

**ARTICLE****Pressure-Induced Instability Characteristics of a Transient Flow and Energy Distribution through a Loosely Bent Square Duct****Sreedham Chandra Adhikari¹, Ratan Kumar Chanda¹, Sidhartha Bhowmick¹, Rabindra Nath Mondal¹ and Suvash Chandra Saha^{2,*}**¹Department of Mathematics, Jagannath University, Dhaka, 1100, Bangladesh²School of Mechanical and Mechatronic Engineering, University of Technology Sydney, New South Wales, Australia

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ABSTRACT

Due to widespread applications of the bent ducts in engineering fields such as in chemical, mechanical, bio-mechanical and bio-medical engineering, scientists have paid considerable attention to invent new characteristics of fluid flow in a bent duct (BD). In the ongoing study, a spectral-based numerical technique is applied to explore flow characteristics and energy distribution through a loosely bent square duct (BSD) of small curvature. Flow is accelerated due to combined action of the non-dimensional parameters; the Grashof number Gr ($=1000$), the curvature δ ($=0.001$), and the Prandtl number Pr ($=7.0$) over a wide domain of the Dean number $0 < Dn \leq 5000$. Fortran code is developed for the numerical computations and Tecplot software with Gost Script and Gost View is used for the post-processing purpose. The numerical study investigates steady solutions (SS) and as a result, a structure of six-branches of SSs composed of 2- to 6-vortex solutions is obtained. Then oscillating behavior with flow transition is discussed by obtaining time-dependent solutions followed by power-spectrum analysis. Results show that the trend of unsteady flow (UF) undergoes in the sequence '*steady-state* \rightarrow *multi-periodic* \rightarrow *steady-state* \rightarrow *chaotic* \rightarrow *multi-periodic* \rightarrow *chaotic*', if Dn is increased. Asymmetric 2- to 4-vortex solutions are obtained for UF. Convective heat transfer (CHT) is then examined obtaining temperature gradients and energy contours, and it is found that CHT is significantly enhanced by the secondary flow (SF). The present study reveals that the role of secondary vortices over heat transfer (HT) is highly significant and HT occurs substantially for the chaotic solutions. Finally, for the interest of validation, the present numerical result is compared with the previously published experimental outcomes, and a good agreement is remarked.

KEYWORDS

Square-shaped duct; curvature; secondary flow; energy distribution; chaos

1 Introduction

Because of tremendous applications of the bent ducts (BD) in physical and natural sciences, bio-mechanical and bio-medical engineering, many highly ambitious researchers have given substantial attention in studying the flow and HT through a BD. The flow pattern inside the aorta and the bifurcation airways of the lung are intricate due to the complex curvature of the



aorta and lung airways. The blood flow or the fluid flow inside the aorta or the bent channel respectively creates SFs causing the centrifugal force, and this SF along with the direction of the axial flow act at the right angle to the main flow direction. The curvature of the aorta and the lung airways shows different physically interesting flow characteristics for the pressure-driven flow. A lot of practical applications like fluid transportation, turbo machinery, gas turbines, heat exchangers, refrigeration, air conditioning system, ventilators, combustion engines, chemical reactors, centrifugal pumps etc., may be mentioned, which attracts the researchers to do advanced research in this fascinating field.

There is a wide-ranging study on fluid flow through a BD that has been continued for several decades. Due to the centrifugal force and tangential stress at the concave wall, acting towards the curvature of the channel center, supplementary secondary vortices appeared which is located near the concave wall, known as the Dean vortices. Dean [1] was the pioneer author who derived the mathematical model first and investigated the viscous incompressible fluid and discovered a pair of counter-rotating vortices appearing in a bent pipe. The bifurcation structure belonging to a combined flow bifurcation consists of several SSs, which are generally influenced by the Centrifugal force (caused due to channel curvature). Several influential investigations for various geometry of the BD were performed by Rudolf et al. [2], Norouzi et al. [3], Yanase et al. [4] for circular cross-section; Nandakumar et al. [5] for semi-circular cross-section; Kao [6] for an oval cross-section; Ligrani et al. [7], Yanase et al. [8], Finlay et al. [9] for a rectangular cross-section.

It has been established that the flow through a stationary bent duct with a temperature difference between the walls, two forces namely centrifugal force and heating-induced buoyancy forces act on the fluid that creates secondary flow. And since the secondary flow enhances heat and mass transfer, knowledge of the magnitude of these effects in different ranges of operating parameters is important in designing the mechanical devices. A comprehensive study of the bifurcation diagram of the fluid through a BSD was performed to investigate the combined solution structure [10]. An extensive simulation of the branching shape of the flow in a BRD was conducted first and detailed by Daskopoulos et al. [11]. Mondal [12] has investigated fluid flow in a BSD and BRD. A detailed study on such system using a spectral method on fluid flow bifurcation structure and stability of 2D flow is available in literature performed by Mondal et al. [13], who showed a close bonding to the transient behavior with the bifurcation diagram. Mondal et al. [14] also studied the bifurcation diagram, stability, and flow state of the flow in a BRD. To obtain reliable and meaningful characteristics and to get a better fundamental understanding of swirling flow and its thermal properties, an advanced numerical simulation model based on 3D vortex structures is used by Watanabe et al. [15]. They have described bifurcation phenomena and stability of the solutions in an SD for both two-and three-dimensional analysis. Chen et al. [16] performed a bifurcation study of the flow passing in a bent tube with increasing Dn and aspect ratio (Ar), where they observed two types of bifurcations depending on the range of Ar . Recently, Hasan et al. [17,18] applied a spectral-based numerical technique to investigate the critical points considering stationary and non-stationary BSD flow. In continuation of this study, very recently, Chanda et al. [19] investigated effects of curvature ratio on fluid flow and thermal distribution in a rotating BRD of aspect ratio 3 maintaining a temperature difference between the horizontal walls using the method that was used by Hasan et al. [20]. They studied flow scenarios over a wide range of the curvature ($0.001 \leq \delta \leq 0.5$) for both co-and counter-rotation of the system. They obtained five branches of SS composed of 2- to 11-pair vortices. Effects of curvature on secondary vortices were also obtained and displayed in the bar diagrams. However, most of the previous studies have been performed to explore flow characteristics and temperature distribution

through a bent square or rectangular-shaped ducts with medium or strong curvature that are differentially heated. The present work is relatively a comprehensive study on bifurcation structure as well as flow transition and energy distribution through a bent square duct with small curvature considering the bottom and outer walls heated while cooling the other two.

To obtain reliable and meaningful data as well as to get a better fundamental understanding of the oscillating behavior of the unsteady flow in a confined geometry, time-history analysis in a BRD was performed first by Yanase et al. [8]. Several works have been conducted for the last three decades about oscillating behavior in a confined geometry. Chandratilleke et al. [21] performed a numerical approach to elucidate the flow properties through the variable geometries duct for different aspect ratios heated the outer surface. Wang et al. [22] studied numerically and empirically the periodic fluctuation for an incompressible fluid in a BSD, and the comparison shows excellent agreement with both the results. Mondal et al. [23] conducted a numerical manner to analyze the flow transition in bent duct (BD). They investigated the impacts of Dn and Gr numbers on the SF pattern. Nowruzi et al. [24] applied the Homotopic perturbation method to investigate hydrodynamic instability in BD of small aspect ratio for several curvatures. However, their study was unable to focus on the influence of the parameters in the flow transition and velocity profiles. Islam et al. [25] deliberated the influence of the Dean number over a wide range of Tr on transition in a rotating CRD flow. Hasan et al. [18] reflected the numerical investigation of UF through a BSD, and the relationship was established between the stability of SS and US. Chanda et al. [26] conducted a numerical investigation through a BRD for both co-and counter-rotation cases. Very recently, Dolon et al. [27] developed a computational model on curved rectangular duct flow and investigated the combined effects of centrifugal and heating-induced buoyancy instability of the flow. They built up a relationship between the flow velocity and isotherms. Impacts of Dean vortex on overall heat transfer were also shown. However, studies on strong centrifugal instability received less attention before, while the transient solution with coupled impacts on buoyancy-influenced centrifugal unsteadiness through a stationary BSD is not considered though it has an extensive application in engineering processes; in this paper, efforts are directed to reduce this gap.

An essential phenomenon for curved-channel flow is the calculation of HT in a BD because of numerous engineering and industrial applications such as aeronautical, petroleum, mechanical and chemical engineering, metallic and plastic industry, etc. The mentionable applications of flows in the various curved duct (CD) are to promote HT in the fluid causing Dean vortices. Wang et al. [22] conducted a numerical analysis to explain the properties of swirling flow in a CD of aspect ratios 1 to 8 heating from the outer surface. Riyi et al. [28] performed the numerical simulations and experimental studies of the HT in an eccentric annular with maintaining temperature differences individually. Mondal et al. [13] studied the oscillating behavior of the thermal flow in a BSD numerically. The authors investigated the SF structure and the effects of HT performance. In the succeeding paper, Mondal et al. [29] investigated the regular and irregular oscillation with identifying the symmetry and without symmetry condition in flow behaviors, respectively. A numerical procedure, known as FDM, is used by Zhang et al. [30] to investigate the time-dependent CHT and mixing between two different geometries. Hasan et al. [31] performed numerical simulation with CHT through a rotating BSD for various curvatures. They discussed the steady and unsteady solutions with linear stability and found that SF enhances CHT significantly, and the chaotic flow, which occurs at large Dn 's, enhances HT more efficiently than the other US. Recently, Zhao et al. [32] illustrated the influence of friction factor and Nusselt number in terms of time instead of curvature ratios and large Reynolds numbers. Very recently,

Chanda et al. [26] discussed the CHT for rotating BRD flow, and they obtained the nearly same result as obtained by Hasan et al. [33]. Very recently, Chanda et al. [34] applied spectral method to investigate heat-flux effect on fluid flow and energy distribution in a BRD. They obtained four SS comprising with 2- to 12-vortex solutions. Effects of curvature on secondary vortices were also obtained and displayed in the bar diagrams. All of these studies admittedly illustrate the flow pattern and heat transfer characteristics in bent square duct for moderate or large curvature, where time-dependent flow features in the presence of centrifugal and buoyancy forces with pressure-induced instability characteristics in a BSD with small curvature are not considered greatly though it has ample engineering applications e.g., plastic industry, metallic industry, gas turbines etc. Considering this issue in mind, an objective of this paper is to find complex structure of the transient flow feature and vortex formation of SF for fully developed 2D flow through a BSD with combined effects of free and forced convection on heat transfer.

The key intention of the current study is to examine the perplexing flow feature and energy distribution in a bent square-shaped duct by finding steady solutions and calculating non-linear behavior of the flow by time-evolution computation. The study articulates and verifies an advanced approach for computational scheme to well identify hydrodynamic variability in a BSD reflected by the generation of Dean vortices. The main purpose of this study is, therefore, to pursuit solution formation of SSs and explores transient behavior with heat-flux properties of secondary vortices (SV) on CHT.

2 Flow Model and Mathematical Formulation

The BSD, whose geometrical parameter of duct height (=width) is $2d$, the radius of curvature δ is considered where the bottom and outer side-wall are heated while the other two walls in room temperature as illustrated in Fig. 1. The x' and y' axes are considered to be in the horizontal and vertical directions respectively and z' along the center-line of the duct. The working fluid is water which is envisaged as viscous and incompressible in the existing discussion that is allowed to flow consistently in the steam-wise direction.

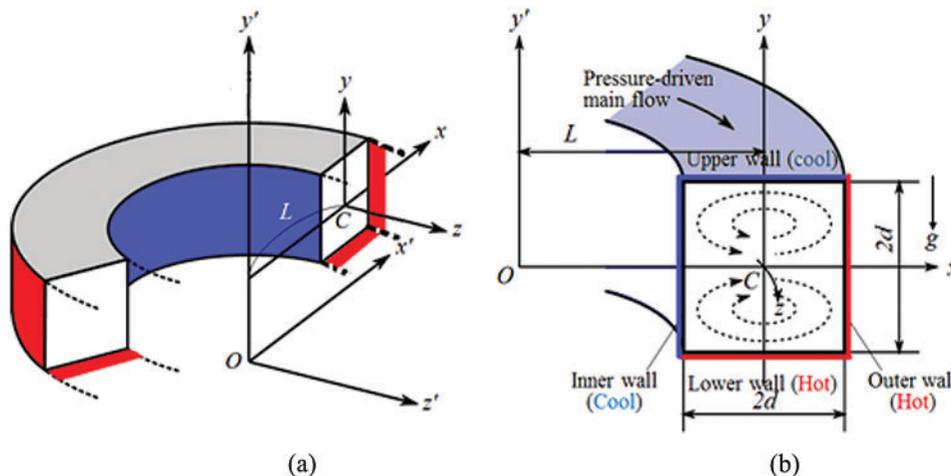


Figure 1: (a) Coordinate system (b) Cross-sectional view

Then, the advancement of transient flow and HT inside a BSD is governed by the following dimensional conservation of mass, momentum, and energy equation can be expressed as:

Conservation of mass equation:

$$\frac{\partial u'}{\partial r'} + \frac{\partial v'}{\partial y'} + \frac{u'}{r'} = 0 \tag{1}$$

Momentum equations:

$$\frac{\partial u'}{\partial t'} + u' \frac{\partial u'}{\partial r'} + v' \frac{\partial u'}{\partial y'} - \frac{w'^2}{r'} = -\frac{1}{\rho} \frac{\partial P'}{\partial r'} + \nu \left[\frac{\partial^2 u'}{\partial r'^2} + \frac{\partial^2 u'}{\partial y'^2} + \frac{1}{r'} \frac{\partial u'}{\partial r'} - \frac{u'}{r'^2} \right], \tag{2}$$

$$\frac{\partial v'}{\partial t'} + u' \frac{\partial v'}{\partial r'} + v' \frac{\partial v'}{\partial y'} = -\frac{1}{\rho} \frac{\partial P'}{\partial y'} + \nu \left[\frac{\partial^2 v'}{\partial r'^2} + \frac{1}{r'} \frac{\partial v'}{\partial r'} + \frac{\partial^2 v'}{\partial y'^2} \right] + g\beta T', \tag{3}$$

$$\frac{\partial w'}{\partial t'} + u' \frac{\partial w'}{\partial r'} + v' \frac{\partial w'}{\partial y'} + \frac{u'w'}{r'} = -\frac{1}{\rho} \frac{1}{r'} \frac{\partial P'}{\partial z'} + \nu \left[\frac{\partial^2 w'}{\partial r'^2} + \frac{\partial^2 w'}{\partial y'^2} + \frac{1}{r'} \frac{\partial w'}{\partial r'} - \frac{w'}{r'^2} \right] \tag{4}$$

Energy equation:

$$\frac{\partial T'}{\partial t'} + u' \frac{\partial T'}{\partial r'} + v' \frac{\partial T'}{\partial y'} = \kappa \left[\frac{\partial^2 T'}{\partial r'^2} + \frac{1}{r'} \frac{\partial T'}{\partial r'} + \frac{\partial^2 T'}{\partial y'^2} \right] \tag{5}$$

where, $r' = L + x'$ and the sign (') used in Eqs. (1)–(5) represents the dimensional variables. Here, P' represents pressure, T' ; temperature, and t' ; time. All these are dimensional variables. In this consideration ρ is the density, ν ; kinematic viscosity, β ; coefficient of thermal expansion, κ ; coefficient of thermal diffusivity, and g is the gravitational acceleration. The variables are made dimensionless by using $U_0 = \frac{v}{d}$, where d is half-width of duct cross-section, as:

$$u = \frac{u'}{U_0}, \quad v = \frac{v'}{U_0}, \quad w = \frac{\sqrt{2\delta}}{U_0} w', \quad x = \frac{x'}{d}, \quad \bar{y} = \frac{y'}{d}, \quad z = \frac{z'}{d}$$

$$\xi = \frac{T'}{\Delta T'}, \quad t = \frac{U_0}{d} t', \quad \delta = \frac{d}{L}, \quad P = \frac{P'}{\rho U_0^2}, \quad G = -\frac{\partial P'}{\partial z'} \frac{d}{\rho U_0^2}$$

The stream function η , satisfying the mass conservation equation, can be stated as:

$$u = \frac{1}{\alpha} \frac{\partial \eta}{\partial y} \quad \text{and} \quad v = -\frac{1}{\alpha} \frac{\partial \eta}{\partial x} \quad \text{where} \quad \alpha = 1 + \delta x \tag{6}$$

Considering the flow as invariant in the z' direction, which is driven by a specific pressure drop G along the center-line of the channel, the resulting dimensionless equations for ω , η , and ξ are as follows:

$$\alpha \frac{\partial \omega}{\partial t} = Dn + \alpha \Delta_2 \omega - \frac{\partial (\omega, \eta)}{\partial (x, y)} - \frac{\delta^2 \omega}{\alpha} - \frac{\delta}{\alpha} \frac{\partial \eta}{\partial y} \omega + \delta \frac{\partial \omega}{\partial x} \tag{7}$$

$$\begin{aligned} \left(\Delta_2 - \frac{\delta}{\alpha} \frac{\partial}{\partial x} \right) \frac{\partial \eta}{\partial t} = & -\frac{1}{\alpha} \frac{\partial (\Delta_2 \eta, \eta)}{\partial (x, y)} + \frac{\delta}{\alpha^2} \left[\frac{\partial \eta}{\partial y} (2\Delta_2 \eta) - \frac{3\delta}{\alpha} \frac{\partial \eta}{\partial x} + \frac{\partial^2 \eta}{\partial x^2} \frac{\partial \eta}{\partial x} \frac{\partial^2 \eta}{\partial x \partial y} \right] \\ & + \frac{\delta}{\alpha^2} \times \left[3\delta \frac{\partial^2 \eta}{\partial x^2} - \frac{3\delta^2}{\alpha} \frac{\partial \eta}{\partial x} \right] - \frac{2\delta}{\alpha} \frac{\partial}{\partial x} \Delta_2 \eta + \omega \frac{\partial \omega}{\partial y} + \Delta_2^2 \eta - \alpha Gr \frac{\partial \xi}{\partial x} \end{aligned} \quad (8)$$

and,

$$\frac{\partial \xi}{\partial t} = \frac{1}{Pr} \left(\Delta_2 \xi + \frac{\delta}{\alpha} \frac{\partial \xi}{\partial x} \right) - \frac{1}{\alpha} \frac{\partial (\xi, \eta)}{\partial (x, y)}. \quad (9)$$

The non-dimensional parameters that characterize the flow and appear in Eqs. (7)–(9) are the Dean number, $Dn \left(= \frac{Gd^3}{\mu\nu} \sqrt{\frac{2d}{L}} \right)$; the Grashof number, $Gr \left(= \frac{\beta g \Delta \xi d^3}{\nu^2} \right)$ and the Prandtl number, $Pr \left(= \frac{\nu}{\kappa} \right)$.

The no-slip boundary condition for ω , η and ξ are taken as:

$$\omega = \eta = \frac{\partial \eta}{\partial x} = 0 \text{ at } x = \pm 1, y = y \quad (10a)$$

$$\omega = \eta = \frac{\partial \eta}{\partial x} = 0 \text{ at } x = x, y = \pm 1 \quad (10b)$$

$$\xi(1, y) = y, \quad \xi(-1, y) = y, \quad \xi(x, 1) = x, \quad \xi(x, -1) = x \quad (11)$$

3 Numerical Analysis

3.1 Method of Numerical Design

Since the method is numerically based, we have used the Spectral method as a numerical technique to solve the Eqs. (7)–(9). This is one of the best methods for solving the Momentum equation as well as energy equations (see Gottlieb et al. [35] for details). By this method, the variables are expanded in a series of functions consisting of Chebyshev polynomials. The expansion functions $\mu_n(x)$ and $\phi_n(x)$ are stated as:

$$\left. \begin{aligned} \mu_n(x) &= (1 - x^2) T_n(x), \\ \phi_n(x) &= (1 - x^2)^2 T_n(x) \end{aligned} \right\} \quad (12)$$

where, $T_n(x) = \cos(n \cos^{-1}(x))$ is the n^{th} order of Chebyshev polynomials. Furthermore, $\omega(x, y, t)$, $\eta(x, y, t)$ and $\xi(x, y, t)$ are expanded in terms of $\mu_n(x)$ and $\phi_n(x)$ as:

$$\left. \begin{aligned} \omega(x, y, t) &= \sum_{m=0}^M \sum_{n=0}^N \omega_{mn}(t) \mu_m(x) \mu_n(y) \\ \eta(x, y, t) &= \sum_{m=0}^M \sum_{n=0}^N \eta_{mn}(t) \phi_m(x) \phi_n(y) \\ \xi(x, y, t) &= \sum_{m=0}^M \sum_{n=0}^N \xi_{mn}(t) \mu_m(x) \mu_n(y) + x - y \end{aligned} \right\} \quad (13)$$

Here, the collocation points (x_i, y_j) are taken to be:

$$x_i = \cos \left[\pi \left(1 - \frac{i}{M+2} \right) \right], \quad y_j = \cos \left[\pi \left(1 - \frac{j}{N+2} \right) \right] \quad (14)$$

where $i = 1, \dots, M + 1$ and $j = 1, \dots, N + 1$. To achieve the steady solution $\bar{\omega}(x, y), \bar{\eta}(x, y)$ and $\bar{\xi}(x, y)$ the expansion chain (13) with coefficients $\omega_{mn}(t), \eta_{mn}(t)$ and $\xi_{mn}(t)$ are transformed into the basic Eqs. (7)–(9) abide by applying the collocation method. To escape difficulty near the point of inflection for the steady solution branches by using the arc-length equation:

$$\sum_{m=0}^M \sum_{n=0}^N \left\{ \left(\frac{d\omega_{mn}}{ds} \right)^2 + \left(\frac{d\eta_{mn}}{ds} \right)^2 + \left(\frac{d\xi_{mn}}{ds} \right)^2 \right\} = 1 \quad (15)$$

which is solved simultaneously with Eq. (17) by using the Newton-Raphson iteration method with path continuation technique. An initial guess at a point $s + \Delta s$ is considered starting from point s as follows:

$$\left. \begin{aligned} \omega_{mn}(s + \Delta s) &= \omega_{mn}(s) + \frac{d\omega_{mn}(s)}{ds} \Delta s \\ \eta_{mn}(s + \Delta s) &= \eta_{mn}(s) + \frac{d\eta_{mn}(s)}{ds} \Delta s \\ \xi_{mn}(s + \Delta s) &= \xi_{mn}(s) + \frac{d\xi_{mn}(s)}{ds} \Delta s \end{aligned} \right\} \quad (16)$$

The convergence is assured by taking suitably small ε_p ($\varepsilon_p < 10^{-10}$) defined as:

$$\varepsilon_p = \sum_{m=0}^M \sum_{n=0}^N \left[\left(\omega_{mn}^{(p+1)} - \omega_{mn}^p \right)^2 + \left(\eta_{mn}^{(p+1)} - \eta_{mn}^p \right)^2 + \left(\xi_{mn}^{(p+1)} - \xi_{mn}^p \right)^2 \right] \quad (17)$$

Finally, in order to compute the time-dependent solution, the Crank-Nicolson and Adams-Bashforth methods along with the function expansion (13) and the collocation methods, are applied to Eqs. (7)–(9). A detailed description of the method is available in Mondal et al. [13].

3.2 Hydrodynamic Resistance Coefficient

The resistance coefficient λ defined as:

$$\frac{\bar{p}_1 - \bar{p}_2}{\Delta \bar{z}} = \frac{\lambda}{d_h} \frac{1}{2} \rho \langle \bar{\sigma} \rangle^2 \quad (18)$$

where, \bar{d}_h is the hydraulic diameter. The mean axial velocity $\langle \bar{\sigma} \rangle$ is calculated by:

$$\langle \bar{\sigma} \rangle = \frac{v}{4\sqrt{2\delta d}} \int_{-1}^1 dx \int_{-1}^1 \sigma(x, y, t) dy \quad (19)$$

λ is related to the mean non-dimensional axial velocity $\langle \sigma \rangle$ as:

$$\lambda = \frac{4\sqrt{2\delta Dn}}{\langle \sigma \rangle^2} \quad (20)$$

The value λ is calculated from Eq. (20) mathematically.

4 Results and Discussion

A detailed investigation has been carried out and discussed the branching structure, consisting of the SSs and unsteady solutions. Pertinent parameters are considered as shown in [Table 1](#).

Table 1: Values or ranges of pertinent parameters considered in the present investigation

Parameters	Considered value/ranges	Comments
Curvature (δ)	0.001	Small curvature
Aspect ratio (Ar)	1.0	Square duct
Grashof number (Gr)	1000	Buoyancy parameter
Prandtl number (Pr)	7.0	Water
Dean number (Dn)	$0 < Dn \leq 5000$	Pressure-gradient parameter

4.1 Branching Structure

In order to find out the structure of SSs using the parameters as presented in [Table 1](#), the result is presented in [Fig. 2a](#). We noticed from [Fig. 2a](#) that six asymmetric branches of SSs are available, which are named as the 1st, 2nd, 3rd, 4th, 5th, and the 6th steady branch (br). Assorted colors and line patterns have been used to distinguish the obtained branches. [Fig. 2b](#) represents the amplification of [Fig. 2a](#) for visualizing the perplexing branch structure more pronouncedly as well as to categorize the SSs from each other. It is observed from [Fig. 2a](#) that only the 1st branch covers the entire region of Dn ($0 < Dn \leq 5000$), while the 2nd, 3rd, 4th, 5th, and the 6th steady br. exist in the regions for $579 \leq Dn \leq 5000$, $2487 \leq Dn \leq 5000$, $2206 \leq Dn \leq 5000$, $3600 \leq Dn \leq 5000$ and $4646 \leq Dn \leq 5000$ respectively with several turnings in every branch. [Figs. 3–8](#) demonstrate the vortex structure of SSs with axial velocity, secondary flow, and energy distribution for various values of Dn for each branch sequentially. It is observed that the 1st, 2nd, 3rd, 4th, 5th and 6th branches are formed with 2- and 3-vortex, 2–6-vortex, only 4-vortex, 4–6-vortex, 3–5-vortex, and 3–4-vortex solutions, respectively, and the axial flow consists of high-velocity regions appeared near the outward side for all branches except the 1st branch. In this study, fluid is accelerated under combined action of the 3 (three) non-dimensional parameters; the Dean number (Dn), which is the pressure gradient parameter that accelerates fluid flow along the centre-line of the duct; the Grashof number (Gr), which is the buoyancy force parameter caused due to temperature difference between the walls and the curvature δ creates centrifugal force. The curvature is considered to be small ($\delta = 0.001$). The reason is that small-curvatures ducts are used in many engineering applications, such as in gas turbines, metallic and plastic industry, power engineering, telecommunication engineering etc. As seen in the figures of SF patterns, the SF consists of two-or more-vortex which are asymmetric with respect to the horizontal plane $y = 0$. The reason is that heating the outer and bottom walls causes deformation of the secondary flow and yields asymmetry of the flow. With the heating and cooling the walls changes of fluid density that induce thermal convection in the fluid; the resulting flow behavior is, therefore, determined by the combined action of the radial flow caused by the centrifugal body force and the convection caused by the buoyancy force due to temperature difference between the walls. This asymmetry of the flow is well discussed by Mondal et al. [36]. In this regard, it should be noted that Mondal et al. [13] studied characteristics of the non-isothermal flow through a BSD for various curvatures and identified a topological change in the bifurcation diagram below or above the critical curvature $\delta_c = 0.279645$. They obtained 4 (four) branches of steady solutions below the critical value of δ (for $\delta = 0.001$ as well). In the present work, however, we investigate solution

structure, energy distribution and vortex structure of secondary flows for non-isothermal flow in loosely coiled square duct and obtained 6 (six) branches of asymmetric steady solutions due to pressure and temperature-induced buoyancy instability.

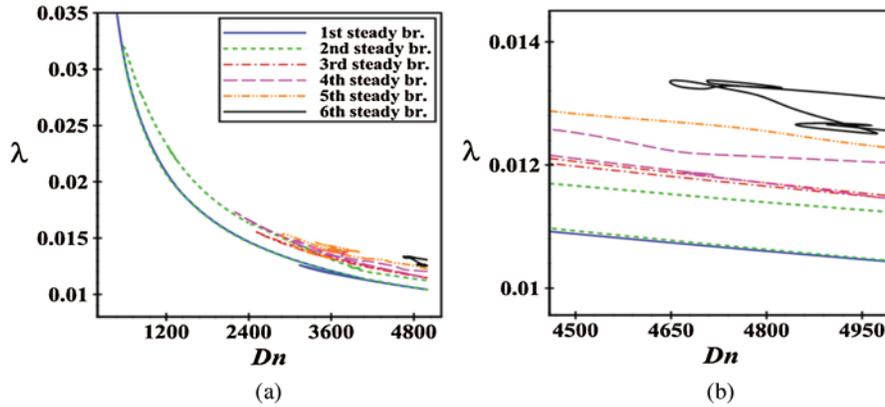


Figure 2: (a) Branching structure of SS; (b) Enlargement of Fig. 2a at large Dn 's

Here, we show the bar diagram of the vortex structure of secondary flows obtained at six branches of SS observed at a glance at various values of Dn for $\delta = 0.001$ presented in the $(Dn - \theta)$ plane in Fig. 9. From the figure, the maximum 6-vortex solution is realized in the 2nd and 4th branches at $Dn = 4500$. On the other hand, the 1st br. contains minimum 2- and 3-vortex. We noticed that an increase in Dn leads to a higher number of vortices. Due to centrifugal-buoyancy instability the Dean vortices are generated at the vicinity of the outer concave wall and because of the reverse flow of the outward secondary flow the Dean vortices are sometimes generated at the convex wall of the channel which is remarked by Islam et al. [25] for rotating BRD flow.

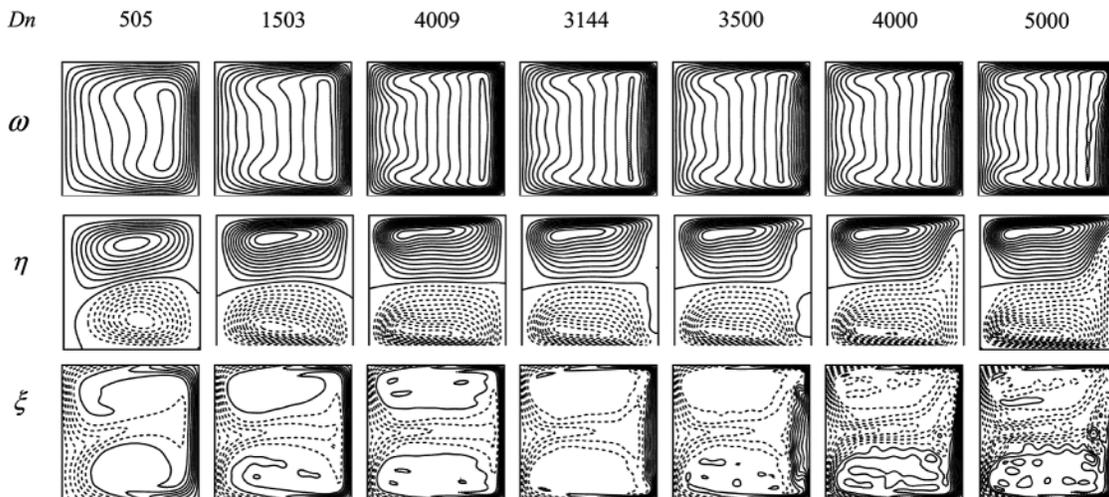


Figure 3: Velocity contour (top & middle) and isotherm (bottom) on the 1st branch

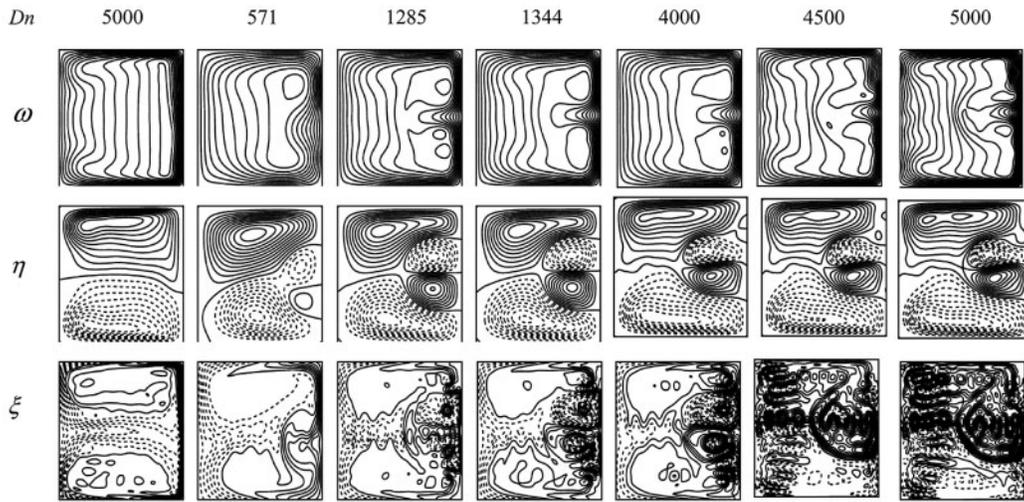


Figure 4: Velocity contour (top & middle) and isotherm (bottom) on the 2nd branch

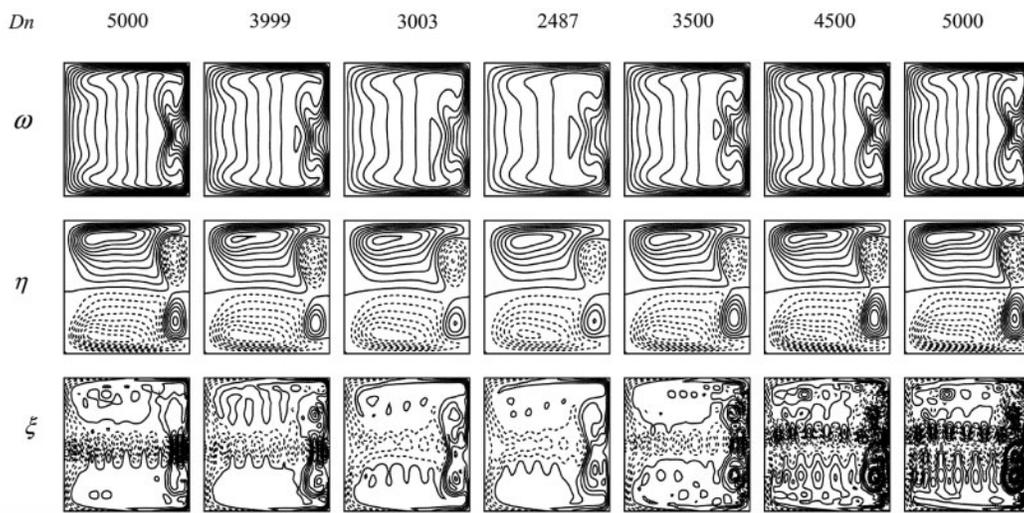


Figure 5: Velocity contour (top & middle) and isotherm (bottom) on the 3rd branch

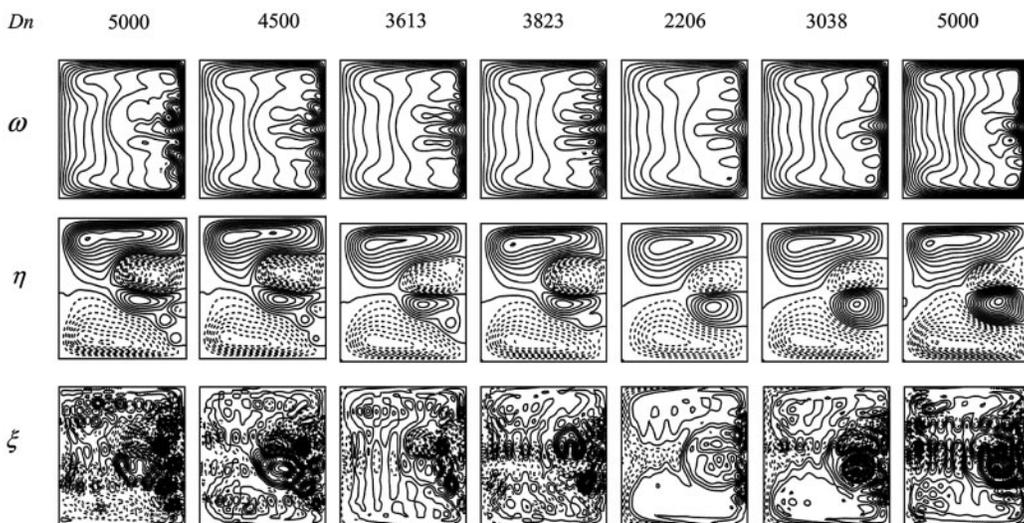


Figure 6: Velocity contour (top & middle) and isotherm (bottom) on the 4th branch

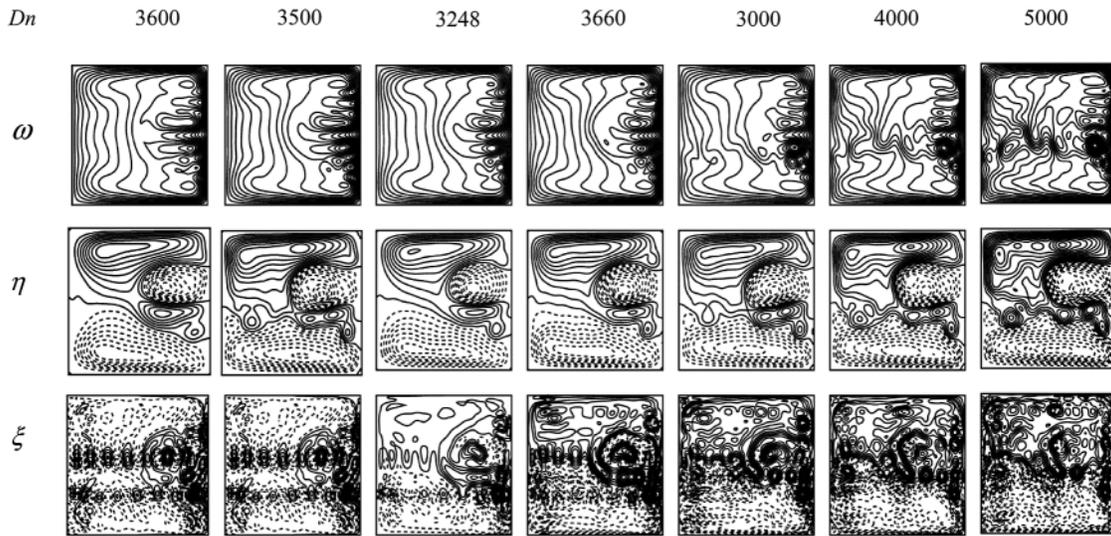


Figure 7: Velocity contour (top & middle) and isotherm (bottom) on the 5th branch

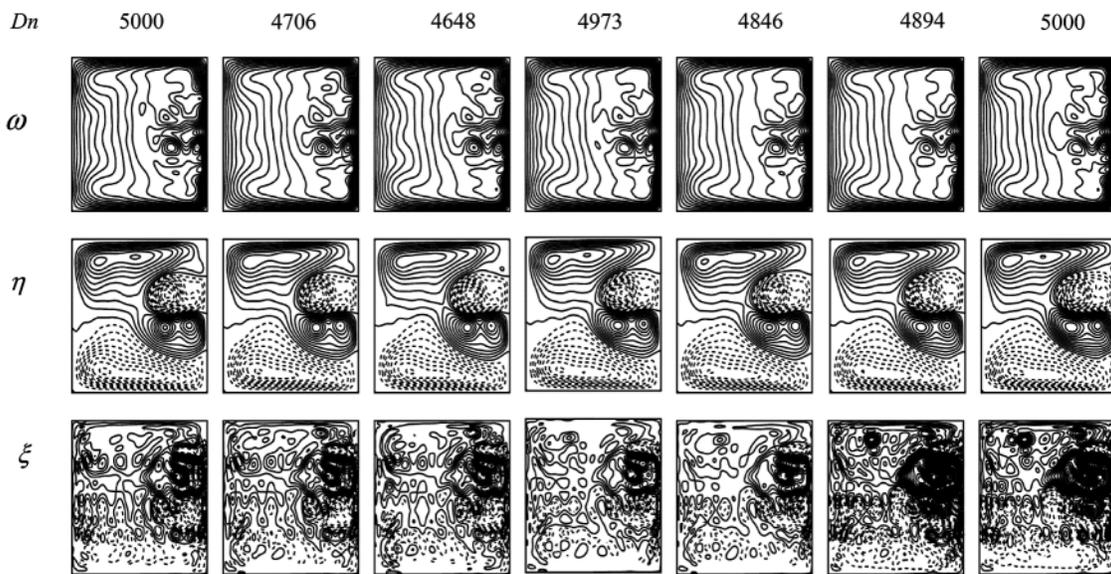


Figure 8: Velocity contour (top & middle) and isotherm (bottom) on the 6th branch

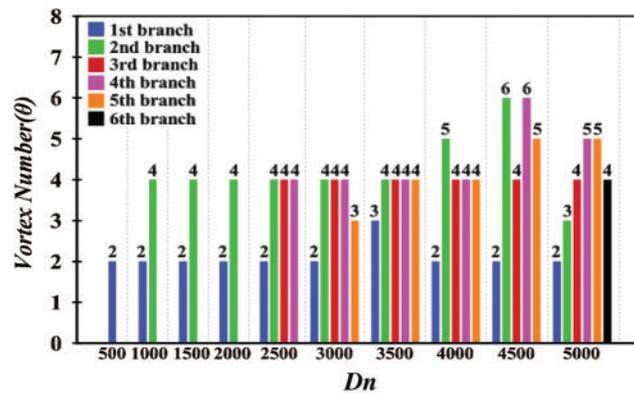


Figure 9: Vortex structure of secondary flow for steady branches for $\delta = 0.001$

4.2 Unsteady Solutions

An exhaustive investigation is presented for calculating the oscillating behavior with the λ values for SSs at the above-mentioned Dn at $\delta = 0.001$ pointed out by straight lines of the same sort as used in Fig. 2a. To well vindicate the flow state more precisely, power-spectrum (P-S) using log-log scale has been analyzed. First, we calculate the oscillating behavior of λ for $Dn = 500$, we discovered the steady-state flow with asymmetric 2-vortex as presented in Figs. 10a and 10b. The present study shows that as Dn is increased gradually, the steady-state flow transforms into a multi-periodic flow that moves around $\lambda = 0.024$ with asymmetric 2- and 3-vortex solutions for one period with time $7.45 \leq t \leq 7.68$ at $Dn = 1000$ as shown in Figs. 11a and 11c. For precise observation of the multi-periodicity, we plot P-S density as depicted in Fig. 11b, where we observe that the line spectrum is distributed to frequency signals with a few signals at high amplitude. In contrast, the others are low and then the frequency signals become flatted gradually that confirmed multi-periodicity. Furthermore, the flow fluctuates above all the SSs, the multi-periodic solutions being independent of the initial condition. Figs. 12a and 12b representing the flow again turns to steady-state with a 2-vortex solution for $Dn = 1500$. An interesting occurrence happens that the flow turns chaotic after $Dn = 2010$. The chaotic solution with asymmetric 2- to 4-vortex for $Dn = 2750$ is observed as shown in Figs. 13a and 13c. The irregular oscillation which moves around $\lambda = 0.0144$ is observed (refer to Fig. 13b). The flow swings between the 1st and 3rd steady solutions, which indicates the transitional chaos. Now, we perform time advancement as presented in Figs. 14a and 14c, which show that the flow oscillates regularly between 2- and 3-vortex solutions for $Dn = 3000$. It can be seen that the periodic flow moves around $\lambda = 0.0137$ and undulates between the 1st and 3rd SS branches. The P-S for justifying the flow state is drawn in Fig. 14b, which indicates the periodic flow.

Next, we deliberated the oscillating behavior for $Dn = 3500$ and observed that the flow oscillates irregularly between the 2nd and the 5th steady solutions, i.e., the strong chaotic solution with 2- to 4-vortex as reflected in Figs. 15a and 15c. We draw P-S density of the unsteady flow to make sure the flow is chaotic as exhibited in Fig. 15b, which confirms the chaotic flow, and it is further interesting to understand that the unsteady flow at $Dn = 5000$ swings in an imbalanced shape again with vibration between the 2nd and 5th steady solutions, i.e., the chaotic flow remains unchanged and it is also strong chaotic with asymmetric 2- and 4-vortex solution (refer to Figs. 16a and 16c). To observe the chaotic flow more apparently, we draw PS density (Fig. 16b). Visibly, the distinct frequency with harmonic modes disappears and gives clear evidence for *strong chaos*. It is also noticed that the chaotic flow becomes stronger as Dn is increased. As seen in the temperature contours, the enhancement of heat transfer for chaotic flow is more effective than the other flow states because of the generation of substantial number of secondary vortices near the concave wall for the chaotic flow. The centrifugal and buoyancy forces influence the overall flow pattern and Dean vortices.

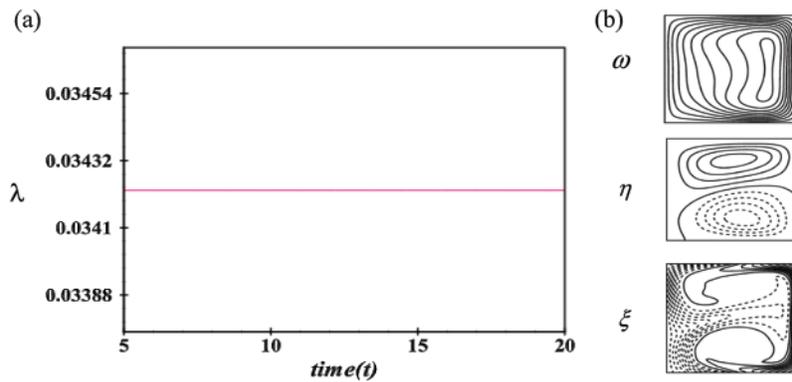


Figure 10: Transient solution for $Tr = 500$ (a) λ as a function of time (b) Velocity contour (top & middle) and isotherm (bottom) $t = 5.0$

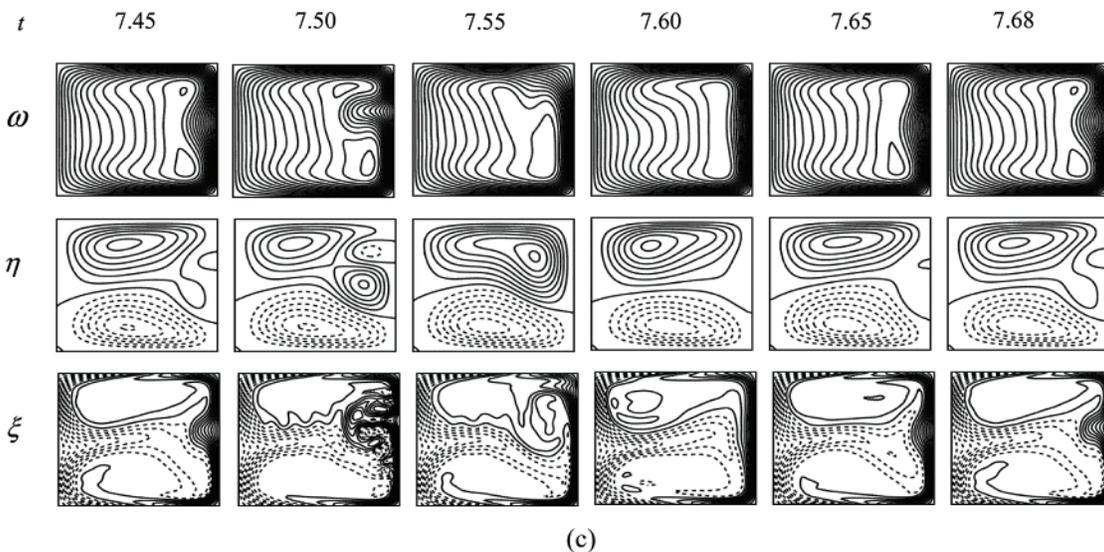
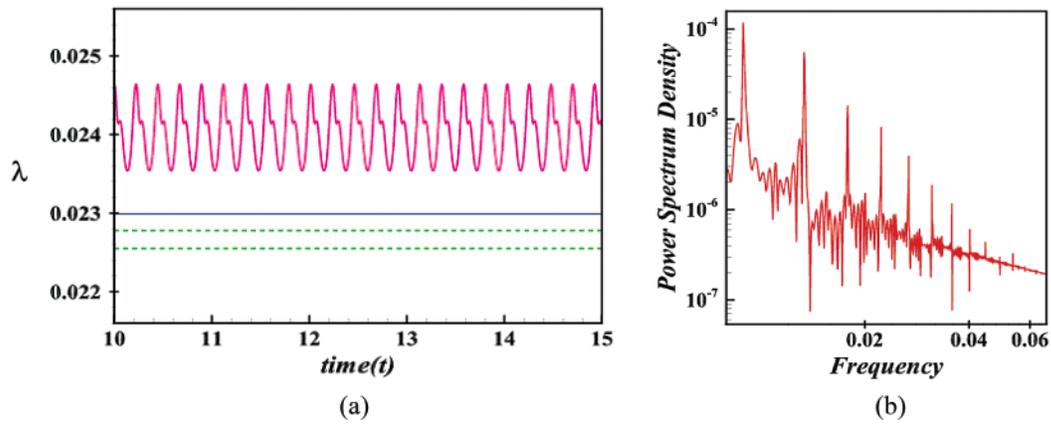


Figure 11: Transient solution for $Dn = 1000$ (a) λ as a function of time (b) P-S of (a) and (c) Velocity contour (top & middle) and isotherm (bottom)

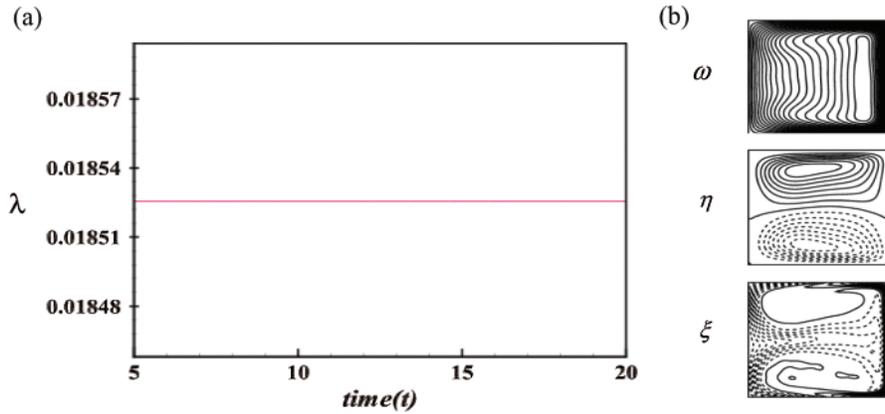


Figure 12: Transient solution for $Tr = 1500$ (a) λ as a function of time, (b) Velocity contour (top & middle) and isotherm (bottom) at $t = 20$

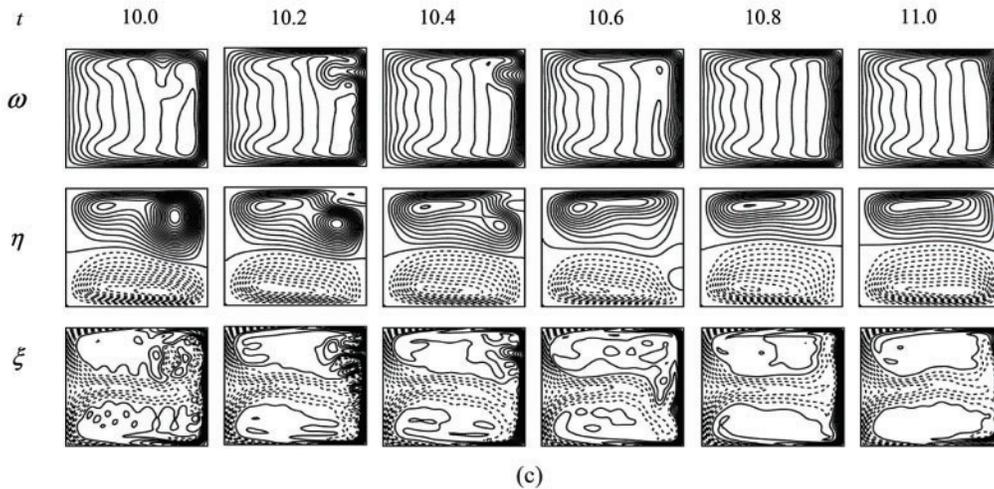
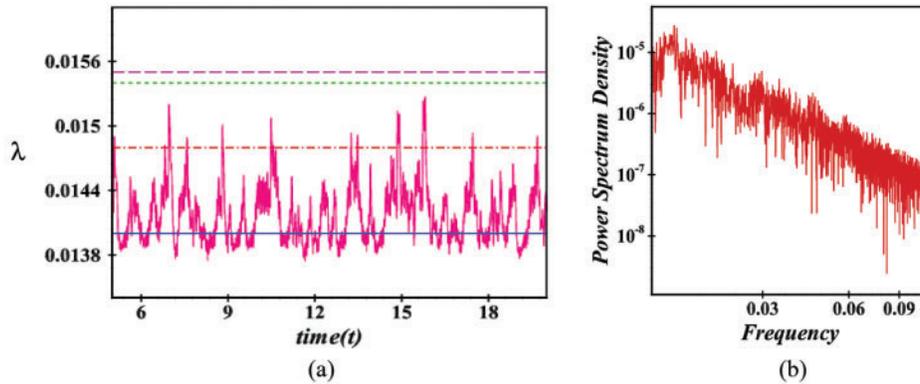


Figure 13: Transient solution for $Dn = 2750$ (a) λ as a function of time (b) P-S of (a) and (c) Velocity contour (top & middle) and isotherm (bottom)

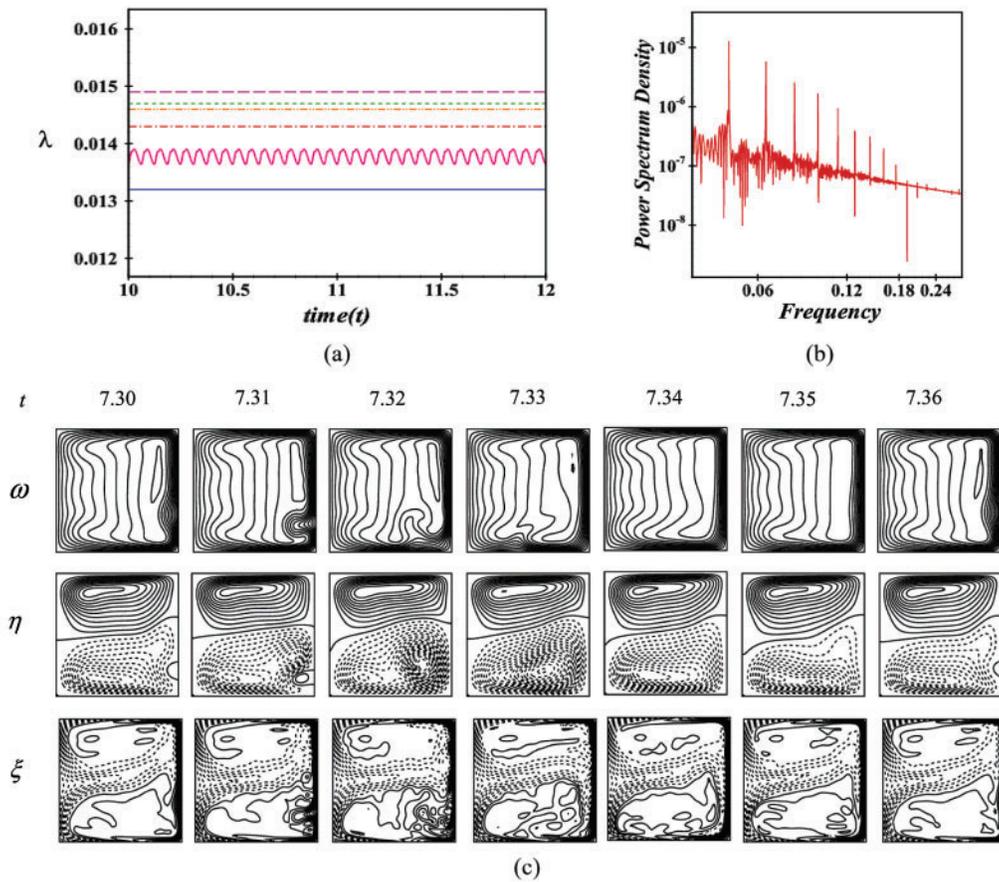


Figure 14: Transient solution for $Dn = 3000$ (a) λ as a function of time (b) P-S of (a) and (c) Velocity contour (top & middle) and isotherm (bottom)

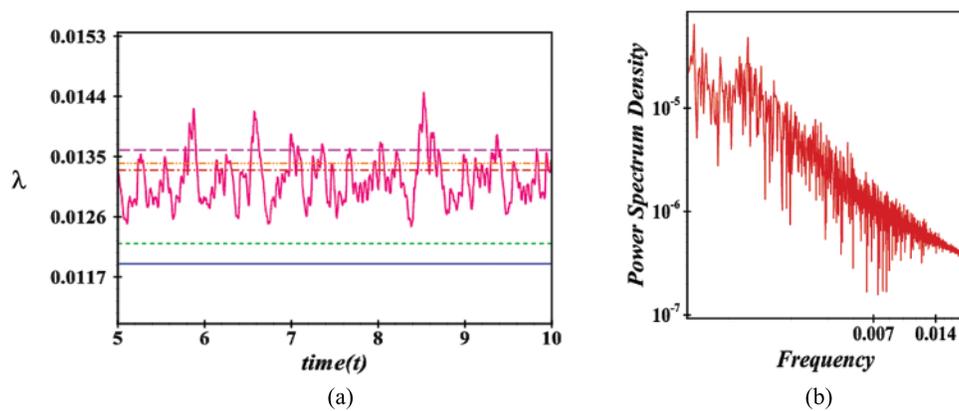


Figure 15: (Continued)

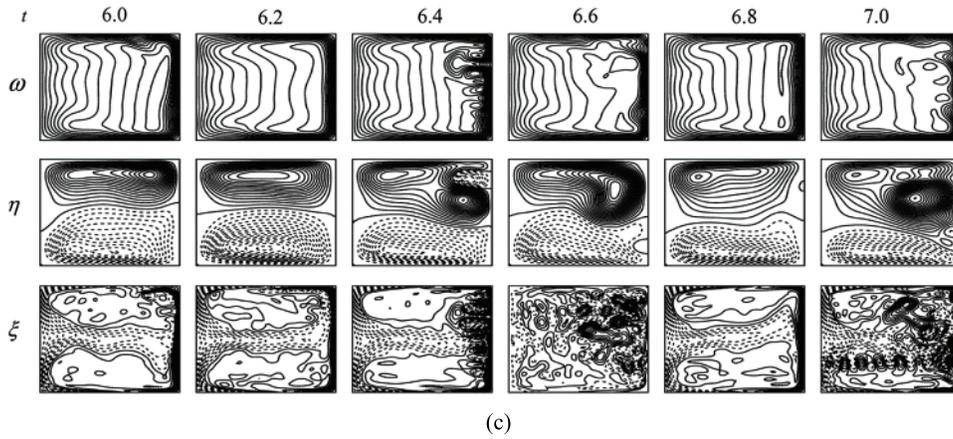


Figure 15: Transient solution for $Dn = 3500$ (a) λ as a function of time (b) P-S of (a) and (c) Velocity contour (top & middle) and isotherm (bottom)

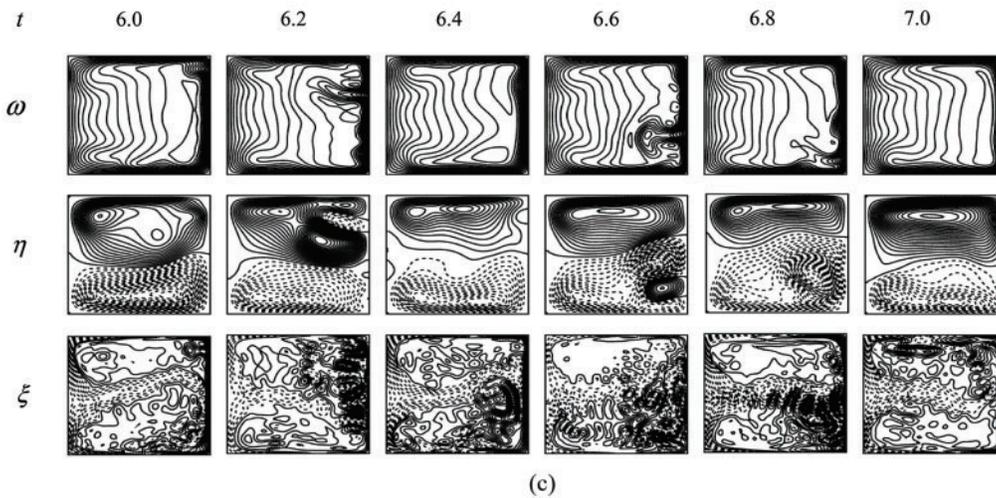
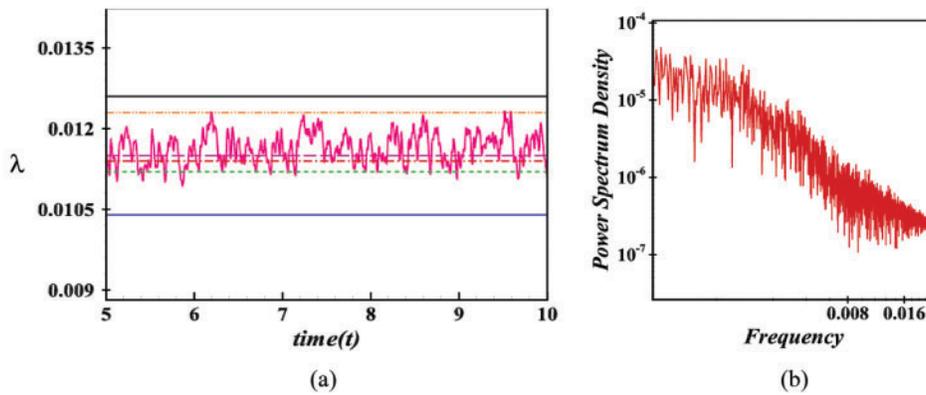


Figure 16: Transient solution for $Dn = 5000$ (a) λ as a function of time (b) P-S of (a) and (c) Velocity contour (top & middle) and isotherm (bottom)

4.3 Flow State and Vortex Structure

A schematic diagram of the variation of unsteady flow state with respect to Dn is shown in Fig. 17a. Here, the steady-state solution is denoted by squares, periodic or multi-periodic by circles and the chaotic by crosses. The intervals for the various US exist: steady-state; $0 < Dn \leq 865$, $1365 \leq Dn \leq 2010$, periodic/multi-periodic; $856 \leq Dn \leq 1365$, $2750 \leq Dn \leq 3245$ and chaotic solution; $2010 \leq Dn \leq 2750$ and $3245 \leq Dn \leq 5000$. The number of Dean vortices has been presented in Fig. 17b. The steady-state flow is composed of asymmetric 2-vortex solution only, whereas periodic flow consists of 2–3-vortex solution. On the other hand, the chaotic flow is composed of a 2–4-vortex solution. In this study, it is observed that the number of secondary vortices increases for chaotic flow and reached at the highest number compared to other cases. As Dn is increased, the fluid particles move in the vicinity of the wall and make friction to each other; at a certain time, Dean vortices are constructed yonder the wall of the channel which plays an outstanding responsibility in transferring heat from the outer wall to the fluid.

In Fig. 18, we present a pie chart to show the percentage of unsteady flow state over the Dn number. Since each unsteady solution for Dn values has a region, so we have established the percentage of steady-state, periodic, and chaotic flow. As visualized in the pie chart described in Fig. 18, the steady-state flow covers almost 29% combining two ranges, whereas periodic is approximately 20% and chaotic 51%. It is observed that the chaotic flow covers the maximum flow region where the number of secondary vortices becomes significant.

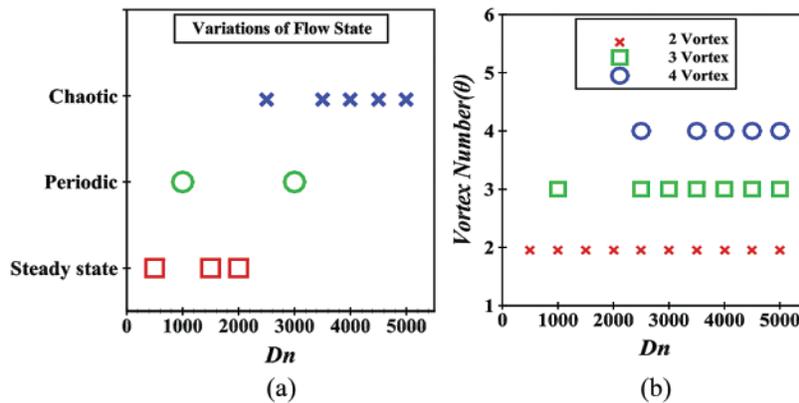


Figure 17: (a) UF characteristics over Dn , (b) Vortices of SF with regard to Dn for US

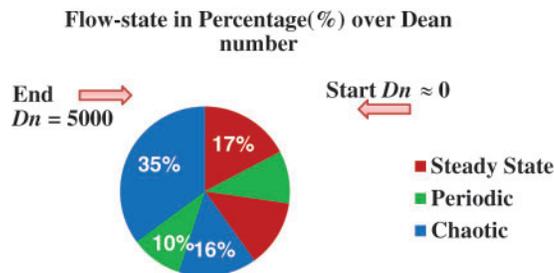


Figure 18: Percentage of unsteady flow state over Dn values

4.4 Heat Transfer

Here, heat transmission is analyzed by the study of temperature gradients (TG). As we know the TG can elucidate in which direction and at what rate the temperature changes around a particular location; therefore, TG on the cooled walls and heated walls are executed as displayed in Fig. 19. From Fig. 19a, it is seen that $\frac{\partial T}{\partial x}$ on the cooled walls decreases and tends to zero towards the central zone around $y=0$ because of increasing Dn . The Centrifugal force results in the generation of the heat transmission of the outward SF around $y=0$. On the other hand, $\frac{\partial T}{\partial x}$ is increasing monotonically in the outer zone rather than the central zone with an increase of Dn except $Dn \approx 0$. This happens to owe to the advection of the SF in the inward direction there, which is a reverse flow of the outward SF in the central zone. Fig. 19b presents that the $\frac{\partial T}{\partial x}$ is increasing in the central part with an increase up to $Dn = 4000$. But for high-pressure gradients like $Dn \geq 4000$, the rate of temperature distribution suddenly drops on the central region. Still, it increases other parts of the duct due to the fluid mixing, which indicates that HT occurs considerably between the heated wall and the fluid.

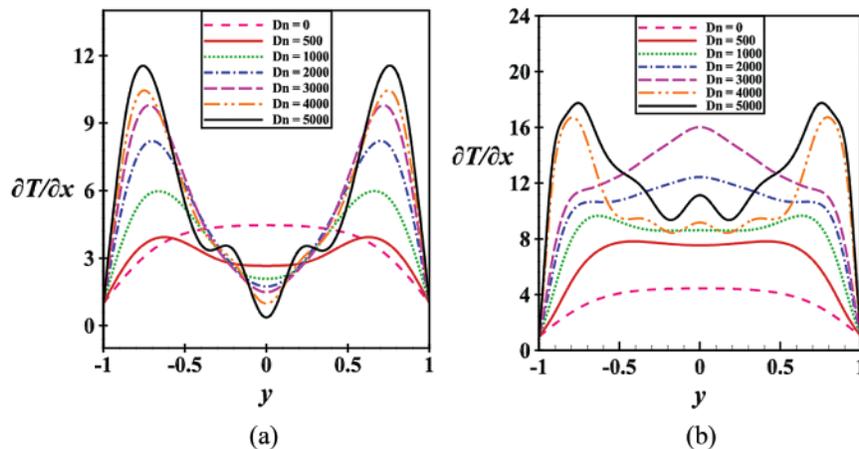


Figure 19: (a) TG at the cooling wall (b) TG at the heated walls

5 Validation test

5.1 Comparison in the Dn vs. Nu ($Dn \sim Nu$) Plane

For validation, the current numerical results subject to heat transfer with the numerical data provided by Mondal et al. [36] and Wang et al. [37] are plotted graphically in the Dn vs. Nu plane in Fig. 20. The bullets indicate the intersecting point of the specific Dean number (Dn) corresponding to the Nusselt number (Nu). A comparison of the results obtained using the cooled surface is presented in Fig. 20, where it is noticed that the three lines of the graph relating to the heat transfer show almost the same trend. The overall result also agrees well with the above-mentioned two studies.

5.2 Comparison in the Secondary Vortex

In this sub-section, the validation of our findings by comparing with the published experimental results available in the literature is performed. Figs. 21a–21d present a relative comparison of our numerical findings with the established investigations by Bara et al. [38], Mees et al. [39], Wang et al. [22] for curvature $\delta = 0.03$ and Chandratilleke [40] with $\delta = 0.032$ for a BSD flow.

Figure on the left of each pair is the SF pattern for experimental outcomes and right figures show our numerical results. As seen in Fig. 21, our present computational results have a good match with the experimental outcomes, which justifies the exactness of the present numerical study.

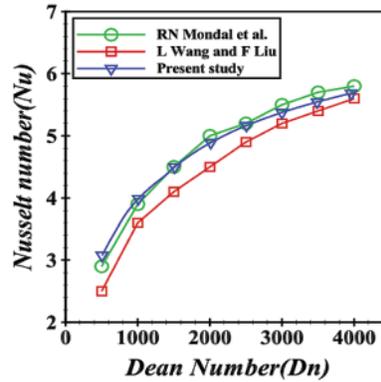


Figure 20: Comparison of the present study with the results by Mondal et al. [36] and Wang et al. [37]

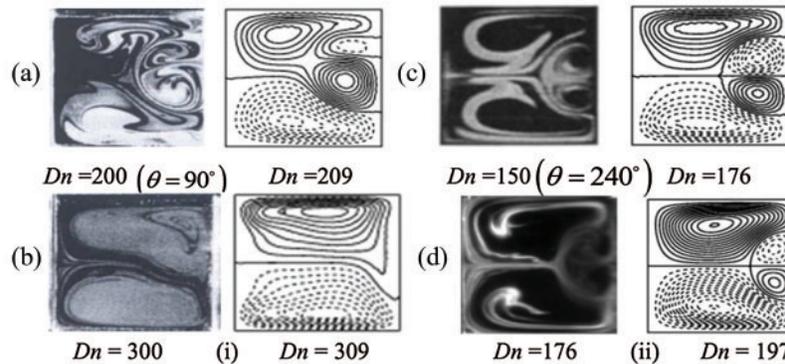


Figure 21: Investigational outcomes vs. numerical data. Left: Laboratory-based experimental results by (a) Bara et al. [38], (b) Mees et al. [39], (c) Wang et al. [22], and (d) Chandratilleke [40] and right: numerical results by the authors

Now we will deliberate the plausibility of applying 2D calculations to study bend channel flows in the present study. Mees et al. [39,41] observed traveling wave solutions in the study of BD flows. They observed the change of secondary flow pattern far downstream using a spiral duct, where Dn increases in the downstream due to an increase of the curvature. Wang et al. [22] showed that periodic flows can be analyzed precisely by 2D calculations. They showed that for an oscillating flow, there exists a close similarity between the flow observation at 270° and 2D calculation. The periodic oscillation, observed in the cross-section of their duct, was truly a traveling wave advancing in the downstream direction that was justified by a 3D study of BSD flows by Yanase et al. [42]. Therefore, it is found that 2D calculations can accurately predict the existence of 3D traveling wave solutions by showing an appearance of 2D periodic oscillation. There is some other evidence showing that the existence of chaotic or turbulent flow

may be predicted by 2D analysis. Yamamoto et al. [43] investigated helical pipe flows by 2D perturbations and compared the results with their experimental data, where they observed a good match between the numerical and the experimental data, which shows that even the transition to chaos can be predicted by 2D analysis. The transition from periodic oscillation to chaotic state, obtained by the 2D calculation in the present paper, may correspond to the destabilization of travelling waves in the BD flows like that of Tollmien-Schlichting waves in a boundary layer. Besides, 2D analysis can accurately describe the asymptotic behavior of the flows and without having a significant knowledge on asymptotic behavior of the flows, it is difficult to have a good physical insight into the BD flows. Nevertheless, complete bifurcation study obtained by the 2D analysis in the present paper, which is hardly possible in 3D analysis, may give a firm framework for the 3D study of steady, periodic and chaotic flows in the bend channel. Our 2D analysis, therefore, may contribute to the study of real flows in the BD at some extent although 3D simulation can give more accurate results but it is expensive.

6 Conclusion

In this study, a spectral-based numerical approach on fluid flow through a BSD with bottom and outer-wall heated while the upper and inner walls in room temperature have been investigated for small curvature varying the Dean number for $0 < Dn \leq 5000$. The numerical findings are validated with the available experimental data. Based on the results carried out, the following conclusions have been articulated:

- An asymmetric six branches of SSs with 2-6-vortex is found on various branches.
- Transient behavior, as well as PS density analysis, shows that the flow-state changes in the sequence $\{steady\ state, multi\text{-}periodic, steady\text{-}state, chaotic, periodic, chaotic\}$ if Dn is increased.
- Flow transition is precisely determined, and it is found that the steady-state, periodic or multi-periodic, and chaotic solution exist in 2 different regions of Dn . The intervals for various US exist like steady-state for $0 < Dn \leq 865$ and $1375 \leq Dn \leq 2010$, periodic/multi-periodic for $870 \leq Dn \leq 1370$ and $2755 \leq Dn \leq 3210$ whereas the chaotic solution for $2015 \leq Dn \leq 2750$ and $3220 \leq Dn \leq 5000$. The transition period occurs $865 < Dn < 870$; steady-state to multiperiodic, $1370 < Dn < 1375$; multi-periodic to steady-state, $2010 < Dn < 2015$; steady-state to chaotic; $2750 < Dn < 2750$; chaotic to multi-periodic and $3210 < Dn < 3220$; multi-periodic to chaotic.
- The study predicts that there exists a 2-vortex solution for steady-state, 2–3-vortex for periodic, 2–4-vortex for multi-periodic oscillation, while 2–6-vortex for the chaotic solution.
- Unsteady flow behavior shows that the steady-state flow remains approximately 29%, periodic 20%, and chaotic 51% in the entire flow region.
- The highly complex secondary flow field develops with higher Dn , and CHT is boosted significantly by the chaotic flow than other flow states.
- The study shows that the existence of axial velocity and wall pressure is greatly influenced by the Dean vortices. The present study also shows that the fluid mixing is certainly induced by the duct curvature and pressure gradient, and as a consequence, overall heat transfer is increased throughout the fluid in the curved channel.

We have plans to study MHD and nanofluid flow in a bent channel in future by CFD.

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Conflicts of Interest: The authors declare that they have no conflicts of interest to report regarding the present study.

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