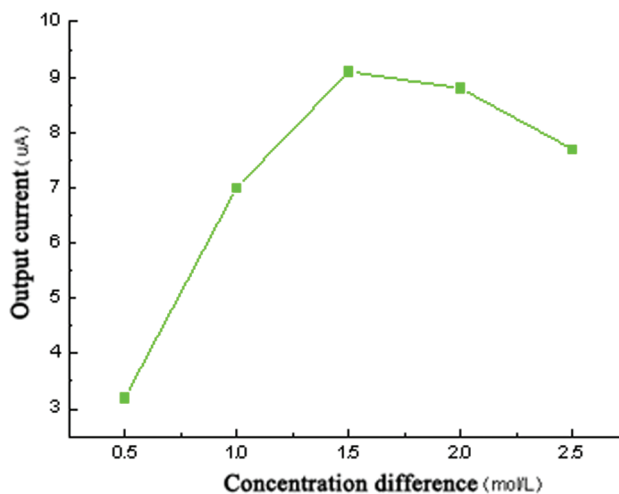
**Figure 5:** Curve of output current vs. temperature

#### 4.3 Experiment of Effect of Concentration Difference on Output Current

The purpose of this experiment is to explore the effect of concentration difference on the stable output current. The experimental result is shown in Tab. 3, and the curve is drawn in Fig. 6. When the concentration difference (sulfuric acid concentration) is less than 1.5 mol/L, the output current increases as the concentration difference increases. When the concentration difference is more than 1.5 mol/L, the output current decreases. Theoretically, the greater the concentration difference, the faster the ion diffusion rate, and the larger the output current. However, excessive solution concentration causes damage to the ion exchange membrane, but instead reduces the output current. Therefore, the property of the power generation system can be improved by increasing the concentration difference, But there is a certain limit, the limit mainly depends on the performance of the ion exchange membrane resistance to solution concentration.

**Table 3:** Table of output current vs. concentration

Concentration difference	0.5	1.0	1.5	2.0	2.5
Output current	3.2	7	9.1	8.8	7.7

**Figure 6:** Curve of output current vs. concentration

## 5 Application and Discussion

Thermal Power Generation based on Reverse Electrodialysis (TPG-RED) realizes thermal power generation, especially in the case of heat sources at normal temperature to 55°C. Explored a new idea of low-temperature thermal energy generation such as low-grade industrial waste heat, geothermal energy, solar heat, and environmental heat. The further development of this technology is expected to solve the technical problem that it is difficult for traditional thermal power generation systems such as solar energy to effectively utilize low-temperature heat sources to generate electricity. The working fluid of this method can be recycled, and only to be heated to increase the internal energy of the working fluid, then the power generation system can directly convert the internal energy of the solution into electrical energy. The system possesses the characteristics of simple structure, low investment and maintenance cost, high safety and reliability, and no pollutants in the working process.

As mentioned above, the output current of TPG-RED increases as the temperature and concentration difference increase; Other studies have shown that the output power and power density of the system depend on the performance of the ion exchange membrane to a great extent [20]. The latest research shows that a nano-porous semipermeable membrane with a thickness of only 0.65 nm is used for reverse electrodialysis power generation and its power density can reach to 1 MW/m<sup>2</sup>, which is 2000 times the power density of solar power generation, 106 times that of most ion exchange membranes on the market currently [21]. Therefore, if this semi-permeable membrane can be promoted, it will make great engineering practical potential to the TPG-RED system.

**Funding Statement:** The author(s) received no specific funding for this study.

**Conflicts of Interest:** The authors declare that they have no conflicts of interest to report regarding the present study.



## References

1. Lizana, J., Bordin, C., Rajabloo, T. (2020). Integration of solar latent heat storage towards optimal small-scale combined heat and power generation by Organic Rankine Cycle. *Journal of Energy Storage*, 29, 101367.
2. Aggarwal, J., Aggarwal, M. L. (2014). Harnessing solar energy for every home: energy saving applications. *Conference Papers in Science, 2014*, 1–3.
3. Liu, Z., Peng, W., Shih, K., Wang, J., Wang, Z. et al. (2016). A MoS<sub>2</sub> coating strategy to improve the comprehensive electrochemical performance of LiVPO<sub>4</sub>F. *Journal of Power Sources*, 315, 294–301. DOI 10.1016/j.jpowsour.2016.02.083.
4. Li, X., Wang, Z., Yang, M., Yuan, G. (2020). Dynamic simulation of a novel solar polygeneration system for heat, power and fresh water production based on solar thermal power tower plant. *Journal of Thermal Science*, 29(2), 378–392. DOI 10.1007/s11630-020-1163-z.
5. Shemelin, V., Matuska, T. (2019). Performance modelling of dual air/water collector in solar water and space heating application. *International Journal of Photoenergy*, 2019(1), 1–10. DOI 10.1155/2019/8560193.
6. Khandelwal, N., Sharma, M., Singh, O., Shukla, A. K. (2020). Recent developments in integrated solar combined cycle power plants. *Journal of Thermal Science*, 29(2), 298–322. DOI 10.1007/s11630-020-1278-2.
7. Zhang, H., Lei, B., Yu, T., Zhao, Z. (2019). Form and operation mode analysis of a novel solar-driven cogeneration system with various collector types. *International Journal of Photoenergy*, 2019, 1–12. DOI 10.1155/2019/5329086.
8. Zhang, L. H., Wu, L. J., Hu, H. R., Gao, X. J. (2013). Comparison and optimization of low temperature flue gas power generation systems in iron and steel enterprises. *Journal of Engineering for Thermal Energy & Power*, 28(3), 257–261.
9. Yi, S. Y., Guo, M. R., Zhu, Q. D., Sun, Z. Q. (2015). Analysis of the performance of recuperative organic rankine cycles utilizing a medium and low temperature waste heat. *Journal of Engineering for Thermal Energy & Power*, 30(1), 24–30, 159–160.
10. Chen, H., Goswami, D. Y., Stefanakos, E. K. (2010). A review of thermodynamic cycles and working fluids for the conversion of low-grade heat. *Renewable and Sustainable Energy Reviews*, 14(9), 3059–3067. DOI 10.1016/j.rser.2010.07.006.
11. Luo, X., Cao, X. X., Mo, Y. H., Xiao, K., Zhang, X. Y. et al. (2012). Power generation by coupling reverse electrodialysis and ammonium bicarbonate: implication for recovery of waste heat. *Electrochemistry Communications*, 19(1), 25–28. DOI 10.1016/j.elecom.2012.03.004.
12. Pattle, R. E. (1954). Production of electric power by mixing fresh and salt water in the hydroelectric pile. *Nature*, 174(4431), 660. DOI 10.1038/174660a0.
13. Post, J. W., Veerman, J., Hamelers, H. V. M., Euverink, G. J. W., Metz, S. J. et al. (2007). Salinity-gradient power: evaluation of pressure-retarded osmosis and reverse electrodialysis. *Journal of Membrane Science*, 288(1–2), 218–230. DOI 10.1016/j.memsci.2006.11.018.
14. Yan, X. W. (1999). Saline difference power generation. *Solar Energy*, 2(1), 6–7.
15. He, J. J., Yin, Y. F., Chen, J. (2017). *The method and device of thermal power generation based on reverse electrodialysis*. China Patent 2017103335499[P].2017-07-28.
16. Perzez, N. (2013). *Electrochemistry and corrosion science*. Beijing: Chemical Industry Press.
17. Yin, Y. F., He, J. J., Chen, J. (2017). *The device of thermal power generation based on reverse electrodialysis*. China Patent 201720526592X[P].2017-07-28.
18. Hui, H. N., Tian, M., Yang, X. L., He, Y. F. (2015). Structure optimization and energy analysis of reverse electrodialysis to recover energy of oceanic salinity gradient. *CIESC Journal*, 66(05), 1919–1924.
19. Hong, J. G., Zhang, W., Luo, J., Chen, Y. (2013). Modeling of power generation from the mixing of simulated saline and freshwater with a reverse electrodialysis system: the effect of monovalent and multivalent ions. *Applied Energy*, 110(1), 244–251. DOI 10.1016/j.apenergy.2013.04.015.
20. Deng, H. N., He, H. F., Hu, B. S., Feng, M. (2017). Progress in ion exchange membranes for reverse electrodialysis. *Chemical Industry and Engineering Progress*, 36(01), 224–231.
21. Feng, J., Graf, M., Liu, K., Ovchinnikov, D., Dumcenco, D. et al. (2016). Single-layer MoS<sub>2</sub> nanopores as nanopower generators. *Nature*, 536(7615), 197–200. DOI 10.1038/nature18593.