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Analysis of Heat Transport in a Powell-Eyring Fluid with Radiation and Joule Heating Effects via a Similarity Transformation

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ABSTRACT

Heat transfer in an Eyring-Powell fluid that conducts electricity and flows past an exponentially growing sheet is considered. As the sheet is stretched in the x direction, the flow develops in the region with $y > 0$. The problem is tackled through a set of partial differential equations accounting for Magnetohydrodynamics (MHD), radiation and Joule heating effects, which are converted into a set of equivalent ordinary differential equations through a similarity transformation. The converted problem is solved in MATLAB in the framework a fourth order accurate integration scheme. It is found that the thermal relaxation period is inversely proportional to the thickness of the thermal boundary layer, whereas the Eckert-number displays the opposite trend. As this characteristic number grows, the temperature within the channel increases.

KEYWORDS

Stretched flow; powell-eyring model; heat flux model; radiated effect; relaxation phenomenon; numerical study

Nomenclature

u, v, w	Velocity components, m/s
λ	Ratio of expansion rates
U_w	Stretching velocity, m/s
K, Γ	Dimensionless Powell Eyring fluid parameters
U_∞	Velocity of external flow, m/s
Pr	Prandtl number
L	Characteristic length, m
C_f	Skin friction coefficient
T_w	Surface temperature, K
Nu	Local Nusselt number
T_∞	Ambient temperature, K
τ_w	Wall shear stress
τ	Stress tensor, $\frac{N}{m^2}$
q_w	Surface heat flux



ν	Kinematic viscosity, $\frac{m^2}{s}$
Re, Re_x	Local Reynolds numbers
μ	Dynamic viscosity, $Kg/m.s$
B	Magnitude of magnetic field vector, $Kg/s^2.A$
ρ	Density of the fluid, Kg/m^3
q_{rad}	Radiative heat flux
β	Powell-Eyring material parameter, Pa^{-1}
K^*	Mean absorption coefficient, m^{-1}
C	Powell-Eyring material parameter, s^{-1}
σ^*	Stefan Boltzmann constant, $\frac{W}{m^2}.K^4$
C_p	Specific heat, $J/Kg.K$
γ^*	Dimensionless thermal relaxation time
T	Temperature of the fluid, K
δ_t	Thermal relaxation time
k	Thermal conductivity of the fluid, $W/m.K$
Ec	Eckert number
Rd	Radiation parameter
M	Magnetic parameter

1 Introduction

Eyring-Powell fluids are a significant type of non-Newtonian fluid. Additionally, these fluids are classified as differential types, integral models, and shear rate models. The Eyring-Powell fluid has a particular advantage over the power-law model because it is based on liquid kinetic theory. For low and high shear rates, this fluid's Newtonian behaviour decreases. These fluids are extremely valuable since they can be used in a variety of engineering, manufacturing, and industrial applications, including pulp, plasma, and other biological technology. Additionally, these fluids play a critical role in fermentation, boiling, bubble formation, column processing, and the processing of plastic foam, with substances such as mud, colours, toothpaste, blood, corn starch, custard, and honey serving as insignificant examples of non-Newtonian fluids [1].

Recent technological and engineering advancements have resulted in the development of a diverse range of non-Newtonian fluids with a number of major differences from viscous fluids. Ziegenhagen [2] explored the slow flow of a Powell-Eyring type fluid and used variational techniques to obtain results. He studied the behaviour of Oldroyd and Powell Eyring fluids and discovered that both fluids behave identically in situations involving extremely slow fluid flow. Sirohi et al. [3] studied it by observing the flow of Powell-Eyring fluid around the accelerating plate. They compared three distinct techniques. Yoon et al. [4] pioneered the concept of a stretched sheet by providing a precise solution to the resulting differential system. Recent academics have investigated this topic from a variety of perspectives [5–13]. Bahia et al. [14] investigated the Powell-Eyring fluid flow and heat transport past a stretched sheet exponentially. They discovered that increasing the velocity ratio parameter results in a thinned boundary layer. Malik et al. [15] examined the Powell-Eyring fluid flow and heat transport with varying viscosity over a stretching cylinder by examining the steady condition. They concluded that as Prandtl and Reynolds numbers increase, the boundary layer shrinks. Akbar et al. [16] studied the effect of magnetic factors on Eyring-Powell fluid flow past a stretched surface. They investigated flow resistance as the magnetic and hydrodynamic properties of the fluid under study increased.

Kumar et al. [17] investigated the Powell-Eyring nanofluid passing via an inclined permeable sheet. They demonstrated that temperature increases as thermophoresis parameter values increase. While the contrary is true for nanoparticle concentration due to higher chemical reactions and Brownian parameters, increasing thermophoresis parameter values results in an increase in concentration. Pal et al. [18] demonstrated magneto-bioconvection of Powell-Eyring nanofluid via a vertical stretched sheet that is convectively heated and also contains motile gyrotactic microorganisms. They discovered that as the Schmidt number and chemical reaction parameters increase, the concentration of nanoparticles drops. Thermal relaxation time is the time required for a fluid to return to its original temperature after being heated. It is a frequently used parameter for determining the time required for heat to leave a fluid. Hayat et al. [19] investigated the effects of mass flux models on Eyring Powell fluid flow in three dimensions. They discovered that temperature and thermal-relaxation time have an inverse relationship. Reddy et al. [20] studied the effect of chemical reaction on the activation energy of Eyring Powell nanofluid flow via a stretching cylinder. They concluded that as the relaxation parameter increases, the temperature curves lose their shape. It takes a long time for an increase in the relaxation parameter assessment to transfer heat to neighbouring material particles. Additionally, the Nusselt number improves behaviour when non-dimensional thermal relaxation calculations are performed.

Mustafa [21] researched the Maxwell fluid with a generalised heat flux model for rotating flow and heat transfer. They also discovered that the thermal relaxation period is inversely proportional to temperature and thermal boundary thickness. On an unstable porous stretching sheet, Ishaq et al. [22] demonstrated the entropy production of Eyring Powell fluid flow with nanofluid thin film flow by considering the heat radiation and MHD impact. They discovered that when the Brinkmann, Hartmann, and Reynolds numbers grow, so does the entropy profile. For increasing values of the Eyring Powell and radiation parameters, the entropy profile reduces. The Eyring Powell nanofluid flow with non-linear mixed convection and entropy generation was explored by Alsaedi et al. [23]. They arrived at the conclusion that entropy generation showed a falling tendency for some fluid parameter values while increasing for others. Through a permeable stretching surface, Bhatti et al. [24] studied the irreversibility of MHD Eyring Powell nanofluid.

Ali et al. [25] used both perturbation and computational methods to examine the steady non-isothermal flow of an Eyring–Powell fluid in a conduit. The findings are provided for two viscosity models, the Reynolds and the Vogel models, which were solved using the shooting and perturbation methods, respectively. It was determined that the shooting approach outperformed the perturbation method. Nazeer et al. [26] investigated the effects of constant and space-dependent viscosity on a circular conduit filled with Eyring–Powell fluid. Additionally, heat transmission analysis is considered. The finite difference scheme is compared to the perturbation method. Numerous researchers discussed the Eyring–Powell model under a variety of scenarios and solved it analytically and numerically using a variety of numerical schemes such as the RK method, the shooting technique, and the perturbation method [27–34].

According to the existing literature, no attempt has been made to investigate the electrically conducting Eyring–Powell fluid with radiation, thermal relaxation time, and joule heating effects beyond an exponentially stretched sheet. This research fills a void in the literature and lays the groundwork for future researchers to contribute their perspectives to the open literature. This is structured as follows: [Section 1](#) contains the literature review, [Section 2](#) the mathematical formulation, [Section 3](#) the methodology, [Section 4](#) the results, and [Section 5](#) the conclusion.

2 The Problem's Formulation

Consider an incompressible Powell Eyring fluid flowing across an exponentially stretched surface subjected to magnetic, joule heating, thermal radiation, and thermal relaxation periods, as illustrated in [Fig. 1](#). The sheet is put on the x - and y -axes, respectively, and the flow is restricted to $y \geq 0$. Let

$U_w(x) = ae^{\frac{x}{l}}$ represent the sheet velocity, $U_\infty = be^{\frac{x}{l}}$ representing the external fluid velocity, and $T_w(x) = T_\infty + ce^{\frac{x}{2l}}$ representing the surface temperature, with T_∞ being the ambient temperature.

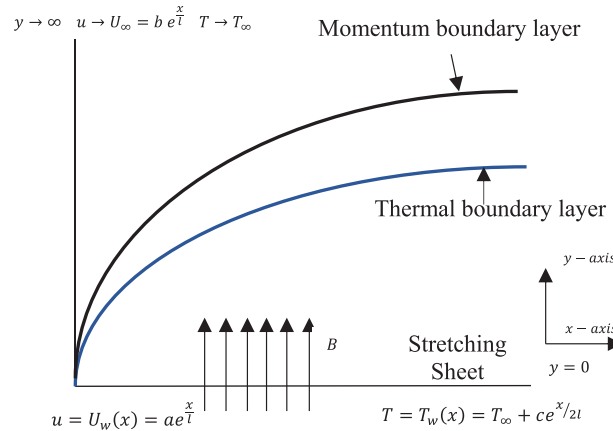


Figure 1: Configuration of the flow over a stretching sheet and geometrical coordinates

The governing equations so obtained are given as [35]

$$u \frac{\partial u}{\partial x} + v \frac{\partial v}{\partial y} = 0, \quad (1)$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = U_\infty \frac{dU_\infty}{dx} + \left(v + \frac{1}{\rho\beta C} \right) \frac{\partial^2 u}{\partial y^2} - \frac{1}{2\rho\beta C^3} \left(\frac{\partial u}{\partial y} \right)^2 \frac{\partial^2 u}{\partial y^2} - \frac{\sigma}{\rho} B_0^2 (U_\infty - u), \quad (2)$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \frac{k}{\rho C_p} (-\nabla \cdot \mathbf{q}) + \frac{\sigma B_0^2}{\rho C_p} (U_\infty - u)^2 - \frac{1}{\rho C_p} \frac{\partial q_{rad}}{\partial y}, \quad (3)$$

where ν , ρ , $u(x, y)$, $v(x, y)$, β , C , T , k , q_{rad} , C_p , B_0 , and \mathbf{q} are kinematic viscosity, fluid density, the velocities, fluid parameters, the temperature, the thermal-conductivity, thermal radiation, the specific-heat at constant pressure, the strength of magnetic field, and heat flux, respectively, which satisfy the relation [36]

$$q + \delta_t \left(\frac{\partial q}{\partial t} + V \cdot \nabla q - q \cdot \nabla V + (\nabla \cdot V) q \right).$$

Furthermore, by means of Rosseland approximation for radiation, we get $q_{rad} = -\frac{4\sigma^*}{3k^*} \frac{\partial T^4}{\partial y}$, k^* and σ^* as absorption coefficient and the Stefan Boltzmann constant. By expanding T^4 in a Taylor's series around T_∞ and neglecting higher order terms, we have the relation $T^4 = 4T_\infty^3 T - 3T_\infty^4$. The appropriate boundary conditions are

$$\left. \begin{aligned} u &= U_w(x) = ae^{\frac{x}{l}}, & v &= 0, \\ T &= T_w(x) = T_\infty + ce^{\frac{x}{2l}}, & \text{at } y &= 0, \\ u &\rightarrow U_\infty(x) = be^{\frac{x}{l}}, & T &\rightarrow T_\infty, & \text{as } y &\rightarrow \infty. \end{aligned} \right\}, \quad (4)$$

Taking the similarity transformations as

$$\eta = \sqrt{\frac{a}{2\nu L}} e^{x/2L} y, \quad u = ae^{\frac{x}{l}} f'(\eta), \quad v = -\sqrt{\frac{\nu a}{2L}} e^{\frac{x}{2L}} [f(\eta) + \eta f'(\eta)], \quad \theta(\eta) = \frac{T - T_\infty}{T_w - T_\infty}. \quad (5)$$

With the above transformation the continuity equation is satisfied identically and Eqs. (2)–(4) is converted into the following form:

$$(1 + K)f'''' + ff'' - 2f'^2 - K\Gamma f''^2 f'''' + 2\lambda^2 - M(\lambda - f') = 0, \quad (6)$$

$$(1 + Rd)\theta'' + Pr((f\theta' - \theta f') - \gamma(3f'^2\theta - \theta ff'' + f^2\theta'' - 3ff'\theta')) + MEc(\lambda - f')^2 = 0, \quad (7)$$

$$f(0) = 0, f'(0) = 1, \theta(0) = 1, f'(\infty) \rightarrow \lambda, \theta(\infty) \rightarrow 0,$$

where (8)

$$\lambda = \frac{b}{a}, K = \frac{1}{\mu\beta C}, \Gamma = \frac{U_w^3}{4\nu LC^2}, Pr = \frac{\mu C_p}{k}, M = \frac{\delta}{\rho} \left(\frac{2LB_0^2}{U_w} \right), Rd = \frac{16T_\infty^3 \sigma^*}{3k^* C_p \mu},$$

$$Ec = \frac{U_w^2}{C_p c e^{\frac{x}{2L}}}, \gamma = \delta_t \frac{ae^{\frac{x}{2L}}}{2L}. \quad (9)$$

Here λ and Pr denote velocity ratio and Prandtl-number respectively. Where, K and Γ are the dimensionless fluid parameters. Since Γ is a function of x , therefore, we use a local similarity solution of (6)–(8) that allows us to analyze parameter behaviour. For $K = 0$, we have the case of Newtonian fluid. The C_f and the local Nu are mathematically describe as

$$C_f = \frac{\tau_w}{\rho U_w^2}, Nu = \frac{xq_w(1 + Rd)}{k(T_w - T_\infty)}, \quad (10)$$

here, τ_w and q_w are mathematically describe as

$$\tau_w = \left(\mu + \frac{1}{\beta C} \right) \Big|_{y=0} - \frac{1}{6\beta C^3} \left(\frac{\partial u}{\partial y} \right)^3 \Big|_{y=0}, \quad q_w = -k \left(\frac{\partial T}{\partial y} \right) \Big|_{y=0}. \quad (11)$$

The mathematical form of local Nusselt number and skin friction coefficient are given as under

$$\sqrt{2Re} C_f = (1 + K)/f''(0) - \frac{K\Gamma}{3} (f''(0))^3, \quad \frac{\sqrt{\frac{2L}{x}} Nu}{Re_x^{\frac{1}{2}}} = -\theta'(0)(1 + Rd), \quad (12)$$

where local Reynolds numbers are $Re = \frac{U_w L}{\nu}$, and $Re_x = \frac{U_w x}{\nu}$.

3 Solution Methodology

Rahimi et al. [37] solved a non-Newtonian model known as the Powell Eyring fluid model using the collocation approach. Agrawal et al. [38] solved the Eyring Powell fluid model using a fourth-order precision methodology and the homotopy analysis method (H.A.M). Jafari Moghaddam [39] studied the Eyring Powell model and described fluid flow and heat transfer over a stretching sheet. The Eyring-Powell model is also solved by using different techniques as mentioned in [40–42]. He then solved the governing PDEs by using homotopy perturbation and homotopy analysis methods to convert them to ODEs. The flow chart of the numerical scheme is presented in Fig. 2 below. The third order nonlinear ordinary differential Eq. (6) and the second order nonlinear ordinary differential Eq. (7) are expressed as difference equations and solved using BVP4C and MATLAB in this article.

$$yy1 = \frac{1}{(1 + K - \Gamma Ky_3^2)} \left(M(\lambda - y_2) - y_1 y_3 + 2y_2^2 - 2\lambda^2 \right), \quad (13)$$

$$yy2 = \frac{1}{(1 + Rd - Pr\gamma y_1^2)} \left(\frac{Pr((y_2 y_4 - y_1 y_5) + \gamma(3y_2^2 y_4 - y_1 y_3 y_4 - 3y_1 y_2 y_5))}{-MEc(\lambda - y_2)^2} \right), \quad (14)$$

$$y_1(0) = 0, y_2(0) = 1, y_5(0) = 1, y_2(\infty) \rightarrow \lambda, y_5(\infty) \rightarrow 0, \quad (15)$$

The iterative approach will conclude with the required precision.

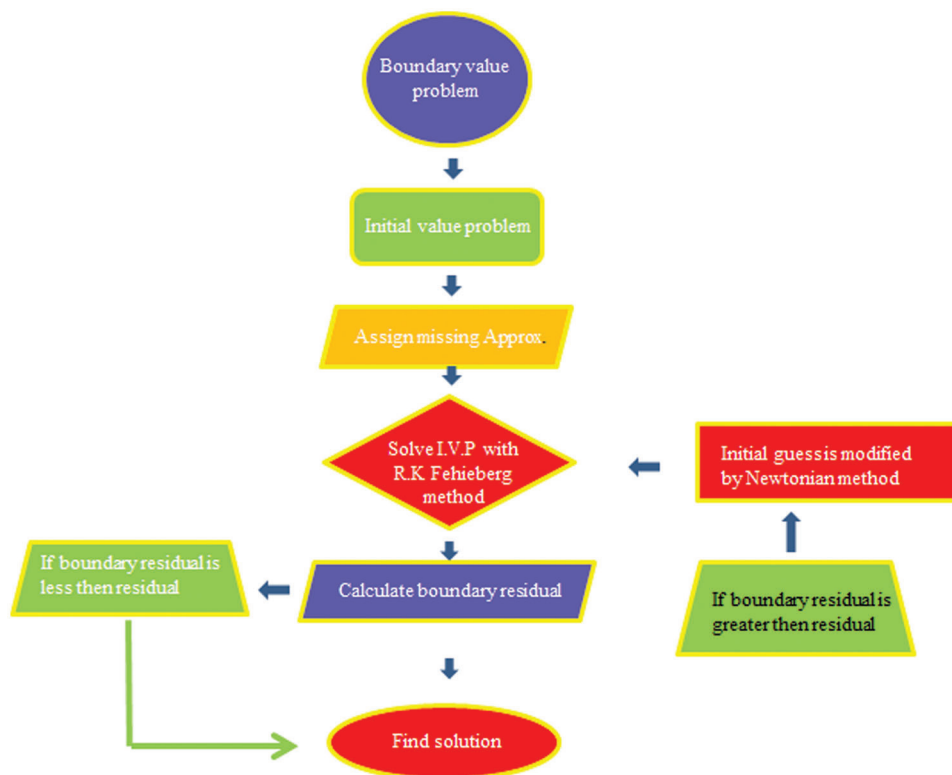


Figure 2: Flow chart related to numerical scheme

4 Result and Discussion

The velocity ratio parameter, the fluid parameter K , the magnetic parameter M , the non-dimensional fluid parameter, and the velocity profile are all monitored for variation. Additionally, this section discusses the influence of the Prandtl number Pr , the velocity ratio parameter, the fluid parameter K , the Eckert number Ec , the radiation parameter Rd , the thermal relaxation time T , and the magnetic parameter M on the dimensionless temperature $\theta(\eta)$. Tables and graphs of heat energy and velocity fields vs. physical parameters are included below.

4.1 Visualization of a Velocity Field

Two types of boundary layers near the sheet have evolved in a flow with exponentially changing free stream velocity over an exponentially stretched sheet. Which means that they are depending on the velocity ratio parameter b/a , for values of b/a greater than or equal to one. Additionally, it is worth to note that when $b/a = 1$, no velocity boundary layer arises near the sheet. The velocity profiles for various values of λ are depicted in Fig. 3. According to Fig. 4, increasing K results in a drop in fluid viscosity, which results in an increase in velocity. Additionally, as K increases, the viscosity of the fluid becomes lower due to the increase in the velocity of the fluid. The velocity profile declines as Γ grows, but changes toward the border, indicating that the boundary layer's thickness has decreased, which is depicted in Fig. 5. As the magnetic field intensity increases, the velocity profile in Fig. 6 drops. This is because an increase in the Lorentz force creates resistance to fluid flow, resulting in a drop in the velocity profile.

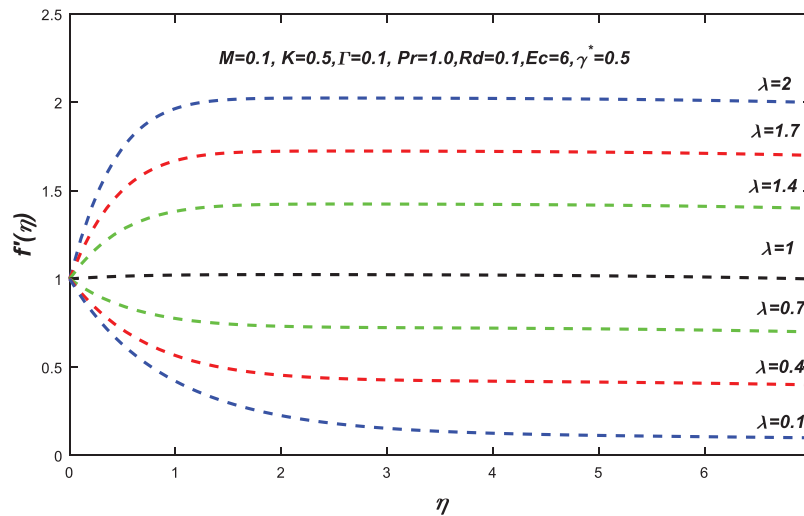


Figure 3: Change in the value of $f'(\eta)$ for different values of λ

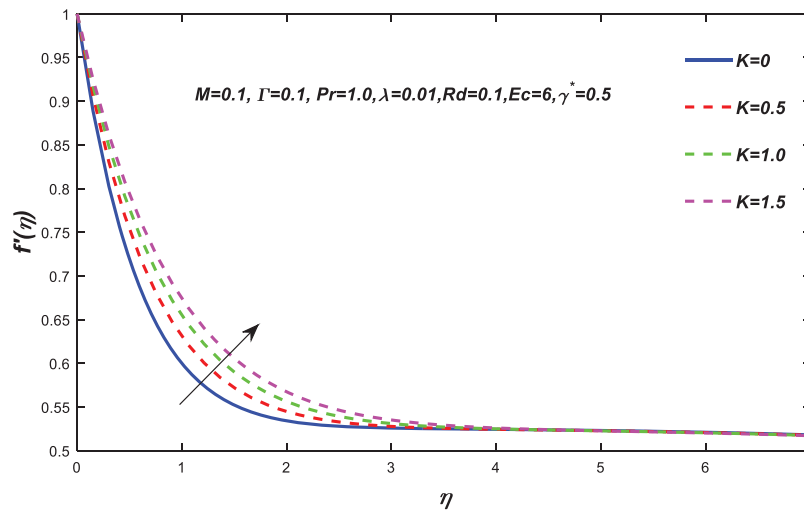


Figure 4: Change in the value of $f'(\eta)$ for different values of K

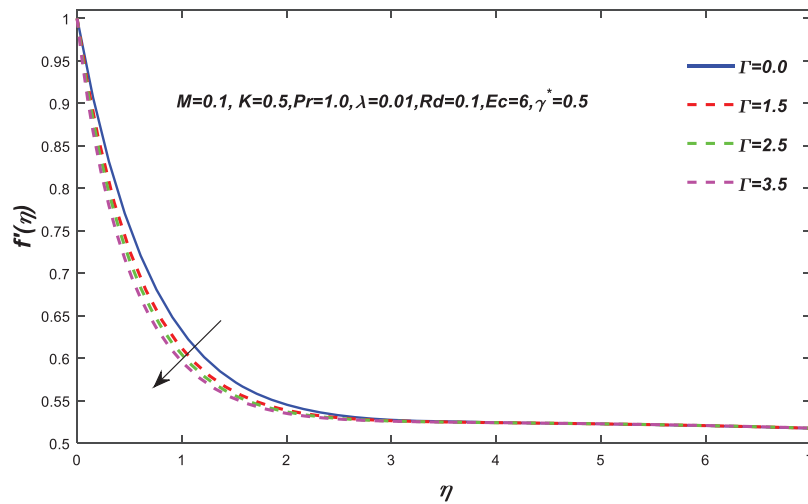


Figure 5: Change in the value of $f'(\eta)$ for different values of Γ

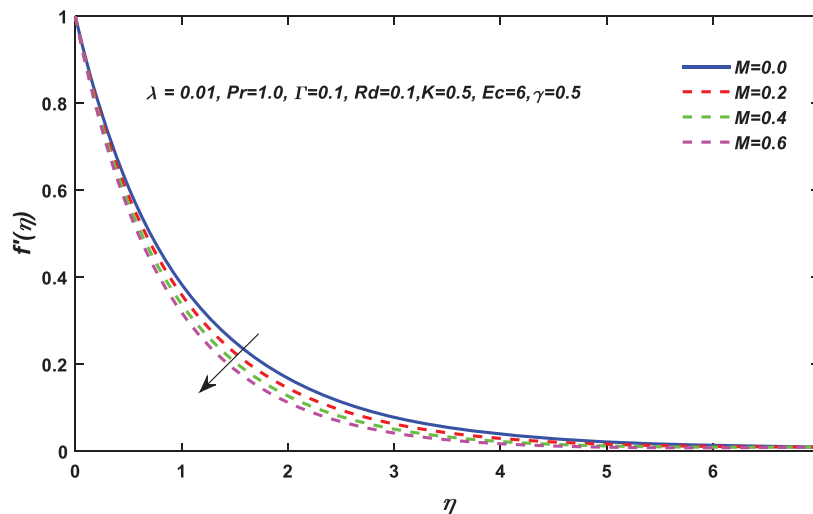


Figure 6: Change in the value of $f'(\eta)$ for different values of M

4.2 Visualization of a Temperature Field

The fluctuation of the velocity ratio parameter on the temperature profile is depicted in Fig. 7. Temperature has been discovered to be a decreasing function of λ . This data may imply that greater sheet velocity results in a thicker thermal boundary layer. As K increases, there is a slight reduction in temperature, as illustrated in Fig. 8. Due to the lack of viscous dissipation effects, the fluid parameter K is not explicitly included in the energy calculation and hence has a reduced effect on the thermal boundary layer. Fig. 9 illustrates the effect of Pr on temperature $\theta(\eta)$. The temperature profile falls as $Pr = \frac{\mu C_p}{k}$ increases. Additionally, rising values of Pr decrease the thickness of the thermal boundary layer. As a result, heat travels rapidly, leading to a decrease in fluid temperature.

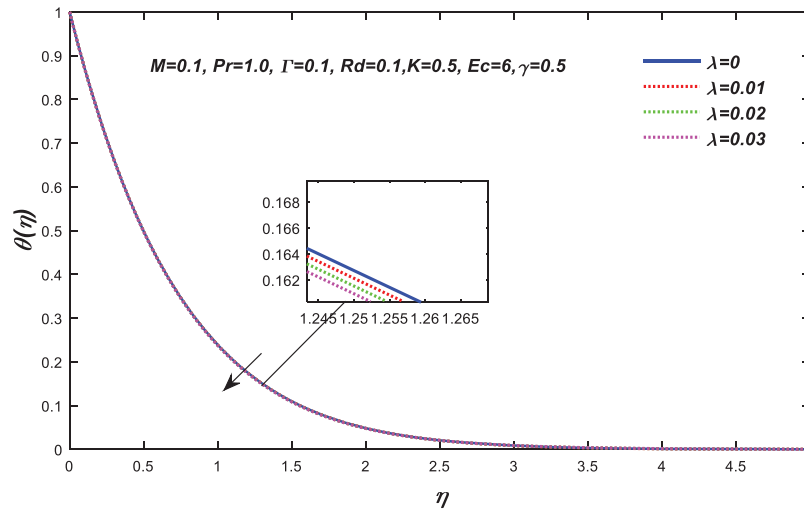


Figure 7: Change in the value of $\theta(\eta)$ for different values of λ

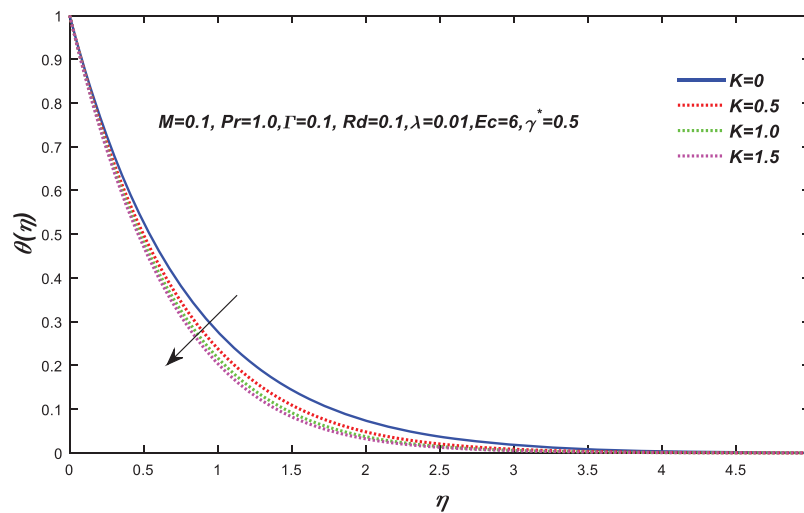


Figure 8: Change in the value of $\theta(\eta)$ for different values of K

The influence of radiation on temperature distributions can be seen in Fig. 10. Increases in Rd result in an increase in heat fluxes from the sheet, which results in a rise in temperature. Ec 's effect on the temperature profile $\theta(\eta)$ is depicted in Fig. 11. As the Ec value grows, the sheet's wall temperature increases. Due to the fact that when Ec is high, the rate of heat transfer at the surface is low, the thickness of the thermal boundary layer increases. Frictional heating happens at the surface, raising the fluid's temperature. The effect of thermal relaxation time γ on the temperature profile is illustrated in Fig. 12. Temperature and thermal relaxation time have been found to have an inverse connection. Physically, when we increase, the fluid elements have to work harder to transfer heat to their neighbouring components, resulting in a temperature drop. When $\gamma = 0$, heat rapidly spreads throughout the fluid. Fig. 13 illustrates the effects of the magnetic parameter M on the temperature profile.

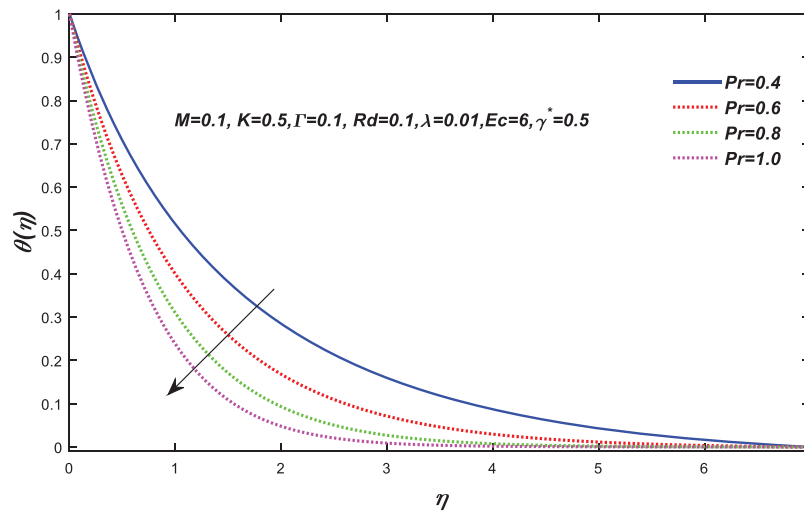


Figure 9: Change in the value of $\theta(\eta)$ for different values of Pr

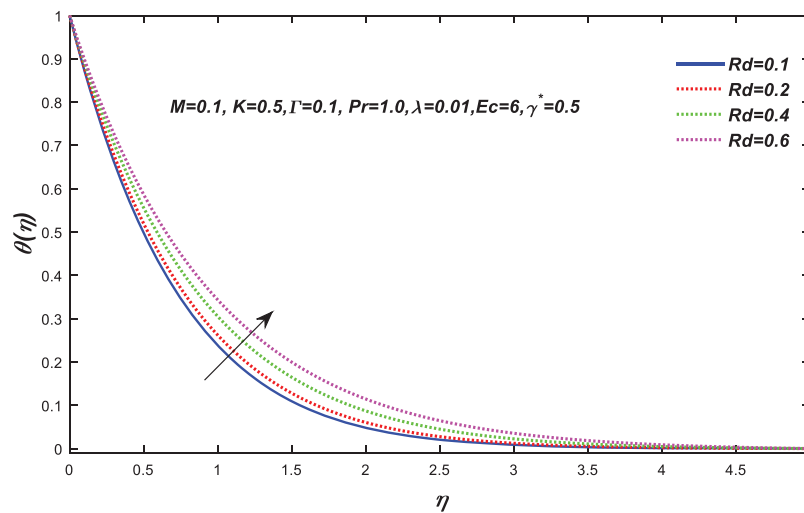


Figure 10: Change in the value of $\theta(\eta)$ for different values of Rd

4.3 Matching Results to Published Work

The local Nusselt number and skin friction are listed in Table 1, and were estimated using a MATLAB method with fourth-order precision (BVP4C). The skin friction coefficient increases as K increases. As a result, as Γ increases, the coefficient of friction on the skin lowers. According to Mushtaq et al. [13], on an exponentially stretched surface, the magnitude of the skin friction coefficient decreases significantly as the velocity ratio grows. It has already been noted that when K grows, the thermal boundary layer's thickness decreases. As a result, the heat transfer rate at the stretching sheet is increased. Additionally, as Γ grows, the size of the local Nusselt population decreases dramatically. Additionally, it increases as the values of K and λ increase.

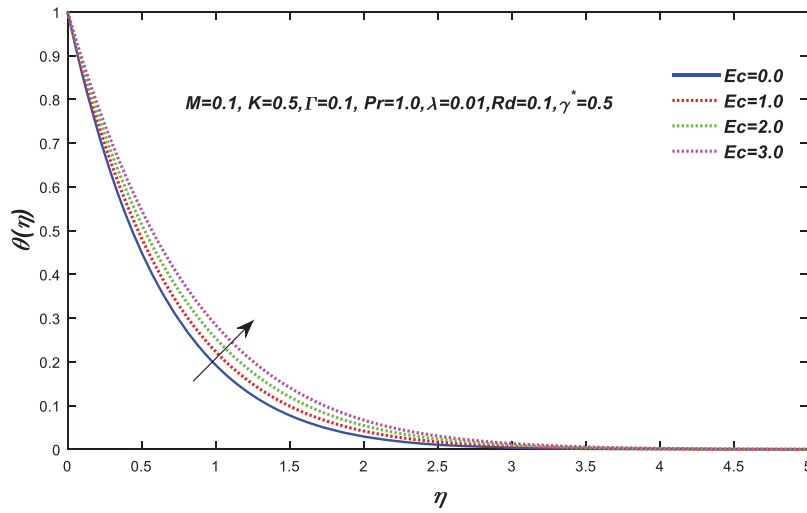


Figure 11: Change in the value of $\theta(\eta)$ for different values of Ec

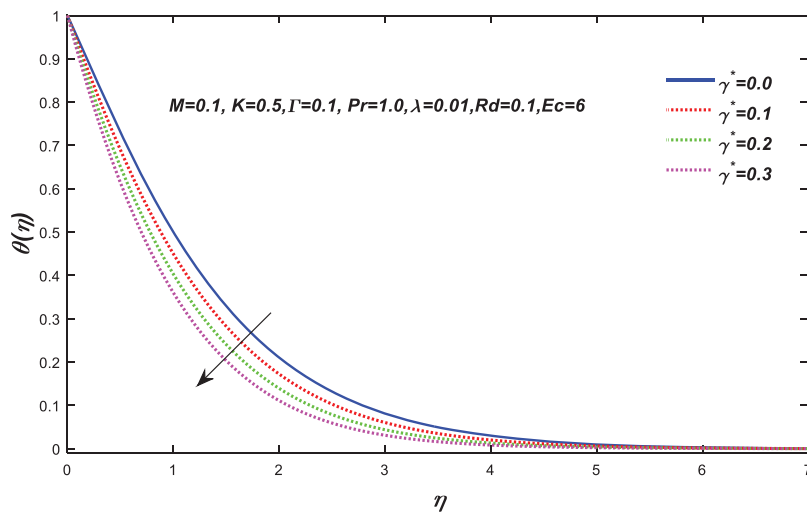


Figure 12: Change in the value of $\theta(\eta)$ for different values of γ

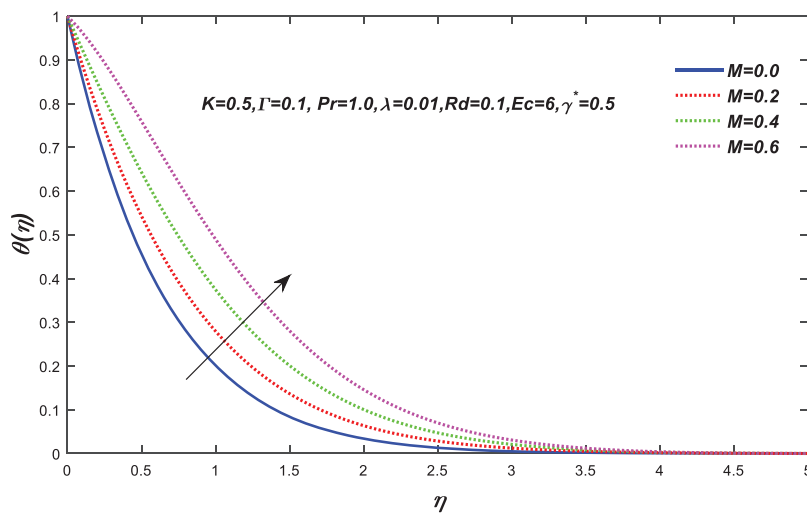


Figure 13: Change in the value of $\theta(\eta)$ for different values of M

Table 1: The local nusselt number and skin friction coefficient for different values of K and Γ , when $\lambda = 0.1$, $Rd = 0.2$ and $Pr = 1$

K	Γ	λ	$-f''(0)$			$-\theta'(0)$		
			HAM [35]	Numerical [35]	Present	HAM [35]	Numerical [35]	Present
0.0	0.1	0.1	1.253580	1.253590	1.25358	0.977953	0.977955	1.0474464
0.5			1.530419	1.530420	1.531183	1.022158	1.022158	1.0981546
1.0			1.766459	1.766456	1.7736449	1.050549	1.050549	1.1311701
1.5			1.975250	1.975260	1.9895533	1.070644	1.070644	1.1542023
0.5	0.0		1.535315	1.535315	1.5353431	1.023016	1.023016	1.0993117
	0.5		1.509342	1.509342	1.5089084	1.018406	1.018406	1.0933034
	1.0		1.478121	1.478140	1.4623461	1.012648	1.012648	1.0866498
	1.5		1.414220	1.413130	1.3774522	1.003943	1.003520	1.079163
	0.5	0.2	1.441522	1.441520	1.4504361	1.040756	1.040756	1.1202891
		0.3	1.343664	1.343664	1.3638739	1.066060	1.066060	1.1502404
		0.5	1.069109	1.069109	1.1092647	1.119838	1.119838	1.2133943
		0.7	0.701535	0.701539	0.74562042	1.174081	1.174081	1.2775278

5 Concluding Remarks

Thermal transport in the Powell-Eyring model via generalised heat flux over an exponentially stretching sheet is examined. The impact of Powell-Eyring fluid parameter, magnetic parameter M , Eckert number Ec , radiation parameter Rd , and thermal relaxation time γ was investigated. The study's most important features are listed below:

- The velocity profile increases as the fluid parameter K increases, but reverse behaviour is noticed for the temperature profile.
- For increasing values of the magnetic parameter M , the velocity profile falls while the temperature rises. In addition, the resistance to flow increases as the magnetic field intensity and K increase.
- The temperature and thickness of the thermal boundary layer are inversely related to the thermal relaxation time γ , whereas the Eckert number Ec has the opposite trend. With an increase in Ec , the temperature rises.
- Increasing values of Rd (radiation parameter) increase the heat fluxes from the surface, which causes the increase in the fluid's temperature and velocity.

Simulations of local Nusselt number and skin friction/co-efficient are used to validate the published work.

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Conflicts of Interest: The authors declare that they have no conflicts of interest to report regarding the present study.

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