



# The Effect of Inlet Angle Structure of Concave and Convex Plate on Internal Flow Characteristics of Alkaline Electrolyzer

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## ABSTRACT

The structure of the concave-convex plates has proven to be crucial in optimizing the internal flow characteristics of the electrolyzer for hydrogen production. This paper investigates the impact of the gradual expansion angle of the inlet channel on the internal flow field of alkaline electrolyzers. The flow distribution characteristics of concave-convex plates with different inlet angle structures in the electrolytic cell is discussed. Besides, the system with internal heat source is studied. The results indicate that a moderate gradual expansion angle is beneficial for enhancing fluid uniformity. However, an excessively large gradual expansion angle may lead to adverse reflux phenomena, reducing the overall performance of the electrolytic cell.

## KEYWORDS

Inlet angle structure; vortex motion; distribution uniformity; computational fluid dynamics simulation

## 1 Introduction

The implementation of carbon neutrality will enhance energy conservation and emission reduction via various approaches [1,2]. Also, it will strengthen the utilization of renewable energy [3–5]. Using the electricity generated by renewable energy to produce hydrogen is a promising way for reasonable consumption of renewable energy [6].

At present, among various hydrogen production technologies, the alkaline electrolyzer is low cost. And it is suitable for large-scale hydrogen production applications. Therefore, in recent years, many scholars have carried out a lot of research on the electrolyzer power sources [7], inputs [8], stack [9], components design, and control strategy [10] to improve the performance of alkaline electrolyzers. Additionally, researchers have explored new hybrid designs and other aspects of the electrolytic cell [11] to enhance its efficiency [12]. In alkaline electrolyzers, the main electrolytic unit's plate is often designed with a distinctive concave-convex shape, aiming to enhance both electrolytic efficiency and flow uniformity. The multi-point electrical contact on both sides of the diaphragm establishes a complex flow path within the electrolytic unit, utilizing a specific concave-convex structure [13]. This effectively improves flow disturbance and ensures uniform distribution by directing the electrolyte through a



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zigzag channel formed by the spherical concave-convex structure. While the inlet channel structure of the alkaline electrolyzer has the characteristics of micro-scale and complexity, resulting in a highly intricate flow field distribution. Therefore, comprehending the impact of the inlet angle structure on the internal flow characteristics of the electrolyzer is crucial in enhancing electrolytic efficiency, reducing energy consumption, and ensuring the long-term stable operation of the equipment.

So far, the impact of alkaline electrolyzers on corrosion and tank pressure has been reported [14,15]. Simultaneously, convex-concave structures have garnered significant attention due to their outstanding heat transfer characteristics [16,17]. Additionally, they have also been recognized for their hydrodynamic properties [18,19]. Some studies have focused on the heat transfer aspects [20,21], others on the flow dynamics [22], while some have investigated both in combination [23,24]. Thus, this concave-convex structure has been extensively investigated, including the relative placement of the convex and the surface of the ball [25] and the dislocation layout [26], as well as its structural parameters such as the height of the convex ball and the depth of the concave ball, to understand their impact on fluidity. Additionally, drawing inspiration from the sphere-concave structure, various novel convex and concave designs, including square, cylindrical, ellipsoid, and teardrop shapes, have been proposed. These designs were also investigated through experimental and simulation methods to explore their flow, heat transfer, and conductivity characteristics. Zhou et al. [27] investigated the heat transfer effect of four different pit shapes under turbulent conditions. Jongmyung et al. [28] studied the flow and heat transfer of seven pit types, with the spherical structure exhibiting the best heat transfer effect. Rao et al. [29] examined flow and heat transfer performance for the teardrop-shaped pit structure. The convex-concave structure, when combined with the electrolytic cell plate, exhibits significant potential in optimizing flow distribution within the electrolytic cell. Millet et al. [30] controlled the friction loss by adjusting the diameter of the inlet channel to ensure that the water is evenly distributed in each compartment of the cell to achieve higher efficiency. Upadhyay et al. [31] discussed the influence of different numbers of inlet and outlet and different sizes of inlet and outlet on the hydrodynamic behavior of the flow field.

In the design of water electrolytic cells, electrolytic efficiency and flow uniformity are the key factors, which directly affect the efficiency and stability of the hydrogen production process. While previous studies have focused on the micro-characteristics of concave-convex structures, the influence of inlet angle structure on the overall flow characteristics has not been deeply understood. Thus, the effect of the inlet angle structure of the concave and convex plate on the internal flow characteristics of the alkaline electrolyzer is investigated in the present work. This study aims to bridge the knowledge gaps in the current research field and provide substantial guidance for future water electrolyzer design and applications.

## 2 Methodology

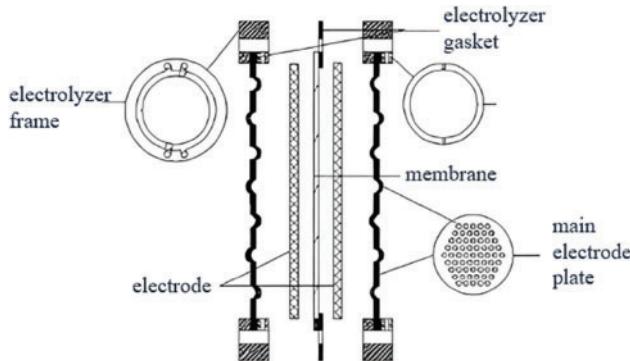
### 2.1 Simulation Model

The structure of the alkaline water electrolyzer is illustrated in Fig. 1. To simplify numerical simulation and reduce computational complexity, identical structures for the positive and negative electrode cells in the electrolytic unit is employed as the benchmark model in this study, with detailed geometrical shapes and dimensions depicted in Fig. 2. The runner structure comprises entrance, plate passage, and exit. To ensure the effective development of flow, extensions have been applied to the entrance and exit sections. Additionally, the plate channel interior features a spherical concave and convex structure. Fig. 3 presents a schematic diagram of the plate runner structure at different entrance angles ( $0^\circ$ ,  $15^\circ$ ,  $30^\circ$ , and  $45^\circ$ ). Simultaneously, to visually illustrate the variation in flow

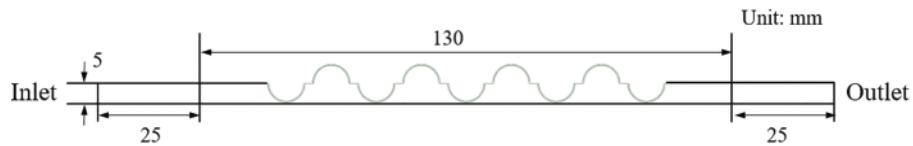
field distribution uniformity in channels with distinct structures, an assessment criterion for flow field velocity uniformity, the velocity uniformity index  $\gamma_v$ , defined based on statistical deviation, has been introduced. The uniformity evaluation index is a flow field velocity uniformity evaluation standard established by Weltens et al. [32], which can comprehensively reflect the fluid velocity distribution characteristics of the entire flow cross section, and has the characteristics of strong comparability and wide application range. The expression for  $\gamma_v$  is,

$$\gamma_v = 1 - \frac{1}{2n} \sum_{i=1}^n \frac{\sqrt{(v_i - \bar{v})^2}}{\bar{v}} \quad (1)$$

where  $\gamma_v$  is taken as  $[0,1]$ , the larger  $\gamma_v$  is, the better the flow uniformity, 1 indicates uniform flow under ideal conditions, 0 indicates that the fluid passes through only one measurement point, these two conditions are assumed conditions,  $v_i$  and  $\bar{v}$  respectively represent the velocity of the measurement point and the average velocity on the measurement section.



**Figure 1:** Structure diagram of alkaline electrolyzer



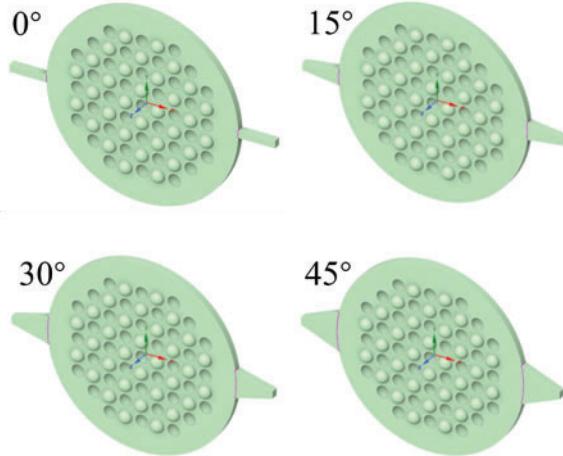
**Figure 2:** Structure diagram of a single electrode chamber of the electrolytic unit

## 2.2 Geometric Models and Meshing

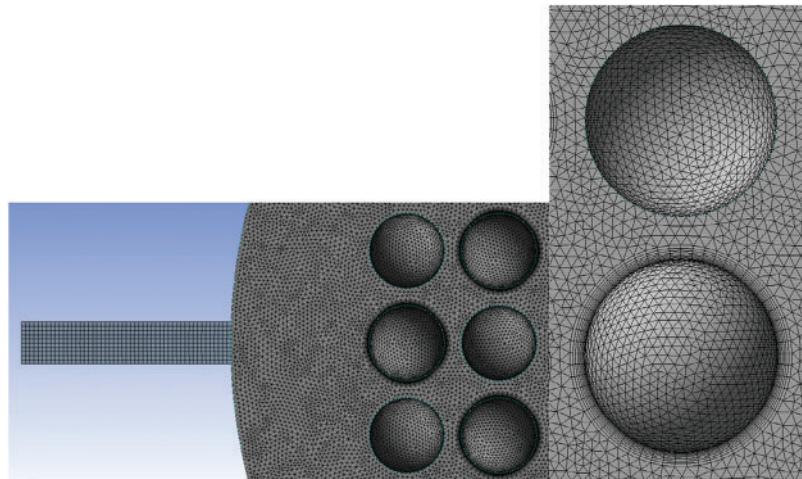
To improve the efficiency of numerical simulation, the model structure and grid were simplified. As the positive and negative cell structures of the electrolytic unit are identical, a single-cell structure was chosen as the computational model, with its geometric layout and size shown in Fig. 2. The flow channel structure comprises three primary sections: entrance, plate passage, and exit. Adjustments were made to the entrance and exit to maintain flow integrity. Within the plate channel, we examined the specific design of the bump. Fig. 3 illustrates the various inlet angles of the runner and outlines the fundamental runner design.

In this study, the mesh model is processed using Ansys Meshing software, employing a combination of structured and unstructured mesh division methods. Local mesh refinement is applied at the boundary of the concave-convex structure of the flow channel. The first layer's thickness of the boundary layer is set to 0.05 mm, with a growth factor of 1.2, and a total of 10 layers are incorporated.

The grids, as finally divided, are illustrated in Fig. 4, with a total count of 2,977,574. Subsequently, numerical simulations were performed using Fluent software.



**Figure 3:** Schematic diagram of plate runner structure with entrance angles of 0°, 15°, 30° and 45°



**Figure 4:** Grid division diagram of electrolytic unit plate channel structure

### 2.3 Mathematical Model

#### 2.3.1 Turbulence Model and Related Governing Equations

The RNG k- $\varepsilon$  turbulence model is used to simulate the low Reynolds number column group turbulent flow in the flow channel of an electrolytic cell. The governing equations are as follows:

$$\text{Continuity equation: } \frac{\partial}{\partial x_i} (\rho \bar{u}_i) = 0 \quad (2)$$

$$\text{Momentum equation: } \frac{\partial}{\partial x_i} (\rho \bar{u}_i \bar{u}_j) = -\frac{\partial p}{\partial x_j} + \frac{\partial}{\partial x_i} \left( \mu \frac{\partial \bar{u}_j}{\partial x_i} \right) \quad (3)$$

$$\text{k-}\varepsilon \text{ equation: } \frac{\partial}{\partial t} (\rho k) + \frac{\partial}{\partial x_j} (\rho k u_i) = \frac{\partial}{\partial x_j} \left( \sigma_k \mu_{\text{eff}} \frac{\partial k}{\partial x_j} \right) + G_k + \rho \varepsilon \quad (4)$$

$$\frac{\partial}{\partial t} (\rho \varepsilon) + \frac{\partial}{\partial x_j} (\rho \varepsilon u_i) = \frac{\partial}{\partial x_j} \left( \sigma_\varepsilon \mu_{\text{eff}} \frac{\partial \varepsilon}{\partial x_j} \right) + C_{1\varepsilon} \frac{\varepsilon}{k} G_k - C_{2\varepsilon} \rho \frac{\varepsilon^2}{k} \quad (5)$$

where  $\rho$  is the density ( $\text{kg/m}^3$ ),  $t$  is time (s),  $u_i$  and  $x_i$  are the velocity components ( $\text{m/s}$ ) and coordinate components (m) in the x, y, and z directions on the coordinate axis, respectively. In  $u_j$ ,  $x_j$ ,  $j$  is the three-dimensional summation subscript,  $p$  is the pressure (Pa),  $\mu$  is the laminar flow viscosity ( $\text{Pa}\cdot\text{s}$ ),  $\mu_{\text{eff}}$  is the effective viscosity ( $\text{Pa}\cdot\text{s}$ ), and  $\mu_t$  is the turbulent viscosity ( $\text{Pa}\cdot\text{s}$ ).  $\sigma_k = \sigma_\varepsilon = 1.38$ ,  $G_k = \mu_t S^2$ ,  $S_{ij} = \frac{(\partial u_i / \partial x_j + \partial u_j / \partial x_i)}{2}$ ,  $S = \sqrt{2S_{ij}S_{ij}}$ ,  $C_{2\varepsilon}^* = C_{2\varepsilon} + C_\mu \eta^{3 \frac{1-\eta/\eta_0}{1+\beta\eta^3}}$ ,  $\eta = Sk/\varepsilon$ , Empirical coefficient  $C_\mu = 0.0845$ ,  $C_{1\varepsilon} = 1.42$ ,  $C_{2\varepsilon} = 1.68$ ,  $\beta = 0.012$ ,  $\eta_0 = 4.38$ .

### 2.3.2 Operating Parameters and Boundary Conditions

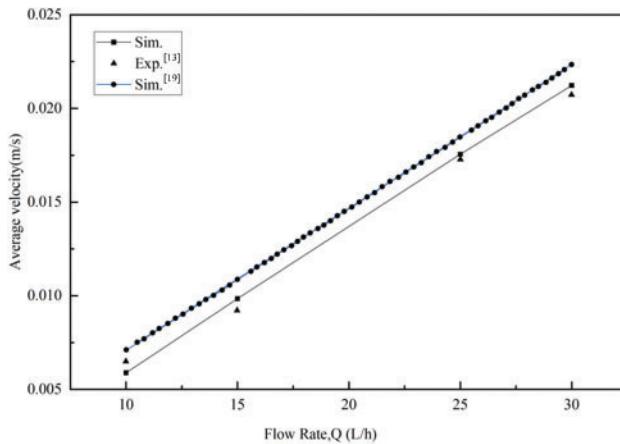
Alkaline water electrolyzers usually use alkaline electrolyte, such as KOH solution, NaOH solution, etc., generally injected electrolyte from the bottom of the electrolytic unit, to both replenish raw materials and provide some degree of cooling for the tank. Since this study focuses on the distribution characteristics of the flow field in fluid flow, water is chosen as the medium in this paper. The temperature is set to 300 K, with water density = 996.5  $\text{kg/m}^3$  and viscosity = 0.00086225  $\text{Pa}\cdot\text{s}$ .

**Boundary Conditions:** The model adopts a speed inlet boundary, with the speed set to 0.0556 m/s. The pressure outlet boundary is utilized, assumed to be fully developed, and set to atmospheric pressure. Enhanced wall functions are implemented in wall simulation. For pressure-velocity coupling, the SIMPLE algorithm is selected due to its fast convergence. A second-order upwind scheme is employed for the treatment of momentum, turbulent kinetic energy, and turbulent dissipation rate. Steady-state calculations are performed. To ensure calculation accuracy, the residual differences of energy and momentum are set as  $10^{-5}$ , ensuring the calculation reaches a converged state.

## 3 Results and Discussion

### 3.1 Model Reliability Verification

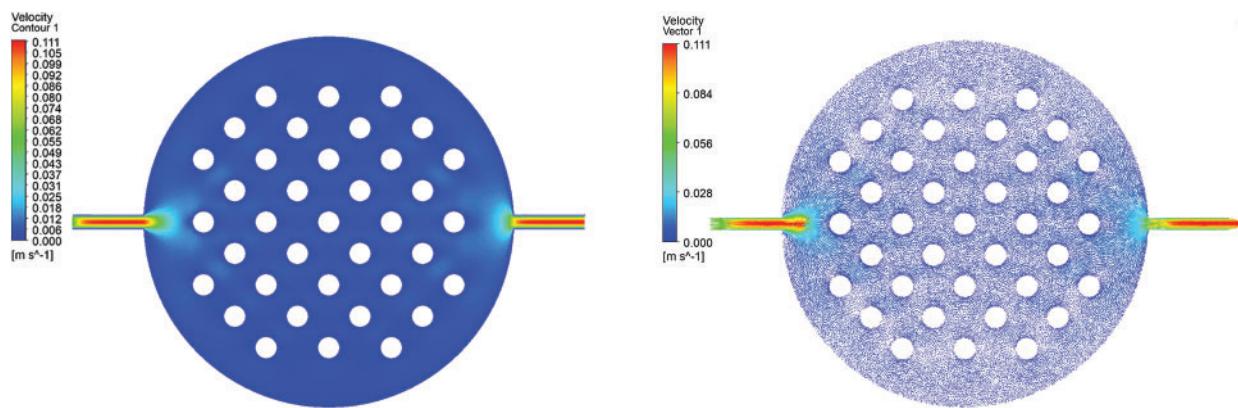
In order to verify the turbulence model and calculation method, the structural parameters of the model are consistent with previous work [19], and the structure is similar to that of hydrogen production by electrolytic water [13]. The flow velocity distribution at the center section of the tank under different flow rates is calculated and compared with the simulation data and experimental data from the aforementioned two literatures, as shown in Fig. 5. As can be seen from the figure, the simulated data is generally larger than the experimental data [13], but slightly lower than that in reference [19]. This is because the PIV velocity measurement experiment used in reference [13] may have certain phenomena of light reflection and scattering in the experimental process, resulting in partial energy loss. Compared with the structured grid division method used in reference [19], the simulation data of the PIV velocity measurement experiment may have some energy loss. In this paper, a combination of structured and unstructured grid division is adopted in the process of grid division, and the average orthogonal mass is 0.78403, which affects the calculation results to a certain extent. In general, the numerical calculation method in this study can be considered reliable.



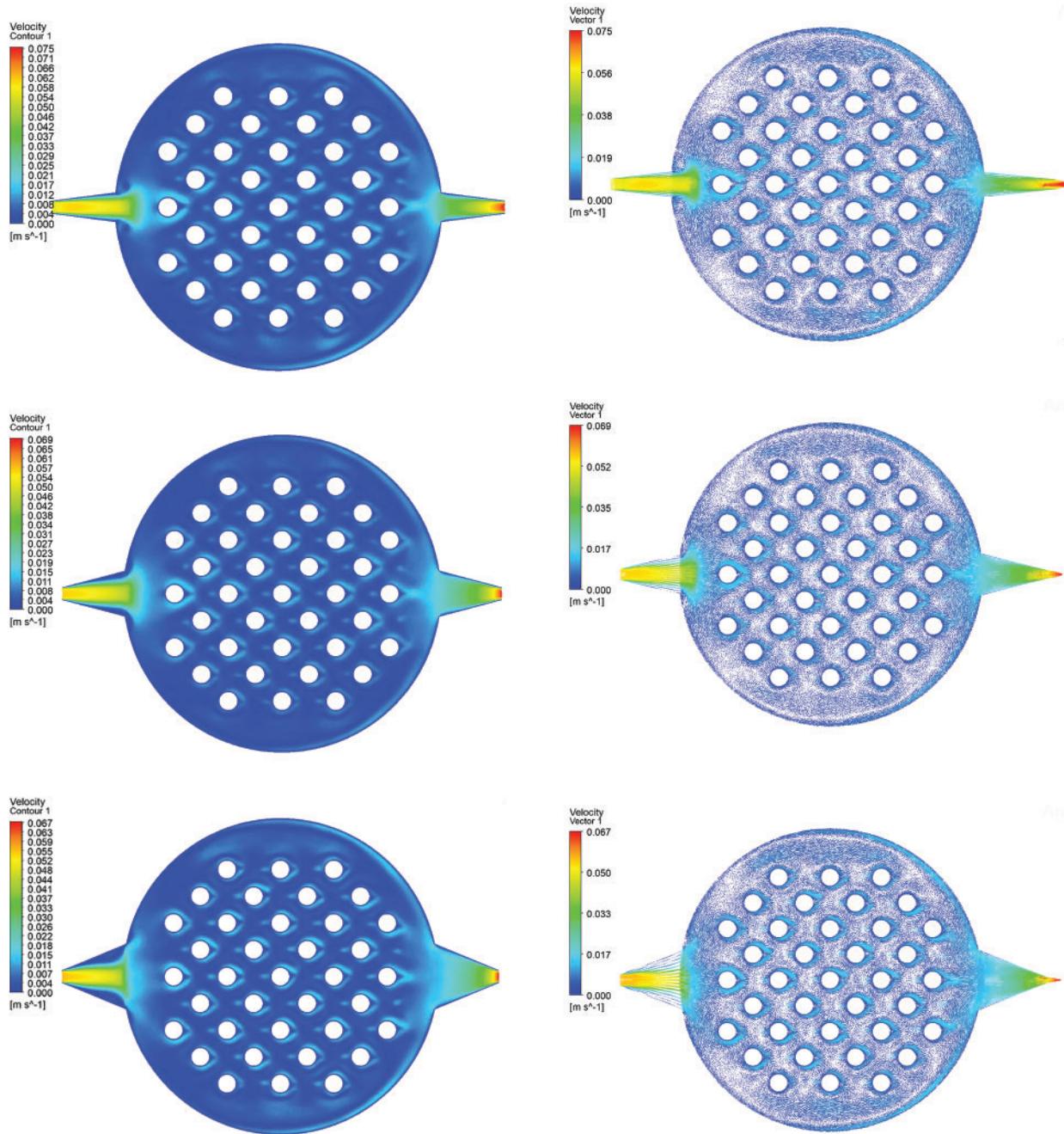
**Figure 5:** Comparison of simulated average flow velocity at the center section of electrolytic cell with data from literature [13,19] under different flow rates

### 3.2 Results and Discussion

As the fluid transitions from the narrow inlet channel to the wide plate channel, the sudden increase in the flow channel section, driven by fluid inertia, can result in a concentration effect as the fluid enters the plate channel. This phenomenon leads to fluid accumulation in specific areas and may induce vortex reflux near the inlet channel, impacting fluid mixing and uniformity, thus affecting the efficiency and stability of the electrolyzer. Contour and vector diagram analysis in Fig. 6 reveal a gradual decrease in the velocity distribution gradient of the fluid in the inlet channel with an increase in the gradual expansion angle. This suggests that a larger inlet angle is conducive to reducing the inhomogeneity of fluid velocity. However, an excessively large gradual expansion angle may lead to the formation of a return zone inside the inlet channel, negatively affecting fluid flow into the plate channel and reducing the overall efficiency of the electrolyzer.



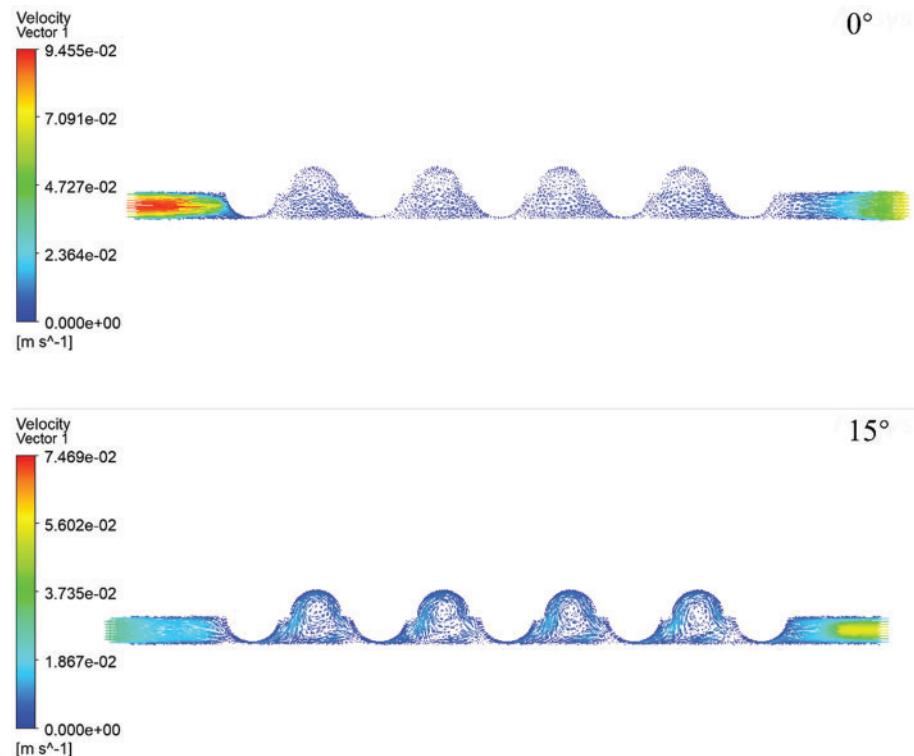
**Figure 6:** (Continued)



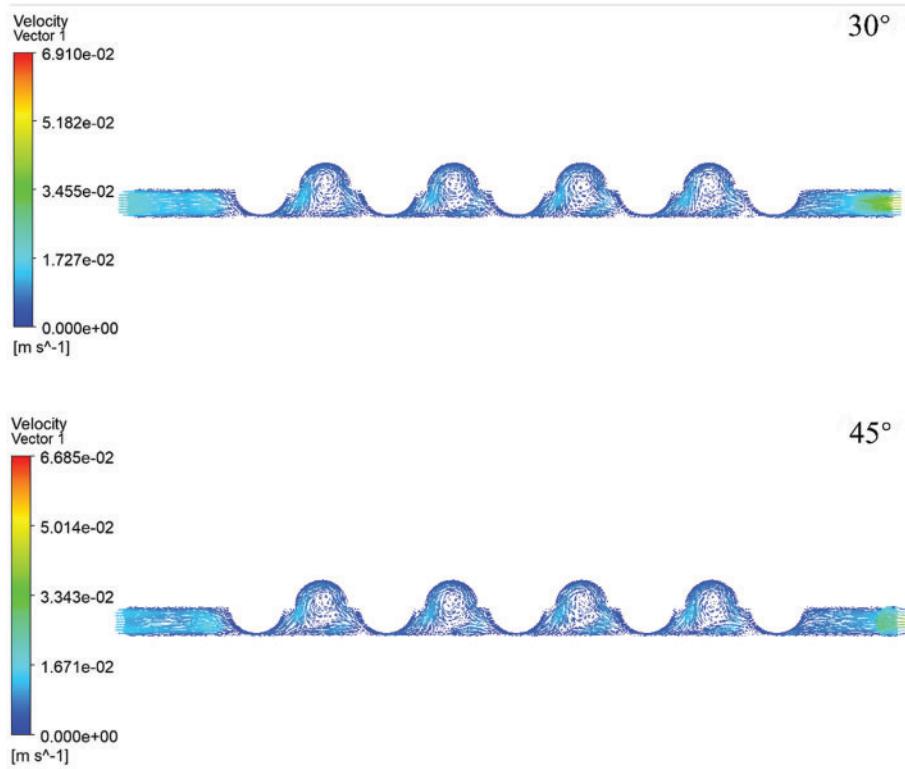
**Figure 6:** Velocity contour plot and vector diagram of the plate at different entrance angles

Through analysis of the velocity vector diagram in Fig. 7, which depicts the cross section of the channel, it can be observed that at the gradual expansion angle of  $0^\circ$ , the inlet channel velocity is concentrated, which may lead to uneven flow distribution; while at the angle of  $15^\circ$ , the inlet channel velocity is reduced, the outlet velocity is concentrated, and eddy currents at the ball bulge are evident. At the  $30^\circ$  inlet widening angle, the inlet channel velocity distribution is more uniform, the outlet velocity is relatively large, and the eddy current degree at the ball convex is similar to that at  $15^\circ$ . At

45° inlet angle, the inlet channel no longer shows velocity concentration, the outlet channel speed concentration decreases, and the eddy current at the ball convex is weak. This series of observations shows that different inlet angles cause significant changes in the flow field inside the water electrolyzer. With the increase in the gradual expansion angle, the flow presents a more uniform distribution, which may be attributed to the gradual reduction of the flow disturbance caused by the angle change, making the velocity more stable in the channel. However, this trend is accompanied by some key effects that require further analysis. First, we observe that the exit velocity decreases as the angle of gradual expansion increases. This may result in a more uniform velocity distribution due to the larger gradual expansion angle, but it restricts the maximum velocity to some extent, making us need to find a balance point between the flow uniformity and the exit velocity. Secondly, the change in vortex characteristics is also an aspect worthy of attention. When the angle of gradual expansion is low, the eddy current at the convex of the ball is relatively weak, but with the increase of gradual expansion angle, the eddy current is gradually strengthened. This suggests that adjusting the gradual expansion angle can directly influence the degree of flow field disturbance, and may have a significant effect on the mass and heat transfer performance of the electrolytic cell. In summary, the influence of different inlet angles on the flow field in water electrolyzer is complex and varied, involving flow uniformity, outlet velocity and eddy current characteristics.

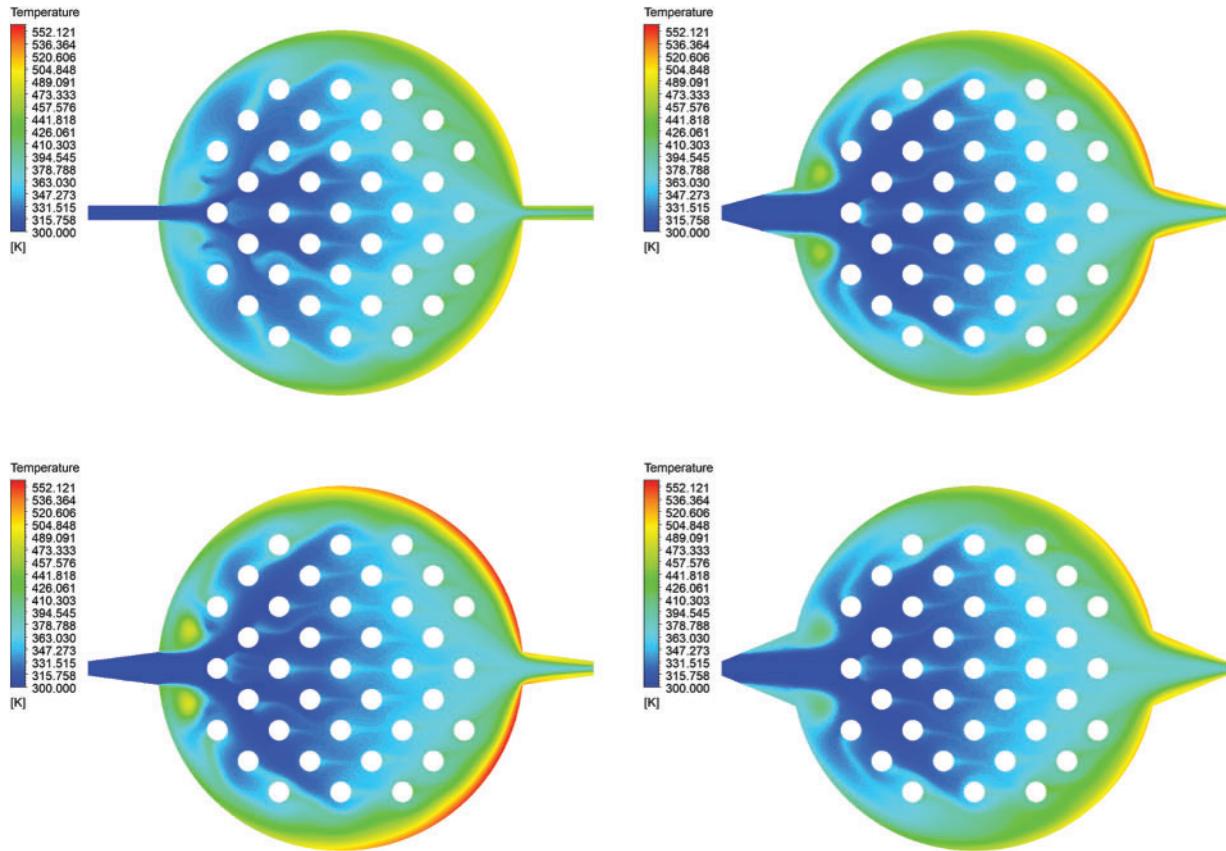


**Figure 7:** (Continued)



**Figure 7:** Velocity vector diagram distribution of channel cross section

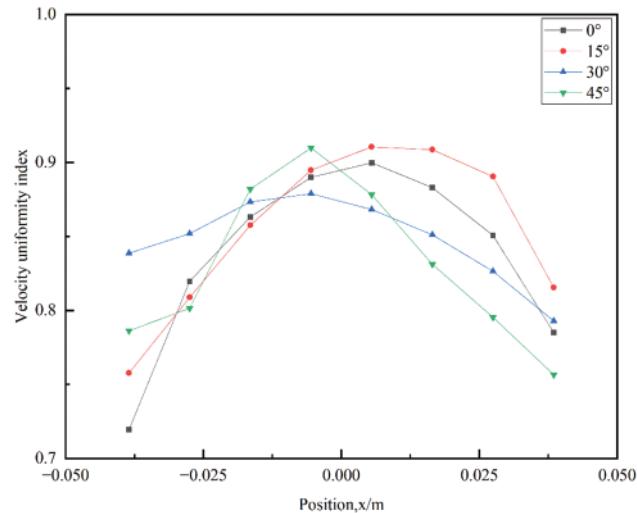
To further investigating the heat and mass transfer of the fluid within the channel of the corrugated plate, here introduces an internal heat source by adding an energy term to the main plate region. This energy source simulates the heat generated during the electrolysis process of water. By observing the temperature field distribution, an internal heat source of 600 watts is incorporated. Fig. 8 presents contour plots of the temperature distribution on the corrugated plate at different inlet angles. It is evident that there are two distinct regions on both sides of the inlet channel. These regions may be attributed to vortices when the fluid enters the circular corrugated plate through the inlet channel. The local temperature rises due to resistance and turbulence. Additionally, a high-temperature layer consistently exists on the right edge of the main plate, which is results of the temperature boundary layer. The temperature boundary layer refers to the region where the fluid experiences temperature changes near a solid surface due to heat transfer. The presence of high temperatures on the right edge of the main plate can be attributed to the sudden reduction of the flow channel cross-section as the fluid exits the plate, leading to inadequate outflow and accumulation on the right side. From the velocity contour plot and vector diagram of the plate at different entrance angles in Fig. 6, we can also find that there is a flow boundary layer at the bottom of the outlet of the main plate channel, which explains the objective cause of the temperature boundary layer. At the same time, considering that our simulation does not take into account the existence of external flow fields, the heat stored in the plate is partially unable to dissipate to the environment, which also exacerbates this phenomenon. Furthermore, it is observed that as the inlet angle increases, temperature non-uniformity becomes evident in the inlet channel, further confirming that excessive inlet angles are not advisable.



**Figure 8:** Temperature contour plot of the plate at different entrance angles

Fig. 9 shows the  $\gamma_v$  distribution diagram of the velocity uniformity index along the passage of the electrolytic cell with different inlet angles. It can be seen from the diagram that the velocity uniformity index of each inlet angle structure presents a trend of first increasing and then decreasing. This is because in the beginning of the process, the fluid enters the main plate channel from the narrow entrance, and the sudden increase in the cross section of the flow channel leads to the inertia of the fluid can not be well filled to the entire main plate channel, so the velocity uniformity index  $\gamma_v$  of the entrance of the channel is generally low. As the flow progresses, the fluid gradually adapts to the geometric structure of the main plate channel, forming a more stable flow pattern at the end of the channel. During this process, key flow phenomena, such as flow redistribution and the formation or disappearance of vortices, may impact the velocity uniformity index. However, in the latter part of the channel, as the flow further advances, complex phenomena such as boundary layer thickening, turbulence strengthening, or other nonlinear effects may occur. These phenomena could lead to increased local velocity fluctuations, thereby reducing the overall velocity uniformity. The sudden reduction in flow cross-section at the exit becomes another crucial factor affecting velocity uniformity. This reduction may result in increased flow velocity, pressure changes, and flow field reconstruction, contributing to enhanced turbulence, vortex formation, and further non-uniformity in the overall velocity distribution. Therefore, the observed pattern of an initial increase followed by a decrease in the velocity uniformity index may be attributed to a combination of fluid adaptation to

channel geometry, overcoming inertia effects, and the complex nonlinear flow phenomena, along with the abrupt change in flow section in the later stages of the channel.



**Figure 9:** Exponential distribution of velocity uniformity along the channel

Thus, it can be concluded that the inlet angle is a parameter requiring careful consideration and optimization. While appropriate scaling enhances fluid uniformity, excessive scaling may introduce undesirable hydrodynamic effects. Therefore, in the design and optimization of the gradual expansion angle, a comprehensive consideration of fluid dynamics, efficiency, and the desired fluid uniformity is necessary to achieve optimal cell performance.

#### 4 Conclusion

In this study, we conducted a comprehensive investigation of the internal flow characteristics of alkaline electrolyzers. The key findings of our study are summarized as follows.

As a key structural parameter of an electrolyzer, the inlet angle plays an important role in alkaline electrolyzer performance. By comparing different angles of gradual enlargement, we found that moderate gradual enlargement can indeed improve the uniform distribution of fluid. Generally, angles between 15° and 30° perform better. A large angle of entrance may lead to backflow phenomena and other adverse hydrodynamic effects, which reduce the overall performance of the electrolyzer. Therefore, in practical applications, the inlet angle and other design parameters need to be carefully considered.

It is worth noting that as a complex engineering system, the performance of alkaline electrolyzers is affected by many factors. The research in this paper also has some limitations. The assumptions in the simulation model are too simplified, for example, the variable property parameters of the simulated fluid are not considered. In addition to the inlet angle structure, other factors such as the rheological properties of the electrolyte, the choice of electrode materials, and operating conditions may have an impact on the overall performance of the electrolyzer. Therefore, further optimized designs and structures will be discussed based on the experiments in our future works.

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**Availability of Data and Materials:** Data will be made available on request.

**Conflicts of Interest:** The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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